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Impact on the cattle feedlot industry in Eastern Australia from grainbased ethanol production



Abstract

The Australian Government is committed to the establishment of a grain-based ethanol production industry. Any increased competition for grain could adversely affect the cattle feedlot industry. While the sector could benefit from a plentiful supply of distillers grain by-product, if it became available, the most energetically efficient and environmentally friendly ethanol plants use the distillers grains as a source of fuel within the plant, and none becomes available for sale to the livestock industries.

The additional grain demands for E10 ethanol production could be met from national grain production in years of above average and average yields, but not in years of low yields. Within a region with a major feedlot capacity, one 160ML ethanol plant would lead to grain being imported into the region in some years. If distillers grains were available for inclusion in feedlot diets, a 160 ML plant would provide enough sorghum distillers grain to support a ration contribution of 25% of the dry matter for 80,000 feedlot cattle every day of the year within the zone of economic transport of the distillers grain.

Executive Summary

1 INTRODUCTION

In recent years, the Australian Federal Government has articulated a commitment to the development of the biofuels industry through the production of biodiesel and ethanol, with attention currently being focussed on expanding Australia's production capacity.

Australia currently has an annual ethanol production capacity of about 165 ML, although actual production is usually in the range of 108–145 ML. The Australian Government has introduced a number of measures to encourage ethanol production as part of a broader policy agenda to promote the use of biofuels in Australia. These measures have three main components as outlined below:

- A commitment that biofuels produced in Australia from renewable resources should contribute at least 350 ML annually to Australia's total fuel supply by June 2010. [It should be noted that this target of 350ML includes both biodiesel and ethanol production.]
- The Biofuels Capital Grants Program [introduced in July 2003 and modified in March 2004] to provide one-off capital subsidy for new and/or expanded projects producing biofuels from renewable resources or biomass waste products. Grants were limited to a maximum of \$10 million per project, and at its completion, seven projects were offered grants totalling \$37.6 million a total of \$12.4 million for three ethanol projects and the balance for the four biodiesel projects.
- The Ethanol Production Grants Program which effectively offsets the excise on domestically produced biofuels until 30 June 2011. From 1 July 2011 to 1 July 2015, the excise will be phased in through five equal annual instalments to reach a final rate of 19.1 cents per litre for bio-diesel and 12.5 cents per litre for ethanol. The final rate represents a 50% discount on excise as compared to other fuels with the same energy content. It will apply to imported ethanol as well.

About 10 new plants are in various stages of planning. Their production capacity is projected to be 1265 ML per annum. Currently there is uncertainty surrounding the details of some proposals. The planning for some has progressed, albeit slowly, and some are stalled. Uncertainties about the cost and supply of feed grains and the sale of ethanol and the by–products are limiting progress. However it is realistic to estimate that across Australia, feed-grain based ethanol production may contribute in the order of 275 to 350 ML annually by 2010. This equates to 1.5% of Australian petrol consumption. If Australia were to mandate 10% ethanol in petrol (E10), 2500 ML of ethanol would be used annually.

Because of concerns about the possible impacts on grain supply for the cattle feedlot industry related to the use of grain for ethanol production, the MLA commissioned this project to address the pertinent major issues. These are, in particular, the potential impact on grain supplies, the availability of the distillers grain by-product, and the capacity of the feedlot industry to utilise this by-product. The particular focus was to establish the likely supply of distillers grain products under Australian crop and ethanol production conditions, and to assess its potential usage in the feedlot industry, taking into consideration its suitability as a feedstuff, costs, established industry practice, infrastructure, and operational considerations.

The project provides the Australian feedlot industry, and its participants, with detailed information on the likely impact on grain supply, the resource energy use and the environmental consequences of an ethanol industry with a competitive advantage for grain purchase. It also provides current information on the nutritive value of distillers grains and the extent to which they can be included in feedlot diets.

The objectives of the project were to:

- Establish the likely grain usage (total and regional) and subsequent production (total and regional) of distillers grain given current and proposed development of grain-based ethanol production facilities to meet the existing government annual target of 350 ML ethanol production, assuming 75% of this production will occur from feed grains.
- Extrapolate this data to evaluate the potential situation should the government move to a position of mandating an E10 inclusion policy.
- Provide a technical assessment of the energetic costs and benefits of ethanol production from grain, under Australian crop and ethanol production conditions.
- Determine a realistic feed value of both the wet and dried distillers grain products under Australian conditions and establish a protocol, which accounts for the variability in the base product because of ethanol extraction efficiency and variable water content, for determining this value.
- Evaluate the likely potential usage of the wet and dried distillers grains in the feedlot sector, given the location, production quantities, and costs of the distillers grain supply in relation to potential feedlot users and likely ration inclusion levels.
- Recommend any additional R&D necessary to establish the value of wet and dried distillers grain under Australian conditions.

The project was undertaken by a consortium of CSIRO Divisions (Livestock Industries, and Energy Technology), and Aquila Agribusiness Pty Limited. Each of these groups has produced a separate report (included as Appendices), with this report summarising the approach and key findings relevant to the objectives.

The roles of the three organisations were:

- Aquila Agribusiness Pty Limited investigated the availability of grain in Eastern Australia, current plans for feed-grain based ethanol production, and the availability and likely use of the distillers grain by-product by the cattle feedlot industry.
- CSIRO Livestock Industries undertook a scientific evaluation of the nutritive value of distillers grains in Australia and the limits to their inclusion rates in feedlot diets.
- CSIRO Energy Technology prepared an overview of world ethanol developments and used a 160 ML per annum hypothetical ethanol plant in New South Wales to prepare a life cycle analysis which documented the energy use and generation, water balances and greenhouse

gas implications. A techno–economic analysis for ethanol production at this plant was also carried out. Both studies considered wheat and sorghum as feedstocks.

Coordination of the project, and a contemporary industrial focus of the whole project, was achieved through regular interaction with an MLA Advisory Committee.

2 GRAIN SUPPLY AND DEMAND

Over the last decade, grain production in eastern Australia (barley, corn, oats, sorghum, triticale, wheat) fluctuated between 11 and 27 million tonnes, depending on the season. Within the eastern Australian Statistical Divisions, annual productions were commonly 30 – 50% of maximum annual yields. Yields as low as 15% of the maximums also occurred.

Ethanol production would require significant supplies of grain feedstock, with the indicative amounts depending on the type of grain as shown in Table 1.

Parameter	Unit	Corn	Wheat	Barley	Sorghum
Dry matter	% AR	88.0	90.0	88.0	88.0
Starch	% DM	70.0	65.3	60.0	74.6
Ethanol yield	L/t grain	382	365	327	407
Grain to produce	t/160 ML	419,000	439,000	489,000	393,000
Wet distillers grain@ 30% dry matter	t/160 ML	386,000	481,000	591,000	310,000
Dry distillers grain @90% dry matter	t/160 ML	129,000	160,000	197,000	103,000

Table 1 Ethanol production - feedstock and products

AR, as received

DM, dry matter

These results show that a typical plant of 160 ML requires between 390,000 and 490,000 tonnes of grain per annum, and produces between 100,000 and 200,000 tonnes of dry distillers grain (90% DM basis). The current Commonwealth government annual target of 350 ML, of which 75% is assumed to be derived from grain, therefore requires 650,000 to 800,000 tonnes of grain each year.

The cattle feedlot industry in eastern Australia is a major user of feed grain, with usage in 2006 estimated at 2.5 million tonnes. Grain, surplus to domestic requirements for the intensive livestock industries and human consumption, is exported. In recent years, with average seasonal conditions, exports were in the order of 15 million tonnes. In the low yielding years of 1998 and 2006, the exports were as low as 3.5 million tonnes.

Murrumbidgee in New South Wales is a major grain producing Statistical Division, and has a substantial cattle feedlot industry (133,000 Standard Cattle Units (SCU's) in June 2006). Annual grain yields fluctuate between 1 and 2.5 million tonnes. Even in low grain yielding years, this region could support current grain demand in addition to that of a 160 ML ethanol plant. In such years, the surplus grain would be 100,000 - 200,000 tonnes, depending on the level of distillers grain incorporated into feedlot rations.

The situation is quite different in the south east Queensland Statistical Divisions of Darling Downs, Moreton, Brisbane and Wide Bay–Burnett. The annual grain production in this region varies between 1.2 and 2.6 million tonnes. Its cattle feedlot capacity is the largest in the country at almost 400,000 SCU's. Any new grain demand by a 160ML ethanol plant, in addition to current grain demands, could only be met under the best seasonal conditions. In average years, the grain deficit would be 400,000 tonnes, and in the years with poor seasonal conditions, almost a million tonnes. The interdivisional movement of grain could reduce or remove the deficit. However the transport of up to a million tonnes of grain in any one year requires considerable transport infrastructure. It would also increase the cost of grain delivered to feedlots.

The northern New South Wales Statistical Division is eastern Australia's major grain producing region with the second largest feedlot capacity (158,000 SCU's). Grain yields fluctuate from 3.8 million tonnes in good years to 1 million tonnes in poor years. The additional grain demand by a 160ML ethanol plant could be met locally every year. Even in years of low grain production, the surplus would be almost half a million tonnes, although the majority of this surplus would likely be required in the south east Queensland region if this area was also experiencing a low production year.

Impact of an E10 inclusion policy

If Australia mandated an E10 inclusion policy (10% ethanol in petrol), the annual ethanol demand would be 2500 ML. In the short term, it is likely that the majority of this ethanol would be derived from grain-based production. The supply of 75% of this amount of ethanol from grain would require annually 5.1 million tonnes of wheat, or 4.6 million tonnes of sorghum. If 95% of the ethanol was from grain the tonnages would be 6.5 and 5.8 million tonnes respectively. This would lead to a national shortfall of grain in some years, and would be exacerbated within a region in low yielding years.

Over the whole of eastern Australia, assuming the transport of grain between regions was logistically and economically feasible, the additional demand of these quantities of grain could only be met in high and average grain yielding years. In the lowest yielding years, the deficit would be up to 4 million tonnes annually, depending on the proportion of ethanol derived from grain. In this situation, the ethanol industry's demand for feed grains will significantly impact the intensive livestock industries. Grain shortages in areas such as south east Queensland will become more acute and more frequent. Cattle feedlots that continue to operate will be faced with higher grain prices. It is likely that the adverse effect of the feedlot industry will flow onto the entire Australian cattle industry, given that 34% of slaughter cattle or 2.6 million head are currently finished in feedlots.

3 NUTRITIVE VALUE OF DISTILLERS GRAINS

The principal by-products of ethanol production in a conventional plant are wet distillers grains and condensed distillers solubles. These are commonly mixed to produce wet distillers grains with solubles. This product has a dry matter content of about 30%. The product can be dried to produce dry distillers grains with solubles. This product has a dry matter content of about 30%.

The chemical composition of distillers grains depends on the composition of the parent grain, the efficiency of conversion of starch to ethanol and the composition of the solubles in the grain; the more efficient the conversion, the less starch remains as residual in the distillers grains. The

fermentation process removes starch and other soluble sugars, thereby concentrating up the other chemical components of the parent grain.

There is plentiful information from the United States on the chemical composition and nutritive value of wet distillers grain from corn, and some information from barley and sorghum. There are also some data from the UK for corn, wheat and barley and the resultant distillers grains. The residual starch content of the distillers grains varies from 1-2% in barley, 2-7% in corn, 5-10% in sorghum and 1-5% in wheat on a dry matter basis, depending on the process efficiency. Principally because of concentration of fat, the energy density of distillers grains is usually higher than that of the parent grain. Literature values for metabolisable energy content of northern hemisphere distillers grains vary from 11 MJ/kg dry matter for sorghum to 16 MJ/kg dry matter for corn. Barley and wheat are intermediate at between 12 and 13 MJ/kg dry matter. Crude protein content varies from 21-30% for barley, 9-19% for corn, 23-50% for sorghum and 30-44% for wheat. Typical fat contents vary from 3 - 4% for wheat and barley to up to 11% for sorohum and corn. The concentration of minerals in distillers grains need to be taken into account in the formulation of total mixed rations. Phosphorus contents vary from about 0.7% for barley to 0.9% for sorghum so there is potential for accumulation in the environment unless mineral contents of other ration inclusions are adjusted accordingly. The greater availability of nutrients from steam flaked compared to dry rolled grain will also influence the formulation of rations which include distillers grains.

There are currently no data on the chemical composition and nutritive value of distillers grains in Australia, apart from that produced at the Manildra plant in Nowra. This plant mostly uses starch from other grain processing operations, but sometimes uses grain to provide additional feedstock. In order to evaluate the nutritive value of distillers grains derived from Australian barley, corn, sorghum and wheat, a methodology has been adopted that assumes that mass balances can be calculated for changes in chemical composition of the grain as a consequence of removal of fermentable carbohydrate during ethanol production. On average, from northern hemisphere data, 2% of the starch and 10% of soluble non-starch carbohydrate remain unfermented by yeast during ethanol production. These values were assumed to apply in determining the likely chemical composition of Australian distillers grains. There is some uncertainty about the role that grain solubles play in determining ethanol/distillers grain yields for grains of interest in Australia and refinement of these estimates will be possible as more experience emerges.

The Project Team and the MLA Advisory Committee agreed that the starch compositions of Australian barley, corn, sorghum and wheat, from Rendell (2006) would be those used in the determination of nutritive value, as those values typified the average compositions of Australian grains. Further, it was agreed that the range of compositions, encountered in Australia, would be accommodated by increasing and decreasing the Rendell starch content by 5%. Thus, the starch contents used for barley were from 57-63%, for corn 67-74%, for sorghum 71-78% and for wheat 62-67%. The consequent changes in the other components were made according to patterns established in existing information on Australian grains.

The nutritive value of grains and distillers grains for ruminant feeding in the USA was determined using the Cornell Net Carbohydrate and Protein System (CNCPS). Estimations of the nutritive value of distillers grains in Australia were made, using the CNCPS software. Using the grain compositions discussed above, and assuming the levels of starch conversions to ethanol by fermentation noted previously, the compositions of distillers grains were calculated. These data were then used to predict the upper limits to the inclusion rates of distillers grains in illustrative feedlot diets formulated to contain 15% crude protein. The model also predicted the liveweight gain of cattle fed these diets.

The inclusion rates of distillers grains in the diets were governed by the protein content of the distillers grains. Lower protein content allowed more of the distillers product to be included under the cap of 15% protein in the total diet. Inclusion rates varied from 5% for low starch, high protein wheat to 40% for low protein, high starch barley. Limits to inclusion rate for corn and sorghum were in the range of 23-35%. In all these illustrative diets, distillers grain was substituted for the protein meal component of the ration. For wheat based diets, the predicted liveweight gain did not vary by more than 0.1kg/d irrespective of whether cotton seed meal or distillers grain was included in the diet (1.9-2.0 kg/d). For sorghum, predicted liveweight gain varied from 1.7 kg/d for low starch sorghum and sorghum distillers grain to 2.1 kg/d for high starch sorghum and distillers grain.

Predicted liveweight gains for diets which included distillers grains were generally in the vicinity of 1.9 to 2.1 kg/d, with the exception of distillers grains from low starch sorghum which was 1.7 kg/d. Diets without distillers grains where cotton seed meal was the major protein source, generally also achieved liveweight gains in the vicinity of 1.9 to 2.0 kg/d.

Potential use of distillers grain in cattle feedlot industry

As shown in Table 1, a 160 ML per annum ethanol plant would produce 591,000, 386,000, 310,000 or 480,000 tonnes of wet distillers grain from input grains of barley, corn, sorghum or wheat respectively, each year. E10 production of 2500 ML per annum of ethanol would produce about 9.2, 6.2, 4.8, and 7.5 million tonnes of wet distillers grains from these grains, respectively.

The 4.8 million tonnes of sorghum wet distillers grain that could potentially be produced each year under E10 is sufficient to feed about 1.25 million head for 365 days a year. This assumes a feed intake of 15 kg per head per day on an as fed basis and an inclusion rate of 25% of sorghum distillers grain in the dry matter of the diet. The feedlot industry does not have this capacity currently. Surveyed feedlot capacity in 2006 was 1.13 million head. On a regional basis, a 160 ML per annum ethanol plant producing 310,000 tonnes of sorghum distillers grain per year could support the daily feed requirements of about 80,000 head of cattle for 365 days a year.

For these calculations to be of practical significance to the feedlot industry, most of the distillers grains would need to be produced sufficiently close to feedlots to make transport cost effective.

4 ETHANOL PRODUCTION

The role of CSIRO Energy Technology (CET) was "to provide a technical assessment of the energetic costs and benefits of ethanol production from grain, under Australian crop and ethanol production conditions", and to assist CSIRO Livestock Industries to "determine a realistic feed value of both the wet and dried distillers grain products under Australian conditions and establish a protocol, which accounts for the inherent variability in the product due to differences in the base product, ethanol extraction efficiency and water content, by which this value can be calculated". In assisting with the latter objective, CET was tasked with determining a realistic economic and environmental value of wet distillers grain, by examining the costs and greenhouse gas emissions of drying and transport.

These objectives for CET were addressed by carrying out a life cycle and techno-economic analysis for ethanol production from wheat and sorghum, using a number of options for processing the

stillage. The analysis was based on a hypothetical plant located at Gunnedah, with a capacity of 160 ML of ethanol per annum.

Whilst a mature technology, ethanol production is continuing to evolve, with improvements throughout the entire process. Anaerobic digestion of stillage is becoming of increasing interest in the USA as a result of over supplies of distillers grain, as well as for offsetting increasing gas and electricity prices.

The analysis considered the life cycle issues of resource energy, greenhouse gas emissions (GGEs), and water consumption, as well as techno-economics.

Resource energy quantifies energy depletion, and relates only to fossil energy inputs; solar energy used for growing the grain is excluded, since it does not represent a depletion of energy resources. *Greenhouse gas emissions* are emissions of CO_2 and CH_4 that are generated in the production and combustion of fossil fuels, as well as nitrous oxide produced from the use of nitrogenous fertilisers. Carbon sequestered from the atmosphere by grain, provides a GGE credit.

Water consumption relates to the amount of fresh water used in the production of fertilisers, fuels, etc (in the form of process water), and is used to quantify the depletion of fresh water resources. Water from rainfall used in grain production is not included.

The study considered 3 systems for the Life Cycle Analyses (LCAs):

- 1) grain production (wheat and sorghum),
- 2) grain through to ethanol with 7 stillage processing options, and
- 3) grain through to 1 GJ of delivered heat energy (*ie* as combusted ethanol).

For ethanol production, the base process routes were fermentation with the production of dry distillers grain, and fermentation with anaerobic digestion and electricity production. This resulted in 7 case studies, for alternative stillage processing:

- Case 1 Wet Distillers Grain (WDG) direct to feedlot.
- Case 2 Dry Distillers Grain with Solubles (DDGS) with conventional drying.
- Case 3 DDGS with high efficiency drying.
- Case 4 Anaerobic digestion, with gas engine electricity generation (33% efficiency; HHV basis).
- Case 5 Anaerobic digestion, with combined cycle electricity generation from biogas (50% efficiency).
- Case 6 WDG for electricity generation by fluidised bed combustion (20% efficiency).
- Case 7 WDG for electricity generation using integrated drying and gasification combined cycle (IDGCC; 40% efficiency).

Life Cycle Analyses (LCAs)

For grain production, the major resource energy component is for the production of fertiliser (70% of the total). GGEs are dominated by the CO_2 taken up by the grain during photosynthesis, while fresh water is dominated by the water used to grow the grain (500-1000 m³/t grain). It should be noted that the CO_2 sequestered in the grain will ultimately be returned to the atmosphere, partly during production of ethanol, and also when the ethanol is combusted. However, the LCA methodology (with the boundary conditions of either grain production, or ethanol production) requires that the CO_2 sequestered in the grain be included. Values without such sequestration have been included for comparison with other non-compliant LCA studies.

When the grain is processed to ethanol, all indicators are dependent on the processing of the stillage, and by-product credits. Process water consumption is again several orders of magnitude less than that used for growing the grain.

There are 3 key findings for resource energy for ethanol production:

- With direct sale of WDG, the resource energy is considerably lower than that for DDGS, due to the large amount of energy required for drying (can be substantially reduced using a higher efficiency process).
- When the stillage is anaerobically digested, the resource energy also becomes negative, since there is no requirement for purchased electricity or natural gas for ethanol production and credits are allocated for by-product fertilizers and exported electricity.
- There are also significant credits for by-product fertilisers and exported electricity. If the WDG is combusted to produce electricity (requires a technology similar to high moisture lignite or biomass), a negative overall resource energy is produced.

The main findings for GGE for ethanol production are as follows:

- All cases have a negative GGE, due to sequestration of CO₂ as grain.
- Direct use of WDG by feedlots gives a lower GGE than for DDGS, due to the emissions associated with drying (again, reduced by a higher efficiency process).
- Use of WDG or DDGS as feed to replace grain increases the overall GGE, as this displaces grain production and lowers the CO₂ being sequestered by photosynthesis.
- WDG can be transported for a large distance (>1000 km) before the GGEs from transport exceeds the GGEs from drying and transport of the DDGS (*cf* the economical distance of only 50-60 km).
- Anaerobic digestion of the stillage gives lower GGE, due to the use of combined heat and power; *i.e.* the use of waste heat from power generation for the fermentation. A similar conclusion applies to the combustion of WDG for electricity generation.

• All of the alternative technologies reduce the overall GGE, with the highest efficiency electricity generation case (with biogas combined cycle, or IDGCC) virtually offsetting the upstream GGEs for ethanol production.

Comparison with other LCA studies

In comparison with the other Australian studies on wheat production, similar GGEs and process water values were obtained, when compared on a similar basis. The values for resource energy, however, vary considerably (some of which may be attributed to different locations).

For ethanol production, comparison with other studies is complicated by uncertainties in how byproducts have been credited, and in some cases by the use of petrol blends as the functional unit. In addition, many of the studies, incorrectly, do not consider the CO_2 sequestered by the grain through photosynthesis, as required by LCA methodology; this significantly reduces the GGE benefit of ethanol production from grain.

Comparison of ethanol and petrol

Using current technology, the life cycle GGEs for ethanol are always less than those for petrol, with ethanol cases involving exported electricity being very much lower. This benefit is likely to be greater in the future due to the potential use of CO_2 capture technologies in the ethanol plant and in power generation from stillage.

Most previous studies have compared ethanol and petrol on the basis of equivalent energy delivered - as fossil energy replacement. Most US studies (based on corn) have shown that, on a fossil fuel basis, the production of ethanol results in approximately 30% more energy than the fossil energy used in its production. The present study has shown similar results for the WDG case. DDGS results in a small negative net energy.

If DDGS were to be the likely by-product from ethanol production in Australia, then, from a resource energy perspective, ethanol production would not contribute to a reduction in the overall energy required for transport, when taking a life cycle approach.

For anaerobic digestion (with electricity generation using internal combustion engines) there is a marked improvement in net energy -2.5-3 times better than for WDG, or than for previous overseas studies.

Overall, ethanol production from grain gives significant resource energy and GGE benefits in comparison to petrol. The exception is for resource energy when DDGS is the by-product. Of course, a number of other issues also need to be taken into account, such as grain availability, acceptability, economics, *etc*.

Techno-economics

Because of the potential variations in key cost parameters, a matrix of values was used for grain price, electricity price/cost, and by-product credits. The findings are that:

• The techno-economic analysis shows the dominating role that the grain feedstock plays (50-80c/L of the ethanol production cost).

- The next most significant issue is the choice of stillage processing whether to produce WDG, DDGS, or biogas/solid fuel for electricity production. In practice, the choice of process will also depend on a number of interrelated factors – capacities, the process route, byproduct credits, and the ability to exploit opportunity biomass, such as straw.
- Sorghum gives lower unit feed cost, but overall production costs are similar due to lower credits (higher level of starch in the sorghum produces a higher yield of ethanol, but less electricity and fertiliser credits).
- The cost of ethanol production was 57-103 c/L for wheat, and 62-96 c/L for sorghum, depending on the combination of assumptions.
- The amount of power generated and exported is very dependent on the amount of stillage, the type of stillage processing, and the generation technology. For the alternative stillage processing options, the cost of ethanol production is lowest for AD-GTCC, due to its high efficiency and low capital cost (particularly for generation plant over 50 MW).

Production of WDG versus DDGS

An interesting question for the study was the trade-off between selling WDG directly, or drying the WDG to provide DDGS, as an animal feed. Drying would cost around \$37-61/t DDGS depending on energy costs, and, from a cost perspective, WDG can only be transported around 50-70 km before it is economically preferable to produce DDGS.

WDG, with its limited storage life, handling characteristics, significantly lower value, and reliance on local use, is likely to provide a lower co-product credit than the equivalent dried product. Overall, credits will depend on the marketability of the various products for the particular plant location.

4 CONCLUSIONS Impact on feedlot industry

The development of a feed-grain based ethanol production capacity in eastern Australia will present significant challenges for the cattle feedlot industry, as well as for the other intensive livestock industries. It will adversely affect grain supplies, and a review of grain importation procedures to cover low crop yield years will be necessary.

The by-products can be valuable feedstuffs, although there are limits to their use in feedlot diets. The most energetically efficient and environmentally friendly ethanol production uses the distillers grains in an anaerobic digestion process to provide fuel for the plant. In this case no by-product is available for the feedlot industry. If wet distillers grain is available, it is only economic to transport it 50-70 km.

The economics of ethanol production are very dependent on grain price and availability, and there are clearly challenges for ethanol producers which will impact on existing domestic grain consumers (such as feedlots) – oil price volatility, availability of long term contracts for grain (and grain price), and competing uses of the stillage (distillers grain as feed component, or for electricity generation).

Further analysis of these interactions is required, with the impacts of climate change also taken into consideration.

While this study serves as a guide to the probable impact of a grain based ethanol industry on the eastern Australia feedlot industry, it is imperative that, if ethanol production plants are established across Australia, a full assessment of the implications are carried out on a plant by plant basis, under Australian conditions.

The variability of grain production in Australia, likely to increase with climate change, provides a strong driver for location of the ethanol plant adjacent to alternative sources of grain supply, eg imports or transfers from other regions of the country. This favours location at a port, as being planned by Primary Energy for plants at Kwinana, and Brisbane. The biodigestion of the stillage (thereby avoiding production of dry distillers grains) avoids the issue of location in the proximity of markets for the dry distillers grain by-product.

From both the techno-economics, and the Life Cycle Analysis results, it is apparent that biodigestion of the overall stillage has a number of important benefits:

- Reduces the net energy input to the ethanol plant.
- Generates excess electricity, and fertiliser credits, which exceed the credits which are associated with the sale of the dry distillers grains.

A potential consequence for the feedlot industry is that using the distillers grain for fuel within the plant does not produce any distillers grain for sale ; *i.e.* does not provide a feed component to partially replace the feed value of the original grain. However, the impact of diverting the wet distillers grain away from the feedlot industry could be alleviated to some extent if the surplus distillers grain in the US could by imported at cheap price. This is likely to be only a short term solution as the increasing cost of energy supplies is now driving interest in the USA in anaerobic digestion of the stillage, which would be expected to impact on the availability and price of dry distillers grain for Australian import.

Finally, there is some doubt as to the long term availability of grain in Australia for conversion to liquid fuels at an economic price (lack of rainfall, competing uses for grain leading to price increases). There is also the developing technology for conversion of cellulose to ethanol, which is likely to shift the focus to the cheaper source of biomass. As the situation unfolds, and new regulatory environments develop, further techno-economic and LCA studies would be worth consideration.

Further R&D

As grain-based ethanol production does not currently occur in Australia (apart from the Manildra plant at Nowra that uses some grain on occasions), compilation of this report has necessitated extrapolation from overseas data. Once plants are established in Australia, it is suggested that an assessment of the implications be undertaken on a plant by plant and a region by region basis. The areas of investigation should largely be those considered in this report.

Those plants which biodigest stillage to produce biogas and electricity are the most energetically efficient, with the lowest overall greenhouse gas emissions. Under certain conditions (grain and electricity prices), they produce ethanol at the lowest price. There is therefore a real possibility that

there may be limited or no distillers grain for the feedlot industry to use as a substitute for whole grain. Competition for feed grains will increase. This scenario demands that the location of ethanol plants and future feedlots be carefully considered as the dependency on imported grains may become acute. In addition, developments in the USA ethanol industry should be reviewed periodically, to assess the impact on dry distillers grain availability and price for import into Australia.

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1 Background

In recent years, the Australian Federal Government has articulated a commitment to the development of the biofuels industry through the production of biodiesel and ethanol, with attention currently being focussed on expanding Australia's production capacity. This interest is part of increased global activity. Total world production of 46 GL/y is approximately equivalent to 140% of Australia's total petrol consumption, on an energy content basis. Currently Brazil and the USA are the major producers of ethanol, with Australia's total existing production capacity equivalent to one medium sized ethanol plant. Rapid expansion in the world wide production of ethanol has occurred over the past 2 to 3 years as a result of:

- Recent increases in the cost of crude oil and the current high petroleum prices.
- The desire of many countries to reduce dependence on imported fuels and extend existing oil capacity.
- An increasing demand for more renewable fuels.
- Attempts to reduce greenhouse gas emissions.
- An attempt to reduce exhaust emissions from cars and the associated health risks.
- The phasing out of methyl tertiary butyl ether (MTBE) as an oxygenate additive for petrol, coupled with the suitability of ethanol as a substitute for MTBE.
- The existence of government policies in some countries to promote the ethanol industry.

The existing production capacity for ethanol in Australia is ~155 ML/y, although the actual production (2005-2006) was ~105 ML (fuel and industrial use) due to limitations in market demand. Contract commitments for ethanol for blending with petrol are only 21 ML/y.

The Australian Government has introduced a number of measures to encourage ethanol production as part of a broader policy agenda to promote the use of biofuels in Australia. These measures have three main components:

- A commitment that biofuels produced in Australia from renewable resources should contribute at least 350 ML annually to Australia's total fuel supply by June 2010. [It should be noted that this target of 350ML includes both biodiesel and ethanol production.]
- The Biofuels Capital Grants Program [introduced in July 2003 and modified in March 2004] to
 provide one-off capital subsidy for new and/or expanded projects producing biofuels from
 renewable resources or biomass waste products. Grants were limited to a maximum of \$10
 million per project and at its completion, seven projects were offered grants totalling \$37.6
 million a total of \$12.4 million for three ethanol projects and the balance for the four biodiesel projects.

• The Ethanol Production Grants Program which effectively offsets the excise on domestically produced biofuels until 30 June 2011. From 1 July 2011 to 1 July 2015, the excise will be phased in through five equal annual instalments to reach a final rate of 19.1 cents per litre for bio-diesel and 12.5 cents per litre for ethanol. The final rate represents a 50% discount on excise as compared to other fuels with the same energy content. It will apply to imported ethanol as well.

About 10 new plants are in various stages of planning. Their production capacity is projected to be 1265 ML. Currently there is uncertainty surrounding the details of some proposals. Some are progressing slowly and some are stalled. Uncertainties about the cost and supply of feed grains and the sale of ethanol and the by–products are limiting progress. However it is realistic to estimate that across Australia, feed - grain based ethanol production may contribute in the order of 275 to 350 ML annually by 2010.

Currently the Australian cattle feedlot industry uses about 2.5 million tonnes of grain per year with significant increases predicted in future years as the industry expands. Establishment of an ethanol production industry would increase competition, and perhaps price, for feed grains. A by–product of grain–based ethanol production is distillers grain which has the potential to be a partial substitute for whole grain in feedlot diets.

The purpose of this study is to provide information for an Australian context, providing the cattle feedlot industry with current knowledge about the ethanol production processes, grain supply, the by-products produced, and their value for inclusion in feedlot diets. In addition, regions suitable for the production of grain-based ethanol are identified and the effects on the feedlot industry in these and adjacent regions examined, taking into consideration both the competition for grain and/or provision of a by-product feedstuff.

2 **Project Objectives**

The objectives of the project were to:

- Establish the likely grain usage (total and regional) and subsequent production (total and regional) of wet distillers grain given current and proposed development of grain-based ethanol production facilities to meet the existing government annual target of 350 ML ethanol production, assuming 75% of this production will occur from feed grains.
- Extrapolate this data to evaluate the potential situation should the government move to a position of mandating an E10 inclusion policy.
- Provide a technical assessment of the energetic costs and benefits of ethanol production from grain, under Australian crop and ethanol production conditions.
- Determine a realistic feed value of both the wet and dried wet distillers' grain products under Australian conditions and establish a protocol, which accounts for the variability in the base

product because of ethanol extraction efficiency and variable water content, for determining this value.

- Evaluate the likely potential usage of the wet and dried wet distillers' grain products in the feedlot sector, given the location, production quantities, and costs of the wet distillers' grain supply in relation to potential feedlot users and likely ration inclusion levels.
- Recommend any additional R&D necessary to establish the value of wet and dried wet distillers' grain products under Australian conditions.

3 Methodology

The project was undertaken by a consortium of CSIRO Divisions (Livestock Industries, and Energy Technology), and Aquila Agribusiness Pty Limited. Each of these groups produced a separate report. They are in the Appendices. The roles of the three organisations were:

- Aquila Agribusiness Pty Limited investigated the availability of grain in eastern Australia, current plans for feed-grain based ethanol production and the availability and likely use of the distillers grain by-product by the cattle feedlot industry.
- CSIRO Livestock Industries undertook a scientific evaluation of the nutritive value of distillers grains in Australia, and the limits to their inclusion rates in feedlot diets.
- CSIRO Energy Technology prepared an overview of world ethanol developments and used a 160 ML per annum hypothetical ethanol plant in New South Wales to prepare a life cycle analysis which documented the energy use and generation, water balances and greenhouse gas implications. A techno–economic analysis for ethanol production at this plant was also carried out. Both studies considered wheat and sorghum as feedstocks.

During the data gathering phase of the project, an MLA Advisory Committee provided advice on the direction to the investigations so that the outputs were aligned with current industry needs.

Each of the three investigations was a "desk-top" study. Data available publicly and restricted information made available to the researchers were integrated and used in the calculations presented. This source information is provided so data used and assumptions made are open to scrutiny. Methodological details for each section are given in the relevant Appendix.

4 Results and Discussion

The results and discussion for each of the three sections of the report are presented in the Appendices.

Appendix 1 deals with the seasonal supply of grain in eastern Australia, projected usage of feedgrain for ethanol production given likely production targets, and the availability and likely use of the distillers grain by–product by the cattle feedlot industry.

Appendix 2 reports the nutritive value of distillers grains for feedlot cattle, the limits to the inclusion of distillers grains in feedlot diets and the resultant effects on the liveweight gain of cattle.

Appendix 3 uses a 160 ML per annum hypothetical ethanol plant in New South Wales to carry out Life Cycle Analyses which document the energy use and generation, water balances and greenhouse gas implications for various options. A techno–economic analysis for ethanol production at this plant is also reported. Both studies considered wheat and sorghum as feedstocks.

5 Success in Achieving Objectives

All six objectives were met.

The report aligns seasonal grain production with feedlot capacity in Statistical Divisions of importance to the feedlot industry. This is the first time that such defined data have been calculated.

Realistic estimates of Australia's ethanol production over the coming years is provided. These assessments were made from personal contact with project managers of proposed ethanol plants and officials of government departments.

The Life Cycle Analyses and the techno-economics for an example of a 160ML ethanol plant at Gunnadah in New South Wales used data from current operating plants overseas and from plants in Australia that are on the drawing board.

The simulations on the nutritive value of distillers grains, their inclusion rates in feedlot diets and the predictions of cattle liveweight gain used the same computer software as that used in the United States for the same purpose.

6 Impact on Meat and Livestock Industry – now & in five years time

The major effect from the establishment of an ethanol industry will be on the availability and price of feed grains. Experience in the USA is that feed grain prices have increased markedly in response to competition from the grain-based ethanol industry. The magnitude of the effect will be proportional to the volume of domestic ethanol production from grain. The Australian Government plans to stimulate biofuel production to achieve an annual production of 350 ML of ethanol and biodiesel by 2010. If 75% of this is from ethanol, the annual grain demand in 5 years time would be 3.2-4 million tonnes. This additional demand could be met from grain currently exported in years of above average and average eastern Australian grain yields, but not in years of low grain yield. The current regional shortfalls in grain supply that occur in some years would be exacerbated.

Within a region, a 160 ML ethanol plant would supply sufficient distillers grain to be included in the ration of about 80,000 cattle. If distillers grains were available locally at an economic price, any shortfall in grain supply would be partially alleviated. However it is most unlikely that the cost of feed for a feedlot would decrease. Feed costs are approximately 80% of the cost of feedlot operations. An inexpensive supply of distillers grains comprising from 5% to 40% of a ration is unlikely to balance the increase in grain costs for the remainder of the ration.

7 Conclusions and Recommendations

The development of a grain-based ethanol production capacity in eastern Australia will present significant challenges and opportunities for the cattle feedlot industry, as well as for the other intensive livestock industries. It will adversely affect grain supplies, and a review of grain importation procedures to cover low crop yield years will be necessary.

The by-products can be valuable feedstuffs, although there are limits to their inclusion rates in feedlot diets. Ultimately, it will be for individual feedlots to make an assessment of the overall potential benefit of distillers grain by-products on the basis of value and cost-effectiveness according to their individual circumstances.

The economics of ethanol production depend on many more factors than the annual price and availability of grain. Volatility in the oil market, availability of long-term grain contracts, impacts of climate change and the competing usage of stillage (distillers grains v electricity generation) are among the factors influencing investment decisions.

The variability of grain production in Australia, likely to increase with climate change, provides a strong driver for location of ethanol plants adjacent to alternative sources of grain supply, *eg* imports or transfers from other regions of the country. This favours location at a port, as being planned by Primary Energy for plants at Kwinana and Brisbane. The biodigestion of the stillage, thereby avoiding production of distillers grain, avoids the issue of location so there is a market for the by-product.

Developments in the USA ethanol industry should be reviewed periodically, to assess the impact on dry distillers grain availability and price for import into Australia.

Technology and research developments will continue to offer new options for optimising plant flexibility, by-products, yields and overall costs for particular plant locations. Ongoing monitoring of these advances will be useful in ascertaining the likely effects on areas of interest to MLA.

From both the techno-economics, and the Life Cycle Analysis results, it is apparent that biodigestion of the overall stillage has a number of important benefits:

- Reduces the net energy input to the ethanol plant.
- Generates excess electricity, and fertiliser credits, which exceed the credits which are associated with the sale of the distillers grains.

As grain-based ethanol production does not currently occur in Australia (apart from the Manildra plant at Nowra that uses some grain on occasions), compilation of this report has necessitated extrapolation from overseas data. Once plants are established in Australia, it is suggested that an assessment of the implications be undertaken on a plant by plant and a region by region basis. The areas of investigation should largely be those considered in this report.

8 Bibliography

Full source material is given in the Appendices

9 Appendices

- 9.1 Appendix 1 Grain supply, grain demands for ethanol production and use of distillers grains by the feedlot industry
- 9.2 Appendix 2 Nutritive value of distillers grains
- 9.3 Appendix 3 Ethanol production

APPENDIX 1

Grain supply, grain demands for ethanol production and use of distillers' grains by the feedlot industry

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1 Background

1.1 Purpose of study

In recent years, the Australian Federal Government has articulated a commitment to the development of the biofuels industry through the production of biodiesel and ethanol. Attention is currently focused on expanding Australia's capacity to produce biodiesel and ethanol however, it is also critical that the consequences of this new policy on other industries are investigated.

This study raises and discusses issues relating to ethanol production which are relevant to the cattle feedlot industry, particularly the potential impact on grain supplies and the availability of a distiller grain by-product.

The proponents of grain based ethanol production imply the feeding value of the distiller grain by-product introduces significant benefits to the intensive livestock industries. It is suggested that the distiller grain products have a greater feeding value than the original cereal grain, and can be used as a major part of the cattle's diet. These claims are based on experimentation and observations in the United States [US] based on the use of corn as feedstock. Studies show that there is variability between production facilities and fermentation processes throughout the US, that result in differences in chemical compositions of the by-products produced.

The purpose of this study is to provide information for an Australian context, providing the cattle feedlot industry with relevant and current knowledge about the ethanol production processes and by-products. This will enable feedlot participants to make informed decisions about the use of distiller grain in their operations.

In addition, regions suitable for the production of grain-based ethanol are identified and the effects on the feedlot industry in these and adjacent regions examined, taking into consideration both the competition for grain and/or provision of a by-product feedstuff.

2 Objectives

2.1 Study Part B

Aquila Agribusiness Pty Limited will address 1, 2, and 5 of the project objectives as described below.

- 1. Establish the likely grain usage [total and regional] and subsequent production [total and regional] of distiller grains given the current and proposed development of grain based ethanol production facilities to meet the existing Government annual target of 350 ML ethanol production, assuming 75% of this production will occur from feed-grains.
- 2. Extrapolate this data to evaluate the potential situation should the Government move to a position of mandating an E10 inclusion policy.
- 3. Provide a technical assessment of the energetic costs and benefits of ethanol production from grain under Australian crop and ethanol production conditions.
- 4. Determine a realistic feed value of both the wet and dried distiller grain products under Australian conditions and establish a protocol, which accounts for the variability in the base product because of ethanol extraction efficiency and variable water content, for determining this value.
- 5. Evaluate the likely potential usage of the wet and dried distiller grain products in the feedlot sector, given the location, production quantities, and costs of the distiller grain supply in relation to potential feedlot users and likely ration inclusion levels.
- 6. Recommend any additional research and development necessary to establish the value of wet and dried distiller grain products under Australian conditions.

3 Grain and Cattle Feedlot Production

This section provides background information about Australia's grain production, including trend analysis for the last eight years' production in Eastern Australia. In addition, data showing the size and distribution of the cattle feedlot industry are examined.

3.1 Cereal feed-grains – An overview

3.1.1 Cereal grain production in Australia

Australian grain production has been trending upwards since the early 1990's. This trend has been achieved principally through increases in the area sown to grains and increases in crop yields^[1]. For example, Australian grain production in 2004-05 was 34.745 million tonnes, comprising of 22.605 million tonnes of wheat and 12.14 million tonnes of coarse grains [barley, corn, oats, sorghum, and triticale]. Export values totalled \$5.045 billion. By comparison, the production for 2005-06 increased by almost 15% to 39.741 million tonnes, 25.090 million tonnes of wheat and 14.651 million tonnes coarse grains. Projected production for 2010-11 is 42.602 million tonnes, comprising of 27.678 million tonnes and 14.924 million tonnes for wheat and coarse grains respectively^[2].

During the past decade, there has also been a steady increase in the sale of feed-grains on the domestic market, with the increase associated primarily with feeding in the intensive livestock industries. The major intensive livestock industries are the cattle feedlot, dairy, pig and poultry industries. Barley, corn, sorghum, and wheat are the main grains with lesser tonnages of oats and triticale. In parts of Eastern Australia, feed-grains are an increasingly scarce commodity as the demand from the intensive livestock industries outstrips local supply, particularly during dry seasons.

Drought is a common occurrence in Australia and can severely affect grain production and supply^[3]. It is the key contributor to cyclical grain and feedstuff shortages. In recent times, because the severity of droughts has been inconsistent across regions of Australia, there has been a sufficient feed-grains produced to meet the demand. However, it is important to note that both nationally and internationally the livestock industry is growing strongly and will require increased quantities of feed-grains to meet these growth requirements. Hafi and Connell^[4] determined grain use by the major intensive livestock industries in the fiscal year 2003-04 to be 6.880 million tonnes, with the projection in 2007-08 to increase to 8.448 million tonnes. This expansion by the major intensive livestock and industrial users of grain, combined with the high inter-annual variability in seasonal grain growing conditions, has given rise to industry concern about the reliability of grain supply^[5].

In Australia, grain is grown in two relatively narrow inland belts – the Eastern Australian grain belt stretching through Central Queensland, New South Wales, Victoria and South Australia; and the Western Australian grain belt which is bordered by Geraldton in the north, Albany to the south and Esperance to the east^[4].

The intensive livestock industries are concentrated in Eastern Australia, particularly in Queensland and New South Wales, where their future growth will be greatest. It is likely that this expansion will further reduce grain exports from these areas, although these states have also experienced the most acute feed-grain supply shortages in recent times.

Consequently, it is in Eastern Australia where a drought induced domestic feed-grain deficiency will potentially be most severe. For short periods, it would be possible to satisfy part of the increased growth demand for feed-grains with interstate transfers from Western and South Australia, but this will be at great cost in terms of transportation.

In the event of a severe back-to-back continental drought, substantial quantities of feed-grains would need to be imported, if the intensive livestock industries were to maintain production. Under the provisions of the Australian Quarantine and Inspection Service [AQIS), such imported grains must be used principally in metropolitan areas to service poultry and compound stockfeed manufacturers [Meat and Livestock Australia^[3]. The major intensive livestock industries inland from ports are unable to access imported grains.

It is logical that an Eastern Australia feed-grain based ethanol industry will further add to the escalating domestic demand for feed-grains, and as a consequence, will further increase the likelihood of acute seasonal domestic grain shortages.

3.1.2 Cereal grain production in Eastern Australia

The annual fluctuation in Eastern Australia cereal grain production is illustrated in Table 1.1. The fluctuations in the principal grain crops are shown in Table 1.2.

 Table 1.1
 Eastern Australia cereal grain production by states

			• •	-				
	1998	1999	2000	2001	2002	2003	2004	2005
Queensland	2,383,705	3,460,029	3,688,853	2,585,064	2,517,781	1,809,854	2,879,742	2,685,164
New South Wales	7,815,548	8,812,695	10,625,612	10,070,297	10,436,862	3,619,524	10,132,049	10,386,984
Victoria	2,446,371	2,331,902	3,834,957	4,761,983	4,442,434	1,385,902	5,428,569	3,234,374
South Australia	4,714,361	5,359,031	3,993,044	6,481,176	7,555,698	3,511,695	6,181,521	4,600,358
TOTALS	17,359,986	19,963,657	22,142,466	23,898,520	24,952,775	10,326,975	24,621,881	20,906,880
Source: Aust	ralian Bureau	of Statistics ^[6]						

	Queensland	New South Wales	Victoria	South Australia
	Tonnes	Tonnes	Tonnes	Tonnes
Barley				
2005-06 latest ABARE estimate	259,000	2,245,000	2,059,000	2,685,000
Five year average to 2004-05 [a]	175,000	1,345,800	1,476,800	2,344,400
Corn				
2005-06 latest ABARE estimate	183,300	183,808	7,000	
Five year average to 2004-05 [a]	174,400	201,400	6,700	
Oats				
2005-06 latest ABARE estimate	4	492	260	129
Sorghum				
2005-06 latest ABARE estimate	1,170,000	840,000	4,500	
Five year average to 2004-05 [a]	1,158,600	724,800	2,000	
Wheat				
2005-06 latest ABARE estimate	1,385,000	7,921,000	2,705,000	3,578,000
Five year average to 2004-05 [a]	987,800	6,646,400	2,366,600	3,424,600

3.1.3 Eastern Australia regional production 1998 - 2006

Source: ABARE[⁷]

In Table 1.3, the Eastern Australian regional grain production for the fiscal years 1998 - 2006 is tabulated according to the Statistical Divisions defined by the Australian Bureau of Statistics [See Attachments for maps]. The crops included are barley, corn, oats, sorghum, triticale, wheat. The extent of the annual fluctuations across regions and states is evident from the data provided.

Table 1.3	Eastern Australia grain production by Statistical Division 1998 - 2006 [Tonnes]
	Eastern Australia grain production by otatistical Division 1990 2000 [Tonnes]

Chata	Statistical Division		Production for fiscal year ending							
State	Statistical Division	1998	1999	2000	2001	2002	2003	2004	2005	2006
Qld	05 Brisbane	821	608	1,409	614	890	325	523	353	
Qld	10 Moreton	29,862	30,946	33,714	18,734	17,830	13,275	17,083	17,323	15,865
Qld	15 Wide Bay-Burnett	81,896	126,906	139,213	90,464	80,340	84,835	76,618	56,254	54,380
Qld	20 Darling Downs	1,449,205	1,952,037	2,452,082	1,133,891	1,620,926	1,216,239	1,909,044	1,698,752	1,795,200
Qld	25 South West	231,010	429,530	364,308	202,376	300,910	69,918	238,285	435,025	422,750
Qld	30 Fitzroy	393,535	651,424	541,226	752,198	359,330	283,770	448,080	356,649	707,850
Qld	35 Central West	3,025	5,183	4,567	445			905	300	
Qld	40 Mackay	190,593	256,556	139,785	375,013	124,912	110,943	154,397	79,792	272,500
Qld	45 Northern	711	3	622		1,556	200	2,162	11,384	
Qld	50 Far North	17,003	25,874	28,957	17,658	18,184	34,184	39,433	39,144	
Qld	55 North West	425								
	Totals	2,398,086	3,479,068	3,705,882	2,591,392	2,524,878	1,813,690	2,886,530	2,694,976	3,268,545

Continued...

Table	1.3	continued

C4-4-	Statistical Division				Productio	on for fiscal ye	ear ending			
State	Statistical Division –	1998	1999	2000	2001	2002	2003	2004	2005	2006
NSW	05 Sydney	885	4,285	7,618	386	5,636	69	430	131	
NSW	10 Hunter	113,855	162,617	152,259	128,515	129,880	70,091	167,093	186,641	92,980
NSW	15 Illawarra	1,791	1	9,283	1,237	1,056	240	447	480	
NSW	20 Richmond-Tweed	9,580	10,671	6,777	11,870	27,131	15,908	18,882	6,970	
NSW	25 Mid North Coast	8,232	3,679	13,091	4,084	150		1,605	1,260	
NSW	30 Northern	2,355,477	2,131,354	3,241,860	1,928,802	3,051,810	960,514	2,755,108	3,798,156	2,727,650
NSW	35 North Western	1,589,316	1,952,746	2,150,265	1,700,546	1,905,148	492,353	1,959,343	2,048,281	1,770,500
NSW	40 Central West	1,722,975	2,169,408	1,963,844	2,218,830	2,133,619	517,685	1,613,300	1,605,057	2,537,500
NSW	45 South Eastern	248,293	304,499	293,336	333,034	329,884	135,555	267,525	322,061	314,800
NSW	50 Murrumbidgee	1,654,533	2,022,770	2,089,307	2,509,568	2,072,130	1,055,728	2,207,239	1,751,029	1,929,000
NSW	55 Murray	855,608	1,035,805	1,333,043	1,789,066	1,414,842	632,261	2,039,997	1,373,286	1,661,250
NSW	60 Far West	10,084	6,113	21,847	17,219	19,515	7,931	3,668	6,575	
ACT	05 Canberra	1	1	1	1,750	120	1,959	2,080	66	
ACT	10 ACT-Bal	183	176	110	88	95		40	25	
	Totals	8,570,814	9,804,126	11,282,641	10,644,995	11,091,017	3,890,293	11,036,758	11,100,018	11,033,680
Vic	05 Melbourne	5,428	11,426	14,378	18,601	12,356	9,953	13,398	9,929	
Vic	10 Barwon	59,196	68,981	83,981	137,316	122,932	119,994	200,751	210,016	115,900
Vic	15 Western District	128,464	111,459	118,330	169,125	175,360	203,031	244,003	182,259	297,000
Vic	20 Central Highlands	136,113	183,761	246,495	288,531	290,580	229,583	328,188	313,425	255,750
Vic	25 Wimmera	1,195,722	1,156,678	1,582,972	1,858,631	1,894,041	536,423	2,304,387	1,212,533	2,071,000
Vic	30 Mallee	965,022	926,545	1,585,376	2,086,914	1,706,760	364,496	2,029,517	974,675	2,005,630
Vic	35 Loddon	249,261	210,100	342,324	403,358	397,820	83,802	502,459	313,988	379,650
Vic	40 Goulburn	225,385	272,505	335,598	419,638	434,873	163,815	552,670	450,623	386,390
Vic	45 Ovens-Murray	32,240	23,772	46,317	35,980	31,692	16,771	36,815	41,761	33,915
Vic	50 East Gippsland	300	923	7,413	9,206		7,790	17,288	7,095	
Vic	55 Gippsland	633	228	3,047	1,683	1,265	4,878	1,860	2,856	
	Totals	2,997,766	2,966,380	4,366,231	5,428,983	5,067,680	1,740,536	6,231,335	3,719,159	5,545,235
SA	05 Adelaide	9,765	4,011	7,179	3,233	83	6,765	8,913	2,204	
SA	10 Outer Adelaide	243,374	281,305	213,847	299,139	351,941	186,640	295,658	246,873	206,900
SA	15 Yorke & Lower North	1,631,356	1,836,547	1,461,742	2,088,939	2,450,027	1,179,702	1,944,753	1,695,740	1,678,580
SA	20 Murray Lands	745,711	953,142	796,362	1,082,243	1,127,017	351,618	1,103,669	652,806	1,152,700
SA	25 South East	231,862	231,934	206,195	252,715	342,710	252,345	304,764	207,293	282,725
SA	30 Eyre	1,748128	1,787,196	1,029,746	2,133,790	2,518,419	1,287,043	2,225,612	1,441,164	2,152,250
SA	35 Northern	396,555	589,400	464,400	895,487	1,147,264	385,328	589,007	516,863	770,700
	Totals	5,006,751	5,683,536	4,179,470	6,755,546	7,937,462	3,649,440	6,472,375	4,762,944	6,243,855
	TOTALS	18,973,416	21,933,110	23,534,225	25,420,917	26,621,036	11,093,960	26,626,998	22,277,098	26,091,315
Sol	urce: Australian Burea	, ,					, ,			
			-							

The average annual grain production [including barley, corn, oats, sorghum, triticale, wheat] for the period 1998 to 2006 is tabulated by region in Table 1.4. Also shown is the highest [maximum] and the lowest [minimum] regional yields which illustrate the fluctuations primarily due to seasonal conditions.

State	Statistical Division	Grain production yields 1998 - 2006 [Tonnes]				
Otate		Average	Maximum	Minimum		
QLD	05 Brisbane	693	1,409	325		
QLD	10 Moreton	21,626	33,714	13,275		
QLD	15 Wide Bay-Burnett	87,878	139,213	54,380		
QLD	20 Darling Downs	1,691,931	2,452,082	1,133,891		
QLD	25 South West	299,346	435,025	69,918		
QLD	30 Fitzroy	499,340	752,198	283,770		
QLD	35 Central West	2,404	5,183	300		
QLD	40 Mackay	189,388	375,013	79,792		
QLD	45 Northern	2,080	11,384			
QLD	50 Far North	27,555	39,433	17,003		
QLD	55 North West	142	425			
NSW	05 Sydney	2,430	7,618	69		
NSW	10 Hunter	133,770	186,641	70,091		
NSW	15 Illawarra	1,817	9,283	1		
NSW	20 Richmond-Tweed	13,473	27,131	6,777		
NSW	25 Mid North Coast	4,586	13,091	150		
NSW	30 Northern	2,550,081	3,798,156	960,514		
NSW	35 North Western	1,729,833	2,150,265	492,353		
NSW	40 Central West	1,831,358	2,537,500	517,685		
NSW	45 South Eastern	283,221	333,034	135,555		
NSW	50 Murrumbidgee	1,921,256	2,509,568	1,055,728		
NSW	55 Murray	1,348,351	2,039,997	632,261		
NSW	60 Far West	11,619	21,847	3,668		
VIC	05 Melbourne	11,934	18,601	5,428		
VIC	10 Barwon	124,341	210,016	59,196		
VIC	15 Western District	181,003	297,000	111,459		
VIC	20 Central Highlands	252,492	328,188	136,113		
VIC	25 Wimmera	1,534,710	2,304,387	536,423		
VIC	30 Mallee	1,404 993	2,086,914	364,496		
VIC	35 Loddon	320,307	502,459	83,802		
VIC	40 Goulburn	360,166	552,670	163,815		
VIC	45 Ovens-Murray	33,251	46,317	16,771		
VIC	50 East Gippsland	6,252	17,288			
VIC	55 Gippsland	2,056	4,878	228		
SA	05 Adelaide	5,269	9,765	83		
SA	10 Outer Adelaide	258,408	351,941	186,640		
SA	15 Yorke and Lower North	1,774,154	2,450,027	1,179,702		
SA	20 Murray Lands	885,030	1,152,700	351,618		
SA	25 South East	256,949	342,710	206,195		
SA	30 Eyre	1,813,705	2,518,419	1,029,746		
SA	35 Northern	639,445	1,147,264	385,328		

Table 1.4Average annual grain production and the highest [maximum] and lowest [minimum] individual
production yields for Eastern Australia Statistical Divisions 1998 - 2006

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3.2 The cattle feedlot industry in Eastern Australia – An overview

3.2.1 The cattle feedlot industry in Australia

The cattle feedlot industry is a vital component of the integrated Australian beef cattle industry. It is a keystone to the industry's growth and security, as well as that of peripheral agricultural businesses, and contributes significantly to the national economy^{[8].}

The feedlot industry has had a stabilising effect on the national cattle herd by lessening the impact of irregular rainfall, dry conditions and/or drought. In recent times, it has also assisted the national turnoff of cattle at a younger age resulting in increased production and the release of a greater proportion of pastoral resources for breeding and other pursuits. The feedlot industry supports greater slaughter carcass weights of higher valued beef, thus enhancing the industry's overall profitability.

The Australian cattle feedlot industry uses grain to finish cattle, rather than to grow cattle. It delivers to the market's growing expectation, a consistent and assured supply of pre-determined quality beef regardless of seasonal conditions. The feedlot finishing of cattle has facilitated improved beef eating qualities and has encouraged increased consumer spending in both the domestic and export beef markets.

Table 1.5 shows that during the calendar year 2005, 81% of feedlot-finished cattle were fed for less than 130 days, and 57 % for less than 100 days. Of the 19% of cattle fed for more than 130 days, only six per cent were fed for more than 200 days.

Number of days fed	%	%
< 50 days	10	
50-100 days	47	
100-130 days	24	
Total less than 130 days		81
130-200 days	13	
> 200 days	6	
Total more than 130 days		19

Table 1.5 Average number of days fed for feedlot-finished cattle [2005]

3.2.2 Australian feedlot capacity

There have been two recent of feedlot capacity, one by ALFA/MLA on numbers of head and the other by AUSmeat on a Standard Cattle Units (SCU) basis.

As at 30 June 2006, ALFA/MLA recorded the capacity at 1.13 million head, expanding by just over 10% in 12 months and 25% since late 2003. There were over 940,000 head on feed, a seven per cent rise from June 2005. Capacity utilisation was 83%. In terms of Eastern Australia, the feedlot capacity was 1,026,712 head with 901,110 on feed, utilising 88% of capacity [Australian Lot Feeders' Association, personal communication, 2006].

During the fiscal year 2005-06, Australian feedlots marketed a record 2.59 million cattle – up five per cent on the record set the previous year and accounting for 34% of Australia's total adult

cattle slaughter^[10]. In the calendar year 2005, feedlots marketed 34% of Australia's total adult cattle, representing around 40% of all beef produced^[9].

Also at 30 June 2006, the National Feedlot Accreditation Scheme [NFAS] had the capacity at 1,093,650 Standard Cattle Units [SCU] with the distribution by state described in Table 1.6.

Size [SCU]	500 and less	501-1,000	1,001-10,000	10,001-30,000	30,001 plus	Totals
Queensland						
Establishments	317	53	50	11	1	432
Capacity	56,173	47,899	178,635	180,290	50,000	512,997
New South Wales						
Establishments	38	32	23	9	2	104
Capacity	10,329	30,651	83,100	165,000	88,333	377,413
Victoria						
Establishments	3	8	4	2		17
Capacity	1,225	6,100	13,000	40,000		60,325
South Australia						
Establishments	20	11	6			37
Capacity	5,027	8,182	12,345			25,554
Tasmania						
Establishments				1		1
Capacity				16,000		16,000
Western Australia						
Establishments	66	19	25			110
Capacity	23,486	17,075	60,800			101,361
Australia						
Establishments	444	123	108	23	3	701
Capacity	96,240	109,907	347,880	401,290	138,333	1,093,650
Source: Aus-meat NFAS	, personal commu	unication [2006	6]			

Table 1.6	Aus-meat NFAS feedlot capacity [SCU] by size and State
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The regional capacity of Australian feedlots is shown in Table 1.7. It can be seen that 26 feedlots have a capacity exceeding 10,000 SCU, accounting for almost 50% of the national capacity. In Eastern Australia, including Tasmania, these same 26 feedlots account for almost 55% of the NFAS capacity of 992,289 standard cattle units.

Queensland		
Queensianu	05 Brisbane	185
	10 Moreton	9,614
	15 Wide Bay-Burnett	52,665
	20 Darling Downs	331,160
	25 South West	25,804
	30 Fitzroy	62,063
	40 Mackay	10,107
	45 Northern	999
	50 Far North	20,400
		512,997
New South Wales	10 Hunter	2,449
	20 Richmond-Tweed	300
	25 Mid-North Coast	1,000
	30 Northern	157,838
	35 North Western	23,568
	40 Central West	22,428
	45 South Eastern	3,100
	50 Murrumbidgee	133,232
	55 Murray	33,498
		377,413
Victoria	10 Barwon	3,600
	15 Western District	1,900
	25 Wimmera	6,000
	30 Mallee	25,000
	40 Goulburn	1,200
	45 Ovens-Murray	22,220
	55 Gippsland	405
		60,325
South Australia	10 Outer Adelaide	7,690
	15 Yorke and Lower North	3,432
	20 Murray Lands	5,045
	25 South East	1,538
	30 Eyre	500
	35 Northern	7,349
		25,554
Tasmania	15 Northern	16,000
rasmama	13 Northern	16,000
Western Australia	05 Perth	400
	10 South West	26,495
	15 Lower Great Southern	23,786
	20 Upper Great Southern	16,370
	25 Midlands	9,950
	30 South Eastern	13,900
	35 Central	10,460
	55 Central	101,361
		,-••
		Total 1,093,650

 Table 1.7
 Aus-meat NFAS feedlot capacity [SCU] by State and Statistical Division

3.2.3 NFAS capacity and cereal feed-grain production

The cattle feedlot industry is the major user of feed - grains amongst the intensive livestock industries. It is estimated that in 2003 it accounted for 22% to 27% of domestically consumed feed-grains^[3]. A comprehensive study^[4] in 2003 projected that in 2004, the feedlot industry would account for 31% of the grain consumed by the livestock industries, increasing to almost 33% by 2008.

For 2006, the Eastern Australia feedlot grain consumption has been calculated to total 2,509,063
tonnes, distributed between the regions on a pro rata basis as in Table 1.8.

State	Statistical Division	Feedlot feed-grain demand 2006				
			Tonnes			
Qld	05 Brisbane		475			
Qld	10 Moreton		24,708			
Qld	15 Wide Bay-Burnett		135,349			
Qld	20 Darling Downs		851,081			
Qld	25 South West		88,316			
Qld	30 Fitzroy		159,502			
Qld	35 Central West		100,002			
2ld	40 Mackay		25,975			
2ld 2ld	45 Northern		2,568			
Qld	50 Far North					
2ld	55 North West		52, 428			
la	55 NORTH West	T ()	1 0 1 0 1 0 0			
		Total	1,318,402			
ISW	05 Sydney		0.004			
ISW	10 Hunter		6,294			
ISW	15 Illawarra					
ISW	20 Richmond-Tweed		771			
ISW	25 Mid North Coast		2,570			
ISW	30 Northern		405,644			
ISW	35 North Western		60,570			
ISW	40 Central West		57,640			
ISW	45 South Eastern		7,967			
NSW	50 Murrumbidgee		342,406			
NSW	55 Murray		86,090			
ISW	60 Far West					
		Total	969,952			
/ic	05 Melbourne					
/ic	10Barwon		9,252			
/ic	15 Western District		4,883			
/ic	20 Central Highlands					
/ic	25 Wimmera		15,420			
/ic	30 Mallee		64,250			
/ic	35 Loddon		- ,			
/ic	40 Goulburn		3,084			
/ic	45 Ovens-Murray		57,105			
/ic	50 East Gippsland		01,100			
/ic	55 Gippsland		1,041			
		Total	155,035			
SA	05 Adelaide	iotai	100,000			
SA SA	10 Outer Adelaide		19,763			
SA SA	15 Yorke and Lower North		8,820			
SA SA						
	20 Murray Lands		12,966			
SA	25 South East		3,953			
SA	30 Eyre		1,285			
SA	35 Northern		18,887			
		Total	85,674			
		Total	2,509,063			

4 Feed-grain Based Ethanol Production

This section provides an overview of the current capacity to produce ethanol and Federal Government targets for feed-grain based ethanol production in Australia. Detailed analysis of the usage of feed-grains in ethanol production in Eastern Australia is also presented, along with an overview of the process through which the distiller grain by-products are produced.

4.1 Ethanol production in Australia – An overview

4.1.1 Current capacity and production

At present, Australia has a limited ethanol production capacity of approximately 165 million litres [ML] annually, using principally cane juice or molasses and wheat starch waste [Table 1.9].

Company	Location	State	Annual capacity	Feedstock
			ML	
CSR Ethanol	Sarina, Yarraville	Queensland, Victoria	60	Cane molasses
Manildra Group	Bombaderry	New South Wales	75-125	Wheat starch
Rocky Point Distillery	Woongoolba	Queensland	5	Cane molasses
Tarac Technologies	Berri, Nuriootpa, Griffith	South Australia, New South Wales	1	Grape marc
Total existing capacity			141-191	

Table 1.9 Current ethanol capacity [ML] in Australia

Current ethanol production is in the order of 108 to 145 ML annually, which is lower than the available capacity. It is notable that in the fiscal year 2005-06:

- 41 ML was blended with fuel;
- approximately 30 to 35 ML was exported by CSR Ethanol; and
- approximately 50 ML was used in a range of domestic industries.

4.1.2 Government policy - Biofuels assistance

The Australian Government has introduced a number of measures to encourage ethanol production as part of a broader policy agenda to promote the use of biofuels in Australia. These measures have three main components as outlined below.

- A **commitment** that biofuels produced in Australia from renewable resources should contribute at least 350 ML annually to Australia's total fuel supply by June 2010. [It should be noted that this target of 350ML includes biodiesel and ethanol production.]
- The **Biofuels Capital Grants Program** [introduced in July 2003 and modified in March 2004] to provide one-off capital subsidy for new and/or expanded projects producing biofuels from renewable resources or biomass waste products. Grants were limited to a maximum of \$10 million per project and at its completion, seven projects were offered

grants totalling \$37.6 million – a total of \$12.4 million for three ethanol projects and the balance for the four bio-diesel projects.

• The Ethanol Production Grants Program which effectively offsets the excise on domestically produced biofuels until 30 June 2011. From 1 July 2011 to 1 July 2015, the excise will be phased in through five equal annual instalments to reach a final rate of 19.1 cents per litre for bio-diesel and 12.5 cents per litre for ethanol. The final rate represents a 50% discount on excise as compared to other fuels with the same energy content.

Table 1.10 shows the excise transition path for these fuels in terms of the fiscal year 2005.

Unit	July 2003 to July 2010	July 2011	July 2012	July 2013	July 2014	July 2015
c/L	0	3.8	7.6	11.4	15.3	19.1
c/L	<u>0</u>	<u>2.5</u>	<u>5.0</u>	<u>7.5</u>	<u>10.0</u>	<u>12.5</u>
c/L	0	1.7	3.4	5.1	6.8	8.5
c/m ³	0	3.8	7.6	11.4	15.2	19.0
	c/L c/L c/L	Unitto July 2010c/L0c/L <u>0</u> c/L0	Unit to July 2011 2010 July 2011 c/L 0 3.8 c/L <u>0</u> <u>2.5</u> c/L 0 1.7	Unit to July 2010 July 2011 July 2012 c/L 0 3.8 7.6 c/L 0 2.5 5.0 c/L 0 1.7 3.4	Unit to July 2010 July 2011 July 2012 July 2013 c/L 0 3.8 7.6 11.4 c/L 0 2.5 5.0 7.5 c/L 0 1.7 3.4 5.1	Unit to July 2010 July 2011 July 2012 July 2013 July 2014 c/L 0 3.8 7.6 11.4 15.3 c/L 0 2.5 5.0 7.5 10.0 c/L 0 1.7 3.4 5.1 6.8

 Table 1.10
 Excise transition path for fuels entering the excise net

Ethanol imports are subject to a customs duty of 38.143 cents per litre until 30 June 2011. From 1 July 2011, imported ethanol will attract a customs duty equal to the excise applicable to domestic ethanol. As a result, imported ethanol will have open access to the currently protected Australian market. This is likely to result in increased competition for domestic producers as imports from low-cost ethanol producing countries are able to enter Australia. Ethanol imported from countries such as Brazil will be landed excise and duty paid in Australia at a price which is financially marginal or even non-viable for proposed local ethanol producers^[12].

At present, the Federal Government does not support a mandate for the use of ethanol, stating that in the interests of consumer choice, "we are not persuaded to mandate the use of ethanol" [13] [14.]

4.1.3 Government policy – The Biofuels Action Plan

The Federal Government has received action plans from the major oil companies, members of the Independent Petroleum Group, and major retailers. These plans collectively provide achievable annual volumetric milestones and underpin progress towards the Government's target of 350 ML of biofuels [made up of both ethanol and biodiesel] by 2010. These targets are reflected in Table 1.11, the notes to which show the type of feed-grain or sugar utilised by each development.

Ethanol capacity	June 2010			
	ML			
Australian Ethanol Ltd, Swan Hill, Vic ^[a]	100			
Babcock & Brown, Leeton, NSW ^[b]	150			
CSR Ethanol, Sarina, Qld ^[c]	100			
Dalby Bio-Refinery Limited, Dalby, Qld ^[d]	84			
Downs Fuel Farmers Pty Ltd, Dalby, Q ^[e]	160			
Lemon Tree Ethanol Pty Ltd, Millmerran, Qld ^[fd]	76			
Manildra Group, Bombaderry, NSW ^[9]	100			
Primary Energy, Kwinana, WA ^[h]	160			
Primary Energy, Pinkenba, Qld ^[i]	160			
Primary Energy, Gunnedah, NSW 🛙	160			
Rocky Point Distillery, Woongoolba, Qld ^[k]	15			
Total capacity:	1,265			

Table 1.11 Proposed ethanol production capacity [ML] by June 2010

Notes:	[a]	Stage 1 - construction started Aug 2006; - production 2007/8; barley/corn/wheat based
	[b]	MoU with Rockdale Beef; feasibility stage; barley/wheat based
	[c]	Capital grant \$4.16 million; expansion under-way, net of exports; cane molasses based
	[d]	Planning 2008 commissioning; sorghum based
	[e]	Planning Stage 1 for 80ML; commissioning 2008-10; sorghum based
	[f]	Capital grant \$5.85 million approved; sorghum/wheat based
	[g]	Expansion of existing fuel ethanol production; waste wheat starch based
	[ĥ]	MoU with BP Australia for total output; construction to start 2007; wheat based
	[i]	MoU with BP Australia; HoA with GrainCorp; construction planned 2007-08; sorghum based
	[i]	MoU with BP Australia; HoA with GrainCorp; construction planned 2007-08; sorghum/wheat based
	[k]	Capital grant \$2.4 million approved expansion; cane molasses based
Source	Pers	onal communications with proponents [2006]: personal communications with the Department of Industry

Source: Personal communications with proponents [2006]; personal communications with the Department of Industry Tourism and Resources, ACT, [2006]; media releases

The Biofuels Taskforce Report to the Prime Minister dated August 2005 identifies current and proposed biofuel production capacities totalling 1,529.3 ML by the fiscal year 2010. This will consist of 1,005.2 ML of ethanol and 524.1 ML of bio-diesel.

Table 1.11 provides a summary of currently known plant developments and it can be seen that there is a potential ethanol capacity totalling 1,265 ML. It is projected that production will rapidly increase from the base capacity to exceed the target of 350ML as early as 2008 [Prime Minister, Media release, 22 December 2005; I Macfarlane, Daily Telegraph, 20 August 2006¹⁴].

It should be noted that new proposals for ethanol production plants are announced from time to time. There is often vagueness surrounding the detail of these proposals and although some have progressed, others have advanced slowly or have stalled. It would appear that at this stage there are major hurdles to developing 'bankable' projects because of variables associated with the cost and supply of the grain feedstock, as well as the sale returns for ethanol and its by-products. As such, it is difficult to forecast with certainty the size, number and/or location of additional ethanol production plants in Eastern Australia and the analysis undertaken in this study is based on data presented in Table 1.11.

4.2 Feed-grain based ethanol production in Eastern Australia

4.2.1 Ethanol production scenarios

This report has clearly identified a number of factors which will impact upon the growth of Australia's ethanol production capacity, including the importation of ethanol from countries such as Brazil at highly competitive prices and the domestic development/expansion of production capacity from both feed-grains and sugar. Setting aside the issue of imported ethanol, this report will now focus on examining scenarios related to feed-grain based ethanol production in Eastern Australia.

It is realistic to estimate that across Australia, feed-grain based ethanol production may contribute in the order of 275 to 350 ML annually to gasoline supplies by the fiscal year 2010, which equates to approximately 1.5% of the Australian petrol consumption. To produce such quantities, approximately 700,000 to 900,000 tonnes of mixed grain stock would be required. It should be noted that the Kwinana plant in Western Australia is the only one located outside Eastern Australia and it produces 160 ML of ethanol and requires approximately 440,000 tonnes of feed-grain.

Across Australia, the total sales of all petroleum products in the fiscal year 2006 amounted to 48,627.1 ML, of which automotive gasoline was 19,017.7 ML [Table 1.12].

	NSW [a]	Vic	Qld	SA	WA	Tas	NT	Australia
Lead Replacement	0.6	2.1	2.8	6.7	2.7	0.3	0.0	15.2
Premium Unleaded	610.2	420.3	438.1	111.8	196.3	76.9	13.8	1,867.4
Proprietary Brand	471.9	333.3	216.4	45.6	80.9	0.0	0.0	1,148.1
Regular unleaded	4,941.3	4,129.0	3,546.4	1,192.1	1,611.7	387.2	124.1	15,931.8
Ethanol Blended Fuel	7.7	1.3	46.2	0.0	0.0	0.0	0.0	55.2
Totals	6,031.7	4,886.0	4,249.9	1,356.2	1,891.6	464.4	137.9	19,017.7

 Table 1.12
 Sales of automotive gasoline by state marketing area for the fiscal year 2006 [ML]

From the table, it can be seen that Eastern Australia's [Queensland, NSW, Victoria, and South Australia] automotive gasoline sales were 16,523.8 ML.

By way of background, it should be noted that a litre of ethanol has an energy content [mega joules per litre] which is typically 68% that of a litre of gasoline, regardless of the feedstock used to produce the ethanol ^[16]. This obviously means that more ethanol is required to reach the same energy content of gasoline.

This study will examine, in detail, scenarios in which 250 ML, 500 ML, 1,000 ML, 2,500 ML and 5,000 ML of grain based ethanol is produced annually for inclusion in the Eastern Australia automotive gasoline market. Table 1.13 compares these ethanol production scenarios to the equivalent automotive gasoline quantities in terms of energy content and as a proportion of market sales in Eastern Australia. The data show that if the Federal Government were to move towards mandating an E10 inclusion policy, this equates to the production of approximately 2,500 ML of ethanol.

Ethanol production scenario	Automotive gasoline equivalents	Proportion of Eastern Australia Automotive gasoline sales [a]
ML	ML	%
250	170	1.03
500	340	2.06
1,000	680	4.12
2,500	1,700	10.29
5,000	3,400	20.58
lote: [a] Based on figures for East	ern Australia for the fiscal year 2006 – 16,5	523.8 ML

Table 1.13Study ethanol production scenarios and comparable gasoline energy equivalents, relative to
Eastern Australia automotive gasoline sales

4.2.2 Feed-grains, usage and yields in ethanol production

Ethanol producers require a consistent supply of grain at a 'realistic' price. Historically, in North America, corn is the most common substrate for ethanol production due to its abundance and greater yield of ethanol relative to other cereal grains^[17]. Sorghum is used in the southern states with satisfaction^[18]. In Canada wheat is the main fermentation substrate due to its availability, however, barley, rye, and triticale may be used during periods of high wheat prices^[19].

Corn is a minor crop in Eastern Australia and sorghum is limited to the more sub-tropical areas. The typical average composition for feed-grains available for ethanol production in Eastern Australia is presented in Table 1.14. There will be recognised composition variation between and within grain types on the basis of varieties and cultural practice and according to seasonal conditions and soil fertility.

	Unit	Barley	Corn	Sorghum	Wheat
Dry Matter [DM]	%	88.0	88.0	88.0	90.0
Metabolisable Energy	MJ/kg DM	12.5	12.8	12.3	13.3
Net Energy _m	MJ/kg DM	8.5	9.0	8.2	9.4
Net Energyg	MJ/kg DM	5.6	6.0	5.4	6.0
Fat	% DM	2.1	4.3	3.1	2.3
Starch	% DM	60.0	70.0	75.0	65.0
Crude Protein	% DM	12.0	9.0	11.0	14.0
ADF	%DM	7.0	3.0	6.0	4.0
NDF	% DM	20.0	9.0	15.0	12.0
Calcium	% DM	0.06	0.02	0.04	0.05
Phosphorus	% DM	0.35	0.30	0.32	0.43
Sulphur	% DM	0.16	0.12	0.14	0.15

Table 1.14 Eastern Australia feed-grains by typical average composition

Grain based ethanol production processes result in residual by-products, some of which are potential feedstuffs suitable for the livestock industries. Following distillation to extract the ethanol, the spent mash goes to a screen press or centrifuge to separate the maximum amount of liquid. The separated liquid either goes back into the cooking system to be sold as livestock feed, or is partially dehydrated into syrup called condensed distiller soluble [CDS]. The spent

grains can be sold as livestock feed as wet distiller grains [WDG] or dried distiller grains [DDG]. The syrup [CDS] can be added to both the wet distiller grains [WDGS] or dried distiller grains [DDGS].

Table 1.15 presents the likely yield of ethanol, WDGS and DDGS from the base grains available in Eastern Australia, together with the grain demand for each of the ethanol production scenarios and the corresponding by-product [WDGS and DDGS] produced.

Looking at the figures for ethanol production from corn, it can be seen that 654,587 tonnes is required to produce 250ML of ethanol with 603,125 tonnes of WDGS or 201,042 tonnes of DDGS as the by-product. In the Eastern Australian context, it is more likely that wheat, sorghum and barley will be used to produce ethanol and the yield of ethanol production and by-product will vary accordingly.

Table 1.15 Yields of ethanol, WDGS, DDGS and grain demand for study scenarios

			Unit	Barley	Corn	Sorghum	Wheat
Dry Matter [DM]			%	88.0%	88.0%	88.0%	90.0%
Starch [DM] in grain			%	60.0%	70.0%	74.6%	65.3%
Yields per tonne feed-g	jrain ['As i	s']					
Ethanol		[a]	litre	327	382	407.0	364.4
Wet distillers grain [3	0%DM]	[b]	tonne	1.209	0.921	0.789	1.095
Dried distillers grain [90%DM]	[b]	tonne	0.403	0.307	0.263	0.365
Feed-grains ['As is'] co	onsumed t	o produce:					
Ethanol production		1 ML	tonne	3,055	2,618	2,457	2,744
		250 ML	tonne	763,685	654,587	614,224	686,108
	Study scenarios	500 ML	tonne	1,527,370	1,309,175	1,228,448	1,372,216
	stud	1,000 ML	tonne	3,054,741	2,618,349	2,456,896	2,744,433
	S SCe	2,500 ML	tonne	7,636,852	6,545,873	6,142,241	6,861,082
		5,000 ML	tonne	15,273,705	13,091,747	12,284,481	13,722,165
Wet distiller grain with	soluble [3	0%DM] produ	iced				
Ethanol production		1 ML	tonne	3,694	2,413	1,938	3,006
	so	250 ML	tonne	923,438	603,125	484,375	751,563
	nari	500 ML	tonne	1,846,875	1,206,250	968,750	1,503,125
	Study scenarios	1,000 ML	tonne	3,693,750	2,412,500	1,937,500	3,006,250
	брг	2,500 ML	tonne	9,234,375	6,031,250	4,843,750	7,515,625
	Sti	5,000 ML	tonne	18,468,750	12,062,500	9,687,500	15,031,250
Dried distiller grain wit	h soluble	[90%DM] prod	duced				
Ethanol production		1 ML	tonne	1,231	804	646	1,002
	so	250 ML	tonne	307,813	201,042	161,458	250,521
	Study scenarios	500 ML	tonne	615,625	402,083	322,917	501,042
	sce	1,000 ML	tonne	1,231,250	804,167	645,833	1,002,083
	Лрг	2,500 ML	tonne	3,078,125	2,010,417	1,614,583	2,505,208
	Sti	5,000 ML	tonne	6,156,250	4,020,833	3,229,167	5,010,417

Note: [a] Assume yield of 620 litres/tonne starch

5 Research on the Use of Ethanol Production By-products in the Feedlot Industry

This section provides a summary of the research to date regarding the use of by-products from ethanol production in the feedlot industry. It is important to note that almost all studies have been undertaken in North America and the relevance of findings to the Australian feedlot industry will need to be verified when Australian plants are operational. The section concludes with a SWOT analysis of the potential value of ethanol production by-products to the cattle feedlot industry.

5.1 Feed-grain based ethanol production by-products

5.1.1 Principal feedstuffs

The principal by-products are wet distiller grain [WDG], dried distiller grain [DDG] and condensed distiller soluble [CDS]. The soluble may be dried and added to the WDG to produce wet distiller grains with soluble [WDGS] or added to the DDG to produce dried distiller grains with soluble [DDGS].

North American experience highlights the significant variability in product quantities and compositions associated with differences in distilling plants and distilling processes. The more recent advances in engineering and technology enable newly established plants to achieve greater efficiencies. Procedures have been modified to influence by-product nutrient composition. The by-product composition, as with many by-product feeds, is also influenced by multiple variables such as the type and variety of grain, agricultural practices on - farm, seasonal conditions and soil fertility^[24; 25].

The DDGS composition is not standardised in North America^[26]. In contrast with many feedstuffs, there is no grading system to differentiate quality and value among DDGS sources and there is no grading system to differentiate quality within ethanol by-product categories. The standardisation of DDGS composition and the introduction of a grading system have been opposed by many in the US ethanol industry.

This study assumes that the distiller grains will contain some soluble but this can vary from plant to plant. Clearly, an assessment of by-product quality for a plant yet to be built in Australia can only be viewed as suggestive, being based on information gained from experience overseas.

5.1.2 Distiller grain nutrient values

Distiller grain by-products clearly offer a potential feedstuff to livestock feeding industries. Suitably priced WDGS and DDGS may be a useful source of nutrient energy, protein and minerals for feedlot cattle. Individual feedlot operators will need to assess by-product nutrient values, respective costs, optimum feeding levels and the economic value to their business when the by-product is sourced.

As a starting point, this study offers a comparison of the nutrient value of the cereal grains which are currently processed by dry-rolling or steam-flaking for consumption by feedlot cattle, to that of the distiller grain by-products. The typical nutrient composition for the WDGS, steam-flaked and dry-rolled form of each grain is given as a guide in Table 1.16.

		Barley			Corn			Sorghum			Wheat		
	Unit	Barley grain dry rolled [a] [b]	Barley grain steam flaked [[a] [b]	Barley WDGS [a] [b]	Corn grain dry rolled [a] [b]	Corn grain steam flaked [a] [b]	Corn WDGS [a] [b]	Sorghum grain dry rolled [a] [b]	Sorghum grain steam flaked [a] [b]	Sorghum WDGS [a] [b] [c] [d]	Wheat grain dry rolled [a] [b]	Wheat grain steam flaked \ [a] [b]	Wheat WDGS [e] [f]
Dry matter [DM]	% AF	88.0	82.0	30.0	88.0	82.0	30.0	88.0	82.0	30.0	90.0	82.0	30.0
Metabolisable Energy	MJ/kg DM	12.5	13.9	10.9	12.8	13.8	14.9	12.3	13.3	13.0	13.3	13.9	n.a.
Net Energy _m	MJ/kg DM	8.5	9.2	7.6	9.0	9.6	10.4	8.2	9.2	8.6	9.0	9.4	n.a.
Net Energyg	MJ/kg DM	5.6	6.5	4.9	6.0	6.5	6.9	5.4	6.3	5.7	6.0	6.4	n.a.
Fat	% DM	2.1	2.1	3.7	4.3	4.1	11.0	3.1	3.1	11.0	2.3	2.3	3.2
Crude protein	% DM	12.0	12.0	30.0	9.0	9.0	30.0	11.0	11.0	31.0	14.0	14.0	40.0
ADF	% DM	7.0	7.0	22.0	3.0	3.0	15.0	6.0	6.0	19.0	4.0	4.0	n.a.
NDF	% DM	20.0	20.0	45.0	9.0	9.0	39.0	15.0	15.0	47.0	12.0	12.0	29.2
Calcium	% DM	0.06	0.06	0.15	0.02	0.02	0.20	0.04	0.04	0.06	0.05	0.05	n.a.
Phosphorus	% DM	0.35	0.35	0.67	0.30	0.30	0.80	0.32	0.32	0.94	0.43	0.43	n.a.

Comparison of typical average wet distiller grain with soluble [WDGS], dry rolled and steam flaked grains Table 1.16

Notes:

[a] After Preston ^[22]
[b] After NRC ^[21]
[c] Adapted from Lodge *et al.*. ^[18]
[d] Kansas Grain Sorghum Producers Association^[27]
[e] After Akayezu *et al.*. ^[28]
[f] Adapted from Nyachotic *et al.*. ^[29]

It has been noted recently^[30] that in 1996 the National Research Council estimated the metabolisable energy for steam-flaked corn and sorghum at 5.6% and 15.6% higher than dry-rolled grain respectively, although a more recent review^[31] found that the metabolisable energy for steam-flaked barley, corn, sorghum and wheat was higher than that for dry-rolled grain by 0%, 15.5%, 21.0%, and 13.6% respectively [based on 605 comparisons]. This suggests that for corn, sorghum and wheat based distiller grain the steam-flaked equivalent grain type offers more energy.

Tabulated values for WDGS are provided only as a guide and it must be stressed that the byproducts require a full assessment upon the establishment of individual plants.

5.1.3 Fresh [WDGS] and dried [DDGS] distiller grain by-product

Distiller grain in the fresh form [WDGS] has a dry matter content of approximately 30%; in the dried form [DDGS] it has a dry matter content of approximately 90%. The drying process is expensive and results in a small loss of nutrient energy of approximately 3% to 6%. WDGS can deteriorate rapidly when exposed to air.

The cost and ease of commodity shipping, storage, handling, milling and delivery to animal all influence feedstuff nutrient evaluations and financial worth. Comparative appraisals adjust for the relative dry matter content. Feedstuffs with low dry matter, such as silage, may be valuable feedstuffs when sourced from a site adjacent to the feedlot but rapidly become financially less attractive once further cartage is required.

WDGS has a low dry matter content which means that handling is difficult and its feedstuff value is noticeably reduced as the distance increases between the ethanol plant and feedlot. The extra bulk incurs extra handling at each stage from ethanol plant to animal. As dry matter costs increase, the optimum inclusion rate will decline and consequently, the value of WDGS needs to be appropriately discounted to compensate for the disadvantages associated with its low DM.

Additionally, the shelf life of WDGS is restricted to approximately four days before spoilage in warm weather. Mould usually occurs upon storage, potentially adversely affecting palatability to livestock. It is possible to extend shelf life by adding preservatives during processing and/or ensiling but these incur additional costs.

In the dry form, DDGS offers enhanced ease in commodity shipping, storage, handling, milling and delivery to animal. However, these benefits to the feedlot as a result of drying, incur increased plant production costs which may or may not be able to be absorbed in the market place. Consequently, drying is frequently discouraged and the distiller grain is more commonly fed as WDGS to ruminants when transport distances are minimal.

In summary, the decision to use either WDGS or DDGS in the feedlot cattle's diet should be principally based on an analysis of its cost as a source of protein and energy relative to those from alternative available feedstuffs within sound nutritional practices.

5.1.4 WDGS and DDGS in feedlot diets

In North America, distiller grains are used widely in feedlot rations, primarily corn and to a limited extent, sorghum grain. The feedstuff is fed fresh as WDGS [approximately 30% dry matter [DM], or dried as DDGS [approximately 90% DM]. Typical inclusion rates range from 5% to 25% [DM] depending on sound ration management and the full cost appreciation of the range of feedstuffs available.

In feedlot diets, fresh corn WDGS and DDGS are palatable and readily consumed by cattle. The moisture in fresh WDGS has the ability to assist the conditioning of dry rations. For corn and sorghum, there is an approximate three-fold concentration of protein, fat and minerals in WDGS as compared to the whole grain. The increased fat proportion contributes to the nutrient energy, compensating for the extracted starch, and digestible fibre maintains high digestible energy.

WDGS and DDGS provide an alternative energy and protein source to grain – approximately 50% is the un-degraded intake protein [UIP] or 'by-pass protein' and approximately 50% the degraded intake protein [DIP]. The nutrient values for both WDGS and DDGS are similar on the basis of dry matter, although energy values are usually lower in the DDGS as a result of fat loss from high temperatures applied during the drying process. Distiller grains dried at higher temperatures are also less digestible^[32].

In the US, much of the research on distiller grains as an energy source has focused on finishing cattle fed dry-rolled corn or dry-rolled corn/high-moisture corn combinations. Results suggest that feeding corn WDGS results in better performance than DDGS^[33], primarily due to the higher energy content.

Erickson *et al.*, [2006] reviewed a number of studies on WDGS in ruminant diets and found that the replacement of corn grain with WDGS consistently improved feed efficiency. For example, WDGS contained 120% to 150% the energy value of dry-rolled corn in beef finishing diets and by comparison, DDGS was found to have 120% to 127% the energy value of dry-rolled corn in high roughage rations. When using WDGS, with its starch largely extracted, there was an associated decline in acidosis. It is likely that acidosis control produces the higher apparent energy values and this is one of the major advantages of using distiller grains in the feedlot industry. In addition, studies have found that it is possible to minimise roughages in diets containing distiller grains relative to inclusion rates^[34] and this is significant in terms of finishing rations.

Another advantage of the high un-degraded intake protein value of distiller grain is that it provides a valuable protein source for young, growing cattle and lactating cows. Drying distiller by-products reduces their net energy value but does not seem to affect their protein value^[33; 25].

Specific studies on diet inclusion rates

In general, the US research suggests there are two nutritional philosophies regarding the use of distiller grain in feedlot finishing diets. Distiller grains may be fed at five to 15% of the diet dry matter to serve as a source of supplemental protein. Alternatively, if fed at higher levels [>15% diet DM], the primary role of distiller grain is to provide an alternative source of energy to the ration grain^[35].

It is common for WDGS to be fed at higher levels than DDGS [on a DM basis] to supply both protein and energy to the animal. This is because WDGS rations delivered at the bunk are cheaper than DDGS given that costs associated with drying are reduced or eliminated in the wet by-product. On the other hand, the transportation costs of WDGS are higher as a consequence of its water content and the feedlot must also consider its disadvantages such as a limited shelf-life and difficulties associated with storage, handling and volume.

Given that drying reduces its net energy value, DDGS is routinely fed as a supplemental protein source, priced relative to other supplemental protein sources. Trenkle³⁶ showed that WDGS and DDGS can be fed to growing and finishing Holstein steers at 10% or 20% [on a DM basis] without affecting performance or carcass value in the market. Calves fed 40% WDGS consumed less fed and had slower gains in weight whereas steers fed 10% WDGS consumed less feed with the same weight gain and improved efficiency.

As Table 1.16 showed previously, it is important to consider the processing [e.g. dry-rolled, steamflaked] of the ration grain when evaluating distiller grains as a diet component substitute. Gordon *et al.*.^[37] experimented to determine the optimal level of DDGS in heifer finishing diets based on steamflaked corn. The study compared diets containing six levels of DDGS [0%, 15%, 30%, 45%, 60%, and 75%] and found that an inclusion rate of 15% was optimal. DDGS affected average daily gain, final weight and hot carcass weight, all of which increased with 15% DDGS but decreased as additional DDGS was added. Heifers on diets containing 15% DDGS finished at a heavier final and hot carcass weight, gained more weight per day, were more efficient and had a higher percentage of cattle graded as 'prime'. It is interesting to note that the growth of heifers fed 30% DDGS was similar to those fed 0% and that the inclusion of more than 45% DDGS in the diet tended to reduce performance and carcass grade.

Similarly, in an experiment to determine the optimum use of sorghum WDGS in steam-flaked corn finishing diets, it was Daubert *et al.*^[38] found that an inclusion rate of 15% was optimal and concluded that the replacement of steam-flaked corn with sorghum based WDGS was a viable option for improving dry matter intake, average daily gain and feed efficiency. WDGS was added at proportions as high as 24% without compromising performance during the last two months before slaughter.

Vander Pol *et al.*.^[39] evaluated six levels of dietary inclusion of corn WDGS [0%, 10%, 20%, 30%, 40%, 50% DM] in terms of feedlot performance and carcass characteristics of yearling steers. The study also compared the energy value of corn WDGS relative to dry-rolled corn. For inclusion rates of 0% to 50%, final body weight, dry matter intake and average daily gain increased quadraticly and feed to gain decreased quadraticly. The energy value of corn WDGS relative to dry-rolled corn was above 100% for all inclusion levels, decreasing from 178% to 121% as dietary corn WDGS inclusion increased from 10% to 50% of dry matter. It was concluded that corn WDGS can be used effectively in finishing diets with optimum feed conversion observed at 30% to 40% dietary inclusion.

Specific studies on the type of distiller grain

Studies comparing corn versus sorghum based distiller grain have found generally similar production efficiencies in cattle diets. For example, when comparing sorghum and corn based WDGS by-products at 30% of diet DM, Lodge *et al.*.^[18] found the sorghum based by-product to have a lower energy value although statistically, the by-products had similar feeding values. The sorghum based product was equal or slightly higher in net energy for gain as compared with dry-rolled corn grain.

Similarly, in a comparison of feeding sorghum and corn based distiller grains in both beef finishing and dairy lactation experiments, Al-Suwaiegh *et al.*.^[40] recorded the average daily gain and efficiency of gain to be alike. Hot carcass weights, fat thickness and yields were greater for steers fed distiller

grains than for controls. Corn and sorghum distiller grains resulted in relatively similar performances when fed to beef or dairy cattle.

There is little relevant data relating to the nutrition value of wheat, and barley based distiller grain for ruminants. On the basis of experiments conducted in Canada,^[29] it was concluded that wheat based DDGS could be effectively used in pig diets as a high level source of nutrient energy, protein, amino acids and non-phytate phosphorus. Other results of Mustafa *et al.*.^[19] indicated barley based distiller grain was characterised by low protein and high fibre contents although the fibre was less degradable than that from wheat based distiller grain.

To date, there is an inadequate amount of creditable research or experience to judge the value of wheat distiller grain in Australia. The data that is available [Refer to Table 5.1.2.1] suggests wheat based distiller grain would have less nutrient energy than the corn or sorghum based by-product as it contains less fat, but on the other hand, would have a higher crude protein value. Again based on the figures, it is expected that barley based by-products would have less nutrient energy than those derived from wheat.

5.1.5 Distiller grain and meat quality

Studies show that corn based distiller grain has no an adverse affect on meat quality when included at customary rates in finishing diets. Roeber *et al.*^[41] concluded that feeding corn based dried distiller grain at up to 50% of dietary dry matter in finishing rations did not affect the tenderness or sensory traits of the meat and was therefore a viable feed alternative. However, the study found that at higher levels, corn based dried distiller grain may have a negative effect on colour stability during retail display, and at low to moderate inclusion rates [10%-25% DM], may enhance retail shelf life without affecting cooked beef palatability.

Evaluating the effect of distiller grain at varying diet inclusion levels, Gordon^[42] concluded that the effects on meat sensory traits and display colour stability were too small to warrant the feeding of DDGS to improve these traits. Gordon *et al.*.^[37] found the percentage of carcasses graded as 'choice' or 'prime' tended to be lower for heifers fed 60% or 70% DDGS as compared to heifers fed 0%, 15%, 30% and 45% DDGS in their diet.

5.1.6 Additional considerations

Sulphur and phosphorous levels in distiller grains are relatively high, having been concentrated in the residual after the starch removal.

Sulphur in excess of 0.4% of distiller grain DM may cause an excess sulphur level in the diet. If distiller grain is used when there are high sulphur levels in drinking water or other dietary feed products, dietary sulphur content could exceed the recommended maximum tolerable dietary levels from all sources ^[21]. High dietary sulphur can interfere with copper absorption and Cmetabolism, an antagonism made worse in the presence of molybdenum. Sulphur excess can be managed via monitoring and ration adjustment.

Distiller grain by-products also have a high phosphorus content. This may necessitate the correction of ill-matched dietary calcium:phosphorus ratio with calcium supplementation. Additionally, a resultant high phosphorous content in feedlot waste necessitates the close monitoring of waste management programs and potentially has an adverse affect on costs associated with manure

management. Evaluation of the cost of managing feedlot manure high in phosphorus suggests that the cost of handling additional manure generated by feeding by-products such as WDGS is between US\$0.75 to US\$1.00 per head for inclusion rates of 0% to 30% and 40% respectively.^[43;44,45]

Another consideration is that diet nutrient excesses such as crude protein can reduce the efficiency of energy utilisation. Excess nitrogen is metabolised and excreted as urea and so requires energy. This can contribute to excessive body heat which is a potential concern under hot conditions^[46]. Furthermore, excess dietary nitrogen excreted to the pen surface can create additional discomforting ammonia release under certain surface conditions and may necessitate additional monitoring and care in waste management. Having said this, in a trial incorporating an assessment of odour emissions, Benson^{[47}] was unable to detect any odour characteristics attributable to the DDGS feed finishing steers at varying inclusion rates to 35% DM.

The possible effects of increased levels of contaminants such as chemical weedicide and pesticides, moulds or ergots concentrated in the distiller grain residual is largely unknown. Whilst these may be considered faint possibilities at this stage, it will be necessary to examine the distiller grain for such contaminants once production units are established.

5.2 SWOT assessment

The following SWOT assessment has been undertaken to summarise the key findings of the research on the use of ethanol production by-products in the Australian feedlot industry. This analysis will assist the industry in understanding and assessing the comparative appeal of WDGS and DDGS by-products.

Strengths of ethanol production by-products

- The increased availability of a high quality ruminant feedstuff with high energy, protein and phosphorus values [based on DM], and highly digestible fibre when using corn and sorghum.
- There is substantial North American research on corn and sorghum WDGS and DDGS in finishing rations to suggest that by-products can be substituted in cattle diets at optimal inclusion rates of between 5% and 25%.
- Fresh corn and sorghum WDGS and DDGS are palatable and readily consumed by cattle. The moisture in WDGS may assist in the conditioning of dry rations.
- A decrease in acidosis in high concentrate rations, relative to the inclusion rate, has been observed.
- In dried form, DDGS is able to be more efficiently transported, stored, handled and processed, and has an extended shelf-life.
- WDGS and DDGS are available around the year and further grain processing is unnecessary.
- Experiments and observations reported indicate there is nil adverse effect on meat quality.

Weaknesses of ethanol production by-products

• In the low dry matter WDGS, the high moisture adversely affects shipping, handling, storage and feeding costs and also limits shelf life, thus reducing its value as a feedstuff.

- The production process for drying distiller grain is energy intensive and expensive, and also reduces the nutrient energy content of the feedstuff.
- The absence of a standardised, descriptive grading system for ongoing composition, quality, and potential contaminant status creates risks and effectively reduces the value of ethanol production by-products as a feedstuff.
- Research suggests that the maximum desirable ration inclusion rate for corn and sorghum based distiller grain is approximately 25% to 30% of dry matter meaning that feedlots remain dependant on alternative high nutrient energy sources.
- There is limited data about the impact of feeding wheat or barley based WDGS and DDGS in the feedlot industry.
- Wheat based distiller grain is assessed to have less nutrient energy than corn or sorghum based by-products as a result of a lower fat content. The barley based by-product has less energy again.
- Both the wheat and barley based by-products have higher protein levels, thus increasing the risk of animal overheating.
- Product composition and quality fluctuates between plants and is subject to multiple variables affecting the feedstock grain.
- The tabulated feeding values can only be used as a guide and the final products will require further testing when a plant is established in Eastern Australia.
- The relative high fat content of distiller grains may affect maximum dietary inclusion rates.
- Diet content must be closely monitored given the high phosphorous and sulphur levels.
- High phosphorous and diet crude protein excess may cause undesirable environmental impacts on loss of ammonia from manure and use of cattle manure as a fertiliser.

Opportunities associated with the use of ethanol production by-products

- WDGS and DDGS are a potential alternative source of ruminant nutrient energy and protein.
- The evaluation of by-products when produced in Australia on a plant to plant basis will lead to the determination of the optimum, cost effective product use.
- WDGS and DDGS may be used by feedlots as a means of controlling acidosis and reducing roughage levels in finishing diets.
- There is an opportunity for savings to the feedlot industry if the WDGS shelf life can be extended without significantly increasing the by-product costs.
- Some studies suggest that at low to moderate inclusion rates, corn based distiller grain may enhance retail meat shelf life without affecting cooked beef palatability.

Threats associated with the use of ethanol by-products

- The grain based ethanol industry will compete with the intensive livestock industries for grain, increasing the overall nutrient energy costs.
- There will be a net loss of high nutrient energy feedstuffs available to the intensive livestock industries.

- The actual nutrient value of the ethanol production by-products will not be fully known until individual plants are in operation and are thoroughly tested.
- Feedlots must factor in higher costs associated monitoring high phosphorus and sulphur levels at upper ration inclusion rates, animal body heat, ammonia levels, and the feedlot's waste management processes.

6 Potential Usage for WDGS and DDGS in the Eastern Australian Feedlot Industry

This section considers the factors affecting the usage of distiller grain by-products across in the Eastern Australian feedlot industry. It also examines in detail the potential impact of ethanol production on grain availability in Eastern Australia with particular reference to meeting the Federal Government's targets for biofuels and ethanol production [approximately 250ML under the current policy and 2,500 ML if an E10 inclusion policy was mandated].

6.1 Factors influencing usage

6.1.1 Availability

The potential WDGS or DDGS availability has been assessed for each of the study scenarios level of ethanol production [Table 1.17].

Ethanol production		Representative 2006 Eastern Australia gasoline sale	Barley	Corn	Sorghum	Wheat
		%	Tonnes	Tonnes	Tonnes	Tonnes
1. WDGS	[30% DM]					
<i>(</i> 0	1 ML		3,694	2,413	1,938	3,006
arios	250 ML	1.03	923,500	603,250	484,500	751,500
cena	500 ML	2.06	1,847,000	1,206,500	969,000	1,503,000
y sc	1,000 ML	4.12	3,694,000	2,413,000	1,938,000	3,006,000
Study scenarios	2,500 ML	10.29	9,235,000	6,032,500	4,845,000	7,515,000
о	5,000 ML	20.58	18,470,000	12,065,000	9,690,000	15,030,000
2. DDGS	[90%DM]					
<i>(</i>)	1 ML		1,231	804	646	1,002
arios	250 ML	1.03	307,833	201,083	161,500	250,500
ene	500 ML	2.06	615,667	402,167	323,000	501,000
y sc	1,000 ML	4.12	1,231,333	804,333	646,000	1,002,000
Study scenarios	2,500 ML	10.29	3,078,333	2,010,833	1,615,000	2,505,000
S	5,000 ML	20.58	6,156,667	4,021,667	3,230,000	5,010,000

Table 1.17 WDGS and DDGS produced relative to ethanol production and gasoline sales

6.1.2 Cost and nutrient value evaluation

Sorghum and wheat will be the predominant base grains in an Eastern Australia grain based ethanol industry. The nutrient value of these distiller grains can be determined via a number of methodologies, dependant on the purpose for which it is utilised. The cattle feedlot industry will have to rely on the guidance provided by the US research (as discussed in the previous section) but the industry is likely to value the product firstly as an energy source feedstuff replacing grain in rations, and secondly, as an organic-based protein source.

Sorghum WDGS and DDGS are evaluated as a source of nutrient energy and crude protein relative to typical dry-rolled feed grains and protein meals in Tables 1.18 and 1.19.

Table 1.18 illustrates the calculated value of sorghum distiller grain relative to dry-rolled grains and whole white cotton seed on nutrient energy [ME] basis alone. For example, sorghum WDGS has 106% and 36% of the relative ME value of dry-rolled sorghum on a DM and 'as is' basis respectively. Similarly, sorghum DDGS has 99% and 102% of the relative ME value respectively. Furthermore, if the DDGS and dry-rolled grain have similar DM [say 90%], the relative values are both 99%.

				Compara	tive ME Value o	f Sorghum Dis	stiller Grain
Grain	DM	N	IE	WDGS		DDGS	
		[a]		[30% DI	A product]	[90% DI	M product]
		DM	'As is'	DM	'As is'	DM	'As is'
	%	MJ/kg	MJ/kg	%	%	%	%
				[c]	[d]	[c]	[d]
Barley	88	12.5	11.0	104	35	98	100
Corn	88	12.8	11.3	102	35	95	98
Sorghum	88	12.3	10.8	106	36	99	102
Wheat	90	13.3	12.0	98	33	92	92
White cotton seed	92	14.5	13.3	90	29	84	82
Sorghum WDGS	30	13.0	3.9			94	282
Sorghum DDGS [b]	90	12.2	11.0	106	35		
Note: [a] [b] [c] [d]	Assuming Compare	ry-rolled proces 3 6% nutrient er s like with like, s like with like,	nergy loss in dr <u>y</u> DM with DM				

Table 1.18	Calculated value of sorghum WDGS and DDGS relative to other typical dry-rolled feed grains and
	whole white cotton seed on metabolisable energy [ME] basis alone

On the next page, Table 1.19 illustrates the calculated value of the sorghum based distiller grain relative to protein meals on the basis of crude protein alone. For example, sorghum WDGS has 82% and 27% of the relative crude protein value of canola meal on a DM basis and 'as is' basis respectively. Similarly, sorghum DDGS has 82% and 82% the relative crude protein value respectively.

Crude DM % 38.0 21.0 44.0 35.0	Protein 'As is' % 34.2 18.9 39.6 24.5		DGS // product] 'As is' % [b] 27 49 23	[90% DM DM [a] 82 148	DGS // product] 'As is' % [b] 82 148
% 38.0 21.0 44.0	% 34.2 18.9 39.6	DM % [a] 82 148	'As is' % [b] 27 49	DM % [a] 82 148	* As is % [b] 82
% 38.0 21.0 44.0	% 34.2 18.9 39.6	% [a] 82 148	% [b] 27 49	% [a] 82 148	% [b] 82
38.0 21.0 44.0	34.2 18.9 39.6	[a] 82 148	[b] 27 49	[a] 82 148	[b] 82
21.0 44.0	18.9 39.6	82 148	27 49	82 148	82
21.0 44.0	18.9 39.6	148	49	148	-
44.0	39.6	-	-	-	148
-		70	23		
35.0	- · -		20	70	70
	31.5	89	30	89	89
31.0	27.9	100	33	100	100
16.5	14.9	188	63	188	188
42.0	37.8	74	25	74	74
50.0	45.0	62	21	62	62
42.0	37.8	74	25	74	74
23.0	21.2	135	44	135	132
31.0	9.3			100	300
31.0	27.9	100	33		
	16.5 42.0 50.0 42.0 23.0 31.0 31.0 res like with like,	16.5 14.9 42.0 37.8 50.0 45.0 42.0 37.8 23.0 21.2 31.0 9.3 31.0 27.9	16.514.918842.037.87450.045.06242.037.87423.021.213531.09.331.027.9100	16.5 14.9 188 63 42.0 37.8 74 25 50.0 45.0 62 21 42.0 37.8 74 25 23.0 21.2 135 44 31.0 9.3 31.0 27.9 100 33 res like with like, DM with DM	16.5 14.9 188 63 188 42.0 37.8 74 25 74 50.0 45.0 62 21 62 42.0 37.8 74 25 74 23.0 21.2 135 44 135 31.0 9.3 100 33 res like with like, DM with DM

Table 1.19 Calculated value of sorghum WDGS and DDGS relative to typical protein meals and whole white cotton seed on crude protein basis alone

Ultimately, the product's nutrient value [metabolisable energy, protein, mineral, vitamin and possible specialised qualities] and cost can only be determined in the process of applying sound ration formulation principles to optimise the return on funds employed on an individual feedlot basis.

6.1.3 Industry capacity to utilise distiller grain

The following tables provide an analysis of the Australian feedlot industry's capacity to utlise distiller grain based on a range of inclusion rates [0% to 25% DM] as well as varying capacity take-up rates across the industry [25%, 50%, 75%, 100%]. It has been also reported that the feedlot industry's consumption of grain is increasing – 3.8 million tonnes of total feedstuffs in 2005-06 [adapted from Hafi and Connell^[4]; ^[10]; Aus-meat NFAS, personal communication, 2006]. Thus, the following table presents figures for a total industry consumption of 3, 4, 5, and 6 million tonnes.

Table 1.20 presents the calculated usage of distiller grain using sorghum based WDGS. The calculation adjusts for individual commodity feedstuff and diet DM as the inclusion proportions vary. The table demonstrates, for example, that when the feedlot industry consumes in total 4,000,000 tonnes ['as is'] of feedstuffs and that 25% of industry capacity utilises WDGS at a diet inclusion rate of 15% of DM, the potential industry demand is approximately 383,750 tonnes of WDGS 'as is' [30% DM]. It is significant to note that this represents about 80% of the by-product of a sorghum based industry which produces 250 ML annually but only just over eight per cent of the by-product if the industry produces 2,500 ML annually [Refer to Table 1.17].

In the unlikely scenario of 100% of industry capacity utilising WDGS at a diet inclusion rate of 15% [DM], the potential industry demand rises to 1,535,000 tonnes. This equates to approximately 30% of potential distiller grain production from a 2,500 ML sorghum based ethanol industry.

It should be noted that if various grains, including wheat and barley, are used for ethanol production, the likelihood of grain shortages based on feedlot industry demand is considerably reduced.

Inc	siusion rates						
Eastern Australia feedlot Diet inclusion industry rate [DM]							
			Tonnes	Tonnes	Tonnes	Tonnes	
Total feedstuffs consumed annually 'as is'			<u>3,000,000</u>	<u>4,000,000</u>	<u>5,000,000</u>	<u>6,000,000</u>	
	25%	0%					
		5%	102,813	137,083	171,354	205,62	
		10%	198,750	265,000	331,250	397,50	
		15%	287,813	383,750	479,688	575,62	
<u> </u>		20%	370,000	493,333	616,667	740,00	
gra		25%	445,313	593,750	742,188	890,62	
Feedlot capacity take-up of distiller grain	50%	0%					
of di		5%	205,625	274,167	342,708	411,25	
b dr		10%	397,500	530,000	662,500	795,00	
Ke-L		15%	575,625	767,500	959,375	1,151,25	
/ tal		20%	740,000	986,667	1,233,333	1,480,00	
bacity		25%	890,625	1,187,500	1,484,375	1,781,25	
ot cap	75%	0%					
edic		5%	308,438	411,250	514,063	616,87	
Fe		10%	596,250	795,000	993,750	1,192,50	
		15%	863,438	1,151,250	1,439,063	1,726,87	
		20%	1,110,000	1,480,000	1,850,000	2,220,00	
		25%	1,335,938	1,781,250	2,226,563	2,671,87	
						. ,	

Table 1.20	Potential distiller grain usage for a range of feedlot capacity take-up at 0% to 25% [DM] diet
	inclusion rates

Eastern Australia feedlot industry	Diet inclusion rate [DM]	Potential distiller grain usage [30% DM] for varying tota feedstuff consumption [a]					
100%	0%						
	5%	411,250	548,333	685,417	822,500		
	10%	795,000	1,060,000	1,325,000	1,590,000		
	15%	1,151,250	1,535,000	1,918,750	2,302,500		
	20%	1,480,000	1,973,333	2,466,667	2,960,000		
	25%	1,781,250	2,375,000	2,968,750	3,562,500		
lote: [a] Sorgh	um WDGS basis for a	all grains 'as is' [30	0% DM]				

Table 1.20continued

6.2 Impact of grain based ethanol production on feed-grain supply in Eastern Australia

6.2.1 Grain demand

As stated in the objective of this study, the Federal Government's current target is to annually produce 350 ML of biofuels in Australia by 2010, 75% of which will come from feed-grain based ethanol production. This equates to 262.5 ML and so for the purposes of assessing the impact of current Government policy, attention should be focused on the data presented for the 250ML ethanol production scenario.

In order to assess the potential impact of a mandated E10 inclusion policy on the feed-grain supply in Eastern Australia, attention should be focused on the data presented for the 2,500ML ethanol production scenario [based on the equivalent proportion of automotive gasoline as presented in Table 1.13].

Table 1.21 presents the various grain demands for ethanol production levels. For 250 ML [approximately 1%] and 2,500ML [approximately 10%] production targets, the sorghum based grain demand would be in the order of 614,000 and 6,142,000 tonnes respectively. Alternatively, if wheat were to be used, approximately 686,000 tonnes would be needed to produce 250 ML of ethanol and 6,861,000 tonnes for 2,500ML of ethanol. The totals can be determined on a pro rata basis if there are multi-grain sources.

Ethan	ol production	Representative 2006 Eastern Australia gasoline sales	Barley	Corn	Sorghum	Wheat
		[a]				
		%	Tonnes	Tonnes	Tonnes	Tonnes
(0	1 ML		3,055	2,618	2,457	2,744
Study scenarios	250 ML	1.03	763,685	654,587	614,224	686,108
Sena	500 ML	2.06	1,527,370	1,309,175	1,228,448	1,372,216
y so	1,000 ML	4.12	3,054,741	2,618,349	2,456,896	2,744,433
stud	2,500 ML	10.29	7,636,852	6,545,873	6,142,241	6,861,082
0)	5,000 ML	20.58	15,273,705	13,091,747	12,284,481	13,722,165
ote:	[a] Refer Table	1.13				

Table 1.21 Feed-grain demand for levels of grain based ethanol production

6.2.2 Grain supply

The establishment of a grain based ethanol industry will obviously increase the domestic demand for grain in Eastern Australia. Based on the above figures, it can be seen that at the 2,500 ML level, the demand for grain ranges from between 6,142,000 and 6,860,000 tonnes annually. This represents about 25% and 65% of cereal grain produced in Eastern Australia in 2002, and the drought year 2003 respectively [Refer to Table 1.1].

Sorghum grain is produced in northern New South Wales and Queensland. The five-year average production to 2005 is approximately 30% of that required for a 2,500 ML grain based ethanol industry [Refer to Table 1.2]. However, as Table 1.22 shows, the current volume of sorghum grain is largely consumed in the domestic market and it is therefore possible that a grain based Eastern Australia ethanol industry may encourage increased sorghum production in a movement away from other crops. Alternatively, the ethanol production industry will be dependent on wheat as its principal source feed-grain.

Approximately 50% of Eastern Australia wheat produced comes from New South Wales [Refer to Table 1.2]. The demand on wheat supplies to support a 2,500 ML grain based ethanol industry would severely diminish the national wheat volume for export. For example, Table 1.22 shows that 38% of the 2004 nationally exported crop would be required for ethanol production or 73% of the drought affected 2003 exported crop.

Table 1.22 Supply and	2001-02	2002-03	2003-04	2004-05	2005-06 [s]	2006-07 [f]
	·000	·000	·000	·000	·000	'000
	Tonnes	Tonnes	Tonnes	Tonnes	Tonnes	Tonnes
Barley	Tonnoo	Tormoo	ronnoo	1011100	1 of mileo	Tormoo
Production	8,280	<u>3,865</u>	10,382	7,740	<u>9,869</u>	<u>5,840</u>
Domestic use	2,535	2,016	2,476	2,685	2,805	2,921
– as malt and other	2,000	2,010	2,0	2,000	2,000	2,021
human use	161	165	168	172	176	180
– feed	2,200	1,650	2,100	2,300	2,450	2,560
– seed	174	201	208	213	180	181
Export	5,274	2,608	6,996	4,862	5,760	5,031
– feed barley	2,971	885	4,241	2,798	3,401	2,972
– malting barley	1,705	1,099	2,135	1,464	1,765	1,493
– malt [grain equivalent]	600	624	624	601	595	565
Corn	000	021	021	001	000	000
Production	<u>454</u>	<u>310</u>	<u>395</u>	<u>420</u>	<u>380</u>	<u>385</u>
Domestic use	440	294	385	302	374	378
– human, industrial	101	104	106	109	112	115
– feed	338	189	277	192	261	262
– seed	1	1	1	1	1	1
Export [c]	63	16	10	5	6	6
Oats				-	-	-
Production	1,434	<u>957</u>	<u>2,018</u>	1,283	<u>1,416</u>	1,080
Domestic use	1,244	836	1,809	1,182	1,229	919
– human	125	128	131	134	138	141
– feed	1,076	656	1,635	1,007	1,053	740
– seed	44	52	43	41	38	39
Export	190	121	210	138	224	272
Sorghum						
Production	<u>2,021</u>	1,465	2,009	2,011	<u>2,019</u>	2,287
Domestic use	1,646	1,401	1,386	1,935	1,721	2,198
– feed	1,643	1,397	1,382	1,930	1,717	2,193
– seed	3	<u> </u>	3	, 4	4	5
	2002-03	2003-04	2004-05	2005-06	2006-07	2007-08
Export [c]	375	64	623	259	276	121
Triticale [b]						
Production	<u>860</u>	<u>327</u>	<u>826</u>	<u>610</u>	676	<u>525</u>
Domestic use	860	327	826	615	676	525
– feed	840	305	809	598	660	508
– seed	20	22	17	17	16	17
Wheat						
Production	24,299	10,132	26,132	21,905	25,090	16,408
Domestic use	4,894	5,666	5,139	5,282	5,457	5,660
 human and industrial 	2,291	2,378	2,351	2,361	2,408	2,458
– feed [b]	2,100	2,700	2,185 c		2,548 c	2,637 c
– seed	503	588	603	584	501	564
Exports	16,317	9,107	17,867	14,675	15,388	16,649
Change in stocks	3,088	-4,641	3,126	1,948	4,244	-5,901
Total grains	·					
Production	37,348	17,056	41,762	<u>33,969</u>	39,449	26,524
Domestic use	11,620	10,540	12,020	12,002	12,262	12,600
Exports [a]	22,219	11,916	25,707	19,938	21,655	22,079

Table 1.22 Supply and disposal of Australian grains

Note: [a] Wheat export figures are for winter crop years defined as October – September. Production may not equal the sum of apparent domestic use and exports in any one year due to reductions or increases in stock levels.

[b] Calculated as a residual: production less exports less change in stocks

[c] Does not include imports

[s] ABARE estimate [f] ABARE forecast

Source: ABARE^[7]

6.2.3 By-product substitution for grain

The figures provided in the previous section, clearly show that ethanol production from feed-grain will cause a net loss of available high energy feedstuffs, particularly to the cattle feedlot industry but also more generally to the intensive livestock industries. These losses are to some extent offset by the use of distiller grain as a substitute for part of the grain in feedlot diets and Table 6.2.3.1 illustrates the scenario in which sorghum is the sole base grain for ethanol production.

Ethanol production		Feed-grain demand	Distiller gra	in produced	High energy feedstuff net gain/[loss] to the intensive livestock industries
		Sorghum Sorghum WDGS Sorghum DDGS		Sorghum grain <i>less</i> Sorghu DDGS	
	[Annual]	[88% DM]	[30% DM]	[90% DM]	[88% DM; 90% DM]
		Tonnes	Tonnes	Tonnes	Tonnes
<i>(</i>)	1 ML	2,457	1,938	646	[1,811]
arios	250 ML	614,224	484,375	161,458	[452,766]
sus	500 ML	1,228,448	968,750	322,917	[905,531]
y sc	1,000 ML	2,456,896	1,937,500	645,833	[1,811,063]
Study scenarios	2,500 ML	6,142,241	4,843,750	1,614,583	[4,527,657]
<i>с</i> у	5,000 ML	12,284,481	9,687,500	3,229,167	[9,055,314]

Table 1.23 Effect of ethanol production on net feed availability with sorghum as the sole base	grain
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For example, ethanol production at 250 ML demands approximately 615,000 tonnes of sorghum annually, with a by-product of approximately 161,000 tonnes of DDGS [or equivalent] of similar dry matter content and nutrient energy value to dry-rolled sorghum. Ethanol production at 2,500 ML produces approximately 1,615,000 tonnes of DDGS of similar nutrient value to dry rolled sorghum. The net loss of high energy feedstuffs to the intensive livestock industries would be approximately 470,000 tonnes at 250 ML and 4,700,000 tonnes at 2,500 ML ethanol production levels.

In addition, the limitations associated with the use and incorporation of distiller grain in diets restricts its use [Refer to Section 5.2]. At typical industry diet inclusion rates of 5% to 25% the amount of by-product rapidly exceeds that capable of being gainfully consumed by the existing feedlot industry as shown in Table 1.20. The fact that a significant proportion of the cattle's diet must come from additional dry matter diminishes the counterbalancing effect of the distiller grain on the reduced supply of grain associated with ethanol production.

Table 1.24 illustrates that if 25% of the Eastern Australia feedlot capacity included distiller grain in feedlot diets at 15% DM, there would be in the order of approximately 33,500 tonnes surplus of DDGS [or equivalent] at the 250 ML and this rises significantly to approximately 1,487,000 tonnes for 2,500 ML ethanol production levels. If feedlots were to include DDGS at 20% of the diet, the table shows that there would be a shortfall of approximately 3,000 tonnes for 250ML ethanol production but a surplus of approximately 1,450,000 tonnes for 2,500 ML ethanol production levels.

Eastern Australia feedlot industry		Potential distiller grain consumption [a]		Distiller grain surplus/[deficiency] for feedlot industry demand and ethanol production levels					
Capacity	take-up	% Diet [DM]	Sorghum WDGS	Sorghum DDGS	[Sor	ghum DDGS	produced <u>le</u>	ess potential c	lemand]
			[30% DM]	[90% DM]	[90% DM]	[90% DM]	[90% DM]	[90% DM]	[90% DM]
			Tonnes	Tonnes	Tonnes	Tonnes	Tonnes	Tonnes	Tonnes
					At 250 ML	At 500 ML	At 1000 ML	At 2500 ML	At 5000 ML
	25%	0%							
		5%	137,083	45,694	115,764	277,222	600,139	1,568,888	3,183,47
		10%	265,000	88,333	73,125	234,583	557,500	1,526,249	3,140,83
		15%	383,750	127,917	33,542	195,000	517,916	1,486,666	3,101,24
		20%	493,333	164,444	[2,986]	158,472	481,389	1,450,138	3,064,72
		25%	593,750	197,917	[36,458]	125,000	447,916	1,416,666	3,031,24
	50%	0%							
rain		5%	274,167	91,389	70,069	231,528	554,444	1,523,194	3,137,77
er g		10%	530,000	176,667	[15,208]	146,250	469,166	1,437,916	3,052,49
stille		15%	767,500	255,833	[94,375]	67,083	390,000	1,358,749	2,973,33
of di		20%	986,667	328,889	[167,431]	[5,972]	316,944	1,285,694	2,900,27
o dn-ə		25%	1,187,500	395,833	[234,375]	[72,917]	250,000	1,218,749	2,833,33
Feedlot capacity take-up of distiller grain	75%	0%							
paci		5%	411,250	137,083	24,375	185,833	508,750	1,477,499	3,092,08
t cal		10%	795,000	265,000	[103,542]	57,917	380,833	1,349,583	2,964,16
ollo		15%	1,151,250	383,750	[222,292]	[60,834]	262,083	1,230,833	2,845,41
Гее		20%	1,480,000	493,333	[331,875]	[170,417]	152,500	1,121,249	2,735,83
		25%	1,781,250	593,750	[432,292]	[270,834[52,083	1,020,833	2,635,41
	100%	0%							
		5%	548,333	182,778	[21,320]	140,139]	463,055	1,431,805	3,046,38
		10%	1,060,000	353,333	[191,875]	[30,417]	292,500	1,261,249	2,875,83
		15%	1,535,000	511,667	[350,208]	[188,750]	134,166	1,102,916	2,717,49
		20%	1,973,333	657,778	[496,320]	[334,861]	[11,945]	956,805	2,571,38
		25%	2,375,000	791,667	[630,208]	[468,750]	[145,834]	822,916	2,437,49

Table 1.24	Effect of feedlot industry up-take and ration inclusion rate on distiller grain consumption with
	sorghum as the sole base grain

Note: [a] Based on Eastern Australia feedlot industry total feed consumption 4,000,000 tonnes annually, adjusted for DM.

6.3 Examples of regional impacts for the feedlot industry in Eastern Australia

6.3.1 Overview

Table 1.25 examines the variability of Eastern Australia grain production over the years 1998 to 2006 as well as the adequacy of grain production during past high, average, and low yielding years in relation to the existing domestic demand. It also considers the extra requirements imposed by the development and expansion of the ethanol industry.

Eastern Australia grain is consumed domestically [primarily for human use and intensive livestock industries] and is also exported. In recent average years, there was in the order of approximately 15,100,000 tonnes for export, rising to approximately 19,200,000 tonnes in high yielding years. In the most recent year of lowest yield between 1998 and 2006 there was only a small surplus of approximately 3,700 tonnes for domestic requirements.

A small grain based ethanol industry producing 250 ML would further reduce this overall surplus, and an industry producing 2,500 ML would bring about a grain deficiency in Eastern Australia of approximately 2,450,000 tonnes before human consumption [Refer to Table 1.25]. Whilst this shortfall may be reduced by the use of the ethanol by-products in the intensive livestock industries, these make a minor contribution in the overall supply of energy feedstuffs. As such, it is possible that Eastern Australia would be required to import grain in such a year to meet domestic demand.

							Eastern Aus	stralia	
					Unit	Year	Tonnes		
Α.		Grain Production							
		Annual Supply							
			Highest yield	[a]	tonnes	2004	26,626,998		
			Average	[b]	tonnes	1998- 2006	22,508,008		
			Lowest yield	[c]	tonnes	2003	11,093,960		
В.		Grain Demand							
	[a]	Established Domesti	С						
		Fe	edlot industry	[d]			2,509,063		
		O	ther domestic	[e]			4,887,467		
			Total				7,396,530		
	[b]	Add Domestic Production	Ethanol						
		Production Capacity:			ML		0	250	2,500
		Annual grain demand:							
			Sorghum	[f]	tonnes			614,224	6,142,240
			Wheat	[g]	tonnes			011,221	0,112,210
			Total		tonnes			614,224	6,142,240
C.		Grain Surplus/[Defici	ency]	[h]					
	[a]	Currently,							
		A - Ba							
			Highest yield	[a]	tonnes		19,230,468		
			Average	[b]	tonnes		15,111,478		
			Lowest yield	[c]	tonnes		3,697,430		
	[b]	Situation, following e production grain den							
		A - [Ba + Bb]					10 000 100		
			Highest yield	[a]	tonnes		19,230,468	18,616,244	13,088,228
			Average		tonnes			14,497,254	
			Lowest yield	[c]	tonnes		3,697,430	3,083,206	[2,444,810]
Notes:	[a] [b] [c] [d] [f] [g] [h] [i]	Highest 1998-2006 Average 1998-2006 Lowest 1998-2006 Based on 2006 Easter Based on 2005 Easter Sorghum DM - 88% Wheat DM - 90% Based on sorghum sta Domestic, before prov	n Australia; Ha	afi and	at 80% utilis. Connell ^{!4]}	ation			

Table 1.25 Overview impact of ethanol production in Eastern Australia on grain availability [i]

6.3.2 Indicative impacts on regional feedlot industries

The potential impact of a grain based ethanol industry is examined in three major feedlot industry regions with particular respect to their grain supply and demand balance. These are South East Queensland, comprising the Darling Downs, Brisbane, Moreton, Wide-Bay Burnett Statistical Divisions, and in New South Wales the Northern and Murrumbidgee Statistical Divisions.

Within each region, four annual levels of ethanol production are examined: 80 ML, 160 ML, 240 ML, and 400 ML. For each of these production levels, it is assumed that 50% of the distiller grain is available to the feedlot industry when commercially and practically attractive. It is assumed that the other 50% will be utilised by intensive livestock industries other than the feedlot industry or further processed [e.g. to electricity, fertiliser, etc]. In all cases, the distiller grain used is DDGS.

The examples reflect the contribution that DDGS will make to the feedlot industry at various capacity take-up rates and diet inclusion rates. The regions' grain surplus/[deficiency] is estimated with recognition that it may replace grain in feedlot diets [Refer to Section 6.1].

Wherever possible, grain movements between regions may balance the indicated shortfalls but it must be noted that this adds cost to the feedstuff. Further demand will necessitate extra grain importation and associated added cartage costs for all users.

South East Queensland [Darling Downs, Brisbane, Moreton, Wide-Bay Burnett]

This region embraces Statistical Divisions with a feedlot capacity of 393,624 SCU as at June 2006 [Refer to Table 1.7]. The current grain demand for this capacity at 80% utilisation is assessed at 1,011,614 tonnes annually.

Table 1.26 highlights the impact of an ethanol industry, before provision for grain exports and interregional transfers. It is notable that:

- Based on current feedlot industry practices, there is adequate grain for the domestic demand before exports in the high yield years between 1998 and 2006. Demand exceeds supply in the average and low yield years. In the low yield year, the shortfall exceeds 566,000 tonnes. The region is thus grain deficient in the average and low yield years.
- Ethanol production has high grain demand. Taking this into account, there are shortfalls in grain supply in all low yield years [by approximately 764,000 and 1,550,000 tonnes at 80 ML and 400 ML respectively], all average yield years [by approximately 205,000 and 991,000 tonnes at 80 ML and 400 ML respectively] and also in the high yield year with a 400 ML ethanol production capability [by approximately 167,000 tonnes].

The by-product distiller grain can be a useful, although restricted use, feedstuff when favourably priced. Its contribution to the nutrient energy supply is demonstrated for the low yield year. It is notable that:

• For a range of feedlot capacity take-ups [25%, 50%, 75% of SCU] and DDGS diet inclusion rates [5%, 15%, 25% DM], there remains major shortfalls in the available grain [or grain plus DDGS] for **all** ethanol production levels. The example shortfalls range from approximately 500,000 to 1,530,000 tonnes.

The grain shortfalls indicated may be fulfilled by increased production on existing cropped land, the development of new agricultural land and/or the change to grain growing from alternative crops. These options may be restricted and the importation of grain from adjoining regions or beyond appears seems most probable.

Clearly, an ethanol industry in South East Queensland will exacerbate the region's already grain deficient status.

						SE Queensla Darling Dow		, Moreton, W	ide Bay-Burne	tt
				Unit	Year	Tonnes				
Α.		Grain Production								
		Annual Supply								
		Highest yield	[a]	tonnes	2000	2,626,418				
		Average	[b]	tonnes	1998-2006	1,802,051				
		Lowest yield	[c]	tonnes	2001	1,243,703				
В.		Grain Demand								
	[a]	Established Domestic								
		Feedlot industry	[d]			1,011,614				
		Other domestic	[e]			799,064				
		Total				1,810,678				
	[b]	Add Domestic Ethanol Production								
		Production Capacity:		ML		0	80	160	240	400
		Annual grain demand:								
		Sorghum	[f]	tonnes			196,552	393,103	589,655	982,758
		Wheat	[g]	tonnes						
		Total		tonnes			196,552	393,103	589,655	982,758
С.		<u>Grain</u> Surplus/[Deficiency]	[h]							
	[a]	Currently,								
		A - Ba								
		Highest yield	[a]	tonnes		815,740				
		Average	[b]	tonnes		[8,627]				
		Lowest yield	[c]	tonnes		[566,975]				
	[b]	Situation, following ethanol production grain demand								
		A - [Ba + Bb]								
		Highest yield	[a]	tonnes		815,740	619,189	422,637	226,085	[167,018]
		Average	[b]	tonnes		[8,627]	[205,178]	[401,730]	[598,282]	[991,385]
		Lowest yield	[c]	tonnes		[566,975]	[763,526]	[960,078]	[1,156,630]	[1,549,733]

Table 1.26	Potential impact of ethanol production on grain availability in the South East Queensland Statistical
	Divisions of Darling Downs, Moreton, Brisbane, Wide Bay-Burnett [i]

Continued...

Table 1.26 continued

				SE Queensl Darling Dov		, Moreton, W	ide Bay-Burn	ett
[c]	Situation, after adding back DDGS included in diet, for lowest yield year	[i], [j]						
	A - [Ba + Bb] + DDGS	[k], [l]					
	Capacity take-up	25%	of SCU					
	Inclusion rate	5%	of diet		[745,964]	[942,515]	[1,139,067]	[1,532,170]
		15%			[710,838]	[907,390]	[1,103,942]	[1,497,045]
	Capacity take-up	50%	of SCU					
	Inclusion rate	5%	of diet		[728,401]	[924,953	[1,121,504]	[1,514,608]
		15%			[658,150]	[854,702	[1,051,253]	[1,444,357]
		25%			[587,899]	[784,451	[981,002]	[1,374,106]
	Capacity take-up	75%	of SCU					
	Inclusion rate	5%	of diet		[710,838]	[907,390]	[1,103,942]	[1,497,045]
		15%			[605,462]	[802,013]	[998,565]	[1,391,668]
		25%			[500,085]	[696,637]	[893,189]	[1,286,292]
Notes:	[k] DDGS incorporated	6 pacity a afi and 6 provisio product d at thr	Connell ^[4]	ake-up rates, three			er, etc	

Northern, New South Wales

The Northern New South Wales Statistical Division is Eastern Australia's predominant grain producing region with the second largest feedlot capacity of 157,838 SCU as at June 2006 [Refer to Table 1.7. The current grain demand for this capacity at 80% utilisation is assessed at 405,644 tonnes annually.

The impact of an ethanol industry in Northern New South Wales before provisions for grain exports or inter-regional transfers is illustrated in Table 1.27.

• Based on current feedlot industry practices, there is adequate grain for the domestic demand before exports in high, average and low yield years between 1998 and 2006.

 Ethanol production has high grain demand. Ethanol production at 240 ML and above will create regional grain shortfalls in the low yield year ranging from approximately146,000 tonnes at 240 ML ethanol production to 553,000 tonnes at 400 ML ethanol production.

As is the case for South East Queensland, the by-product distiller grain can be a useful, although restricted use, feedstuff when favourably priced. Its contribution to the nutrient energy supply is demonstrated for the low yield year. It is notable that:

 For a range of feedlot capacity take-ups [25%, 50%, 75% of SCU] and DDGS diet inclusion rates [5%, 15%, 25% DM], there remains major shortfalls in the available grain [or grain plus DDGS] for ethanol production at 240 ML and above. The shortfalls range from approximately 41,000 to 546,000 tonnes.

Whilst the grain shortfalls may be reduced by increased production on existing cropped land, the development of new agricultural land and/or the change to grain growing from alternative crops, these options may be restricted. The region may have to rely on the importation of grain from adjoining regions or beyond.

An ethanol industry in Northern New South Wales will lead to grain shortfalls in low yield years, eliminating surpluses for export. This may be further exacerbated with grain transfers to South East Queensland to meet the concurrent potential shortfalls and grain deficit status.

						Northern, Ne	w South Wale	es		
				Unit	Year	Tonnes				
Α.		Grain Production								
		Annual Supply								
		Highest yield	[a]	tonnes	2005	3,798,156				
		Average	[b]	tonnes	1998-2006	2,550,081				
		Lowest yield	[c]	tonnes	2003	960,514				
В.		Grain Demand								
	[a]	Established Domestic								
		Feedlot industry	[d]			405,644				
		Other domestic	[e]			90,917				
		Total				496,561				
	[b]	Add Domestic Ethanol Production								
		Production Capacity:		ML		0	80	160	240	400
		Annual grain demand:								
		Sorghum	[f]	tonnes			137,586	275,172	412,759	687,931
		Wheat	[g]	tonnes			65,866	131,733	197,599	329,332
		Total		tonnes			203,453	406,905	610,358	1,017,263
C.		<u>Grain</u> Surplus/[Deficiency]	[h]							
	[a]	Currently,								
		A - Ba								
		Highest yield	[a]	tonnes		3,301,595				
		Average	[b]	tonnes		2,053,520				
		Lowest yield	[c]	tonnes		463,953				Continued

Table 1.27 Potential impact of ethanol production on grain availability in the Northern NSW Statistical Division [i]

	Northern, New South Wales											
[b]	Situation, following ethanol production grain demand											
	A - [Ba + Bb]											
	Highest yield	[a]	tonnes	3,301,595	3,098,143	2,894,690	2,691,238	2,284,33				
	Average	[b]	tonnes	2,053,520	1,850,068	1,646,615	1,443,163	1,036,25				
	Lowest yield	[c]	tonnes	463,953	260,501	57,048	[146,404]	[553,31				
[c]	Situation, after adding back DDGS included in diet, for lowest yield year	[i], [j]										
	A - [Ba + Bb] + DDGS	[k], [l]									
	Capacity take-up	25%	of SCU									
	Inclusion rate	5%	of diet		267,543	64,091	[139,362]	[546,26				
		15%			281,628	78,175	[125,277]	[532,18				
		25%			295,713	92,260	[111,192]	[518,09				
	Capacity take-up	50%	of SCU									
	Inclusion rate	5%	of diet		274,586	71,133	[132,320]	[539,22				
		15%			302,755	99,303	[104,150]	[511,05				
		25%			330,925	127,472	[75,980]	[482,88				
	Capacity take-up	75%	of SCU									
	Inclusion rate	5%	of diet		281,628	78,175	[125,277]	[532,18				
		15%			323,883	120,430	[83,023]	[489,92				
		25%			366,137	162,685	[40,768]	[447,67				
otes:	[k] DDGS incorporated	5 bacity a fi and brovisic broduct d at thr	Connell ^[4]	take-up rates, three			er, etc					

Murrumbidgee, New South Wales

Murrumbidgee, New South Wales, is a major grain producing Statistical Division and has the third largest feedlot capacity – 133,232 SCU as at June 2006 [Refer to Table 1.7]. The current grain demand for this capacity at 80% utilisation is assessed at 342,406 tonnes annually.

The impact of an ethanol industry in Murrumbidgee before provision for exports or inter-regional transfers is illustrated in Table 1.28. It is notable that:

- Based on current feedlot industry practices, there is adequate grain for the domestic demand before exports in the high, average and low yield years between 1998 and 2006.
- Ethanol production has high grain demand. With annual ethanol production at 240 ML and above, there are regional grain supply shortfalls in the low yield year. These shortfalls are approximately 113,000 tonnes at 240 ML and 552,000 tonnes at 400 ML.

The by-product distiller grain can be a useful, although restricted use, feedstuff when favourably priced. Its contribution to the nutrient energy supply is demonstrated for the low yield year. It is notable that:

• For a range of feedlot capacity take-ups [25%, 50%, 75% of SCU] and DDGS diet inclusion rates [5%, 15%, 25% DM], there remains major shortfalls in the grain available [or grain plus DDGS] for ranges of ethanol production at 240 ML and above. The example shortfalls range from approximately 24,000 to 546,000 tonnes.

As stated previously, grain shortfalls may be reduced by increased production on existing cropped land, the development of new agricultural land and/or the change to grain growing from alternative crops, but these options appear to be restricted. The region may have to rely on the importation of grain from adjoining regions or beyond.

An ethanol industry in Murrumbidgee will lead to grain shortfalls in low yield years, eliminating surpluses for export which may be further exacerbated with regional grain transfers to adjoining regions.

					Murrumbidg	ee, New Sout	h Wales		
			Unit	Year	Tonnes				
-	Grain Production								
	Annual Supply								
	Highest yield	[a]	tonnes	2001	2,509,568				
	Average	[b]	tonnes	1998-2006	1,921,256				
	Lowest yield	[c]	tonnes	2003	1,055,728				
	Grain Demand								
[a]	Established Domestic								
	Feedlot industry	[d]			342,406				
	Other domestic	[e]			167,356				
	Total				509,762				
[b]	Add Domestic Ethanol Production								
	Production Capacity:		ML		0	80	160	240	400
	Annual grain demand:								
	Sorghum	[f]	tonnes						
	Wheat	[g]	tonnes			219,555	439,109	658,664	1,097,773
	Total		tonnes			219,555	439,109	658,664	1,097,773
									Continued

Table 1.28 Potential impact of ethanol production on grain availability in the Murrumbidgee NSW Statistical Division [i]

Table 1.28 continued

				Murrumbidg	vidgee, New South Wales					
	<u>Grain</u> Surplus/[Deficiency]	[h]								
[a]	Currently,									
	A - Ba									
	Highest yield	[a]	tonnes	1,999,806						
	Average	[b]	tonnes	1,411,494						
	Lowest yield	[c]	tonnes	545,966						
[b]	Situation, following ethanol production grain demand									
	A - [Ba + Bb]									
	Highest yield	[a]	tonnes	1,999,806	1,780,251	1,560,696	1,341,142	902,03		
	Average	[b]	tonnes	1,411,494	1,191,939	972,384	752,830	313,72		
	Lowest yield	[c]	tonnes	545,966	326,411	106,856	[112,698]	[551,80		
[c]	Situation, after adding back DDGS included in diet, for lowest yield year	[i], [j]	I							
	A - [Ba + Bb] + DDGS	[k], [l]							
	Capacity take-up	25%	of SCU							
	Inclusion rate	5%	of diet		332,356	112,801	[106,754]	[545,86		
		15%			344,245	124,690	[94,865]	[533,97		
		25%			356,134	136,579	[82,975]	[522,08		
	Capacity take-up	50%	of SCU							
	Inclusion rate	5%	of diet		338,300	118,746	[100,809]	[539,91		
		15%			362,078	142,524	[77,031]	[516,14		
		25%			385,857	166,302	[53,253]	[492,36		
	Capacity take-up	75%	of SCU							
	Inclusion rate	5%	of diet		344,245	124,690	[94,865]	[533,97		
		15%			379,912	160,357	[59,197]	[498,30		
		25%			415,579	196,025	[23,530]	[462,63		
lotes:	 [a] Highest 1998-2006 [b] Average 1998-2006 [c] Lowest 1998-2006 [d] Based on 2006 cap [e] Based on 2005; Ha [f] Sorghum DM - 88% [g] Wheat DM - 90% [h] Domestic, <u>before</u> p [i] DDGS DM - 90% [j] Assumes 50% by-p 	6 pacity a afi and 6 provisio	Connell ^[4]	orm: 50% further	processed to e	energy, fertilise	er, etc			

- DDGS incorporated at three feedlot capacity take-up rates, three diet inclusion rates Incorporation of DDGS dependent on commercial acceptance [k]
- [1]

7 Conclusion

This study has evaluated the competitive effect of a grain based Eastern Australia ethanol industry for grain supplies and the likely impact on the established and expanding intensive livestock industries. The nutritional worth of the principal by-products of such an industry has been reviewed and their worth to the feedlot industry assessed.

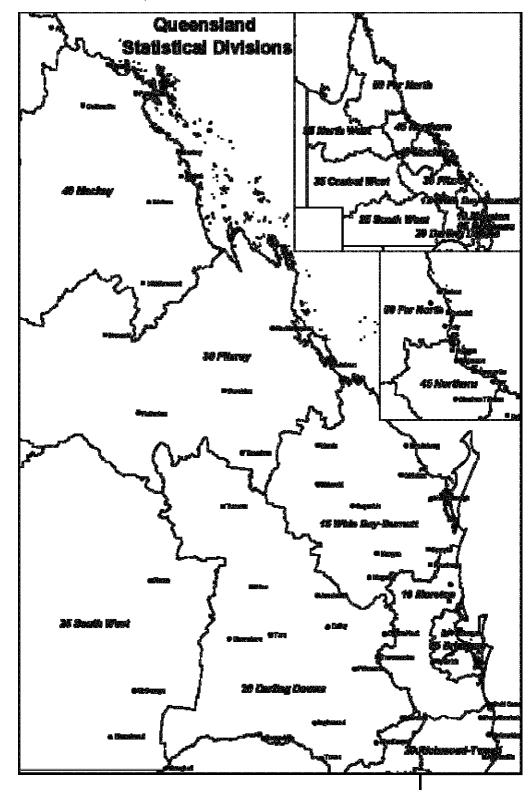
This study provides a detailed analysis of the likely additional grain usage to support grain based ethanol production in line with the current Federal Governments biofuels agenda. This analysis has been conducted for Eastern Australia as a whole, and also with a particular focus on the primary feedlot industry regions in South East Queensland and in the New South Wales Statistical Divisions of Northern and Murrumbidgee. From these calculations, it has been possible to estimate the potential distiller grain by-product production capacity of a range of ethanol plant production facilities. Furthermore, it has been possible to extrapolate this data to evaluate the impact of a potential change in Federal Government policy should there be a mandate for an E10 inclusion policy.

The following primary conclusions can be drawn from the data presented in this study, as well as the North American research in to the use of distiller grains in the feedlot industry:

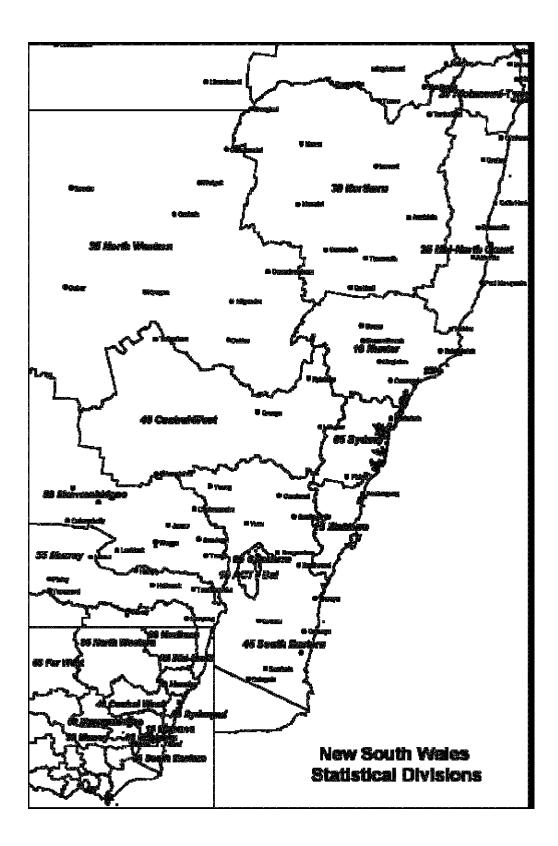
- It is obvious that the ethanol production industry's demand for feed-grains will impact on the
 intensive livestock industries such that shortages which are currently experienced in areas
 such as South East Queensland will become much more acute. Taking into consideration
 ongoing drought conditions, it is likely that there will be significant grain shortages in Eastern
 Australia in average and low yield years, thus resulting in higher costs for the feedlot industry
 as grain will need to be sourced and transported from other regions. This will adversely affect
 the entire Australian beef cattle industry.
- The feed-grain based ethanol production by-products WDGS and DDGS are recognised as quality feedstuffs which are high in nutrient energy, protein and fibre. North American research suggests that these by-products can positively impact on the growth and weight gain of feedlot cattle at diet inclusion rates between five and 25%. However, these byproducts are unable to fully compensate for the grain diverted from the intensive livestock industries, and the feedlot industry will remain dependant on alternative high nutrient energy sources.
- The analysis provided in this study serves only as a guide to the probable impact of a grain based ethanol industry on the Eastern Australia feedlot industry. It is imperative that once ethanol production plants are established across Australia, a full assessment of the quality of the by-products will be required on a plant to plant basis, under Australian conditions.

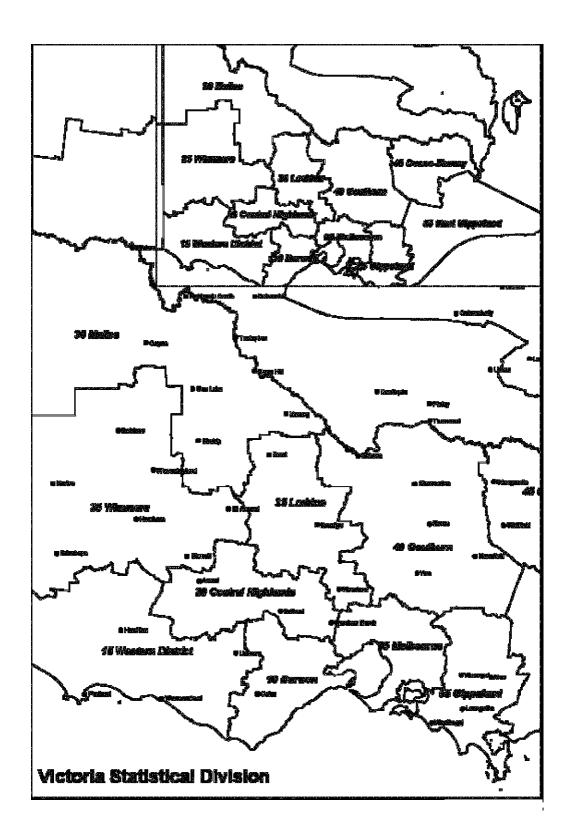
In summary, the development of a feed-grain based ethanol production capacity in Eastern Australia will present significant challenges and opportunities for the cattle feedlot industry, as well as the other intensive livestock industries. It will adversely affect grain supplies and their sources of nutrient energy. A review of grain importation procedures to cover low crop yield years will be necessary. The by-products can be valuable feedstuffs but have associated disadvantages. Ultimately, it will be for individual feedlots to make an assessment of the overall potential benefit of distiller grain by-products on the basis of value and cost-effectiveness according to their individual circumstances.

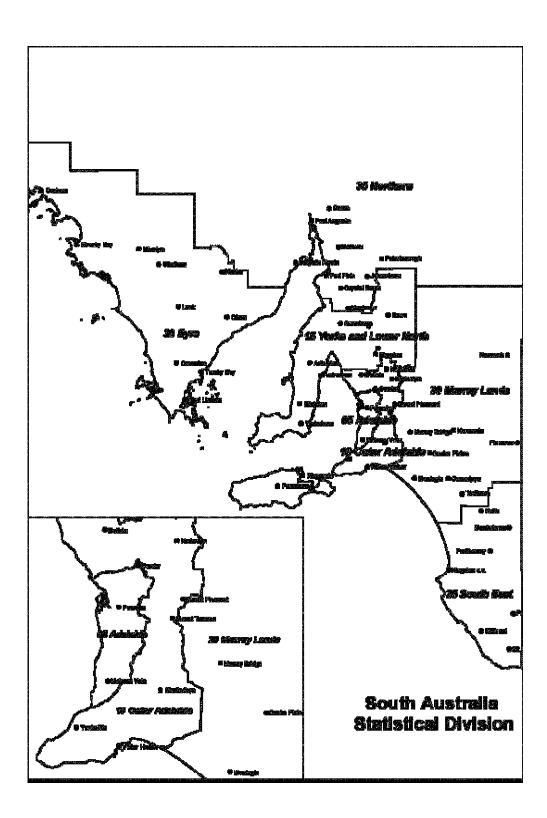
8 Attachments

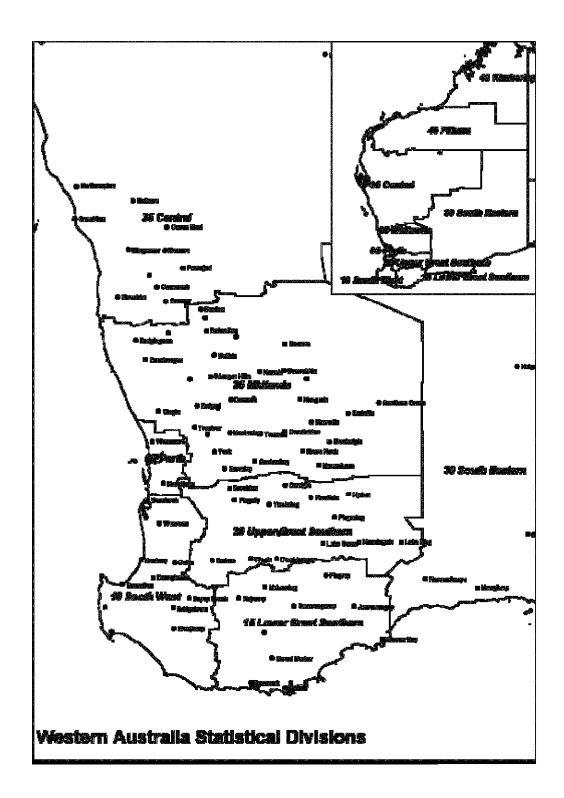


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APPENDIX 2

Nutritive value of distillers grains

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1 BACKGROUND AND METHODOLOGICAL APPROACH

General information is plentiful on the nutritive value of wet (WDG) and dry distillers grains with solubles (DDGS) derived from US corn in the Cornell Net Carbohydrate Protein System (CNCPS) listing (essentially the NRC data) but there is a paucity of data for the other grains of interest. The "Preston" 2006 Feed composition tables (<u>http://www.beef-mag.com/mag/beef_feed_composition_tables_2/</u>) shows data for barley distillers grains, sorghum and corn WDG, dry distillers grains (DDG) and DDGS, The RUMNUT UK database (<u>http://www.rumnut.com/</u>) lists proximate analysis for "Distillers grains" for barley, wheat and corn- these data appear to include solubles, as judged from the fat content relative to the corresponding grain, but the origin of the data is not defined. It is uncertain if the reported proximate composition of distillers grains can be related to that of the parent grain, even within the same database. Available data for the chemical composition of distillers grains in the northern hemisphere are tabulated in Table 2.1

In order to evaluate the nutritive value of Distillers grains derived from Australian grains, we have adopted a methodology that assumes that mass balances can be calculated for changes of proximate composition of the grain as a consequence of removal of fermentable carbohydrate during ethanol production (see ^[1]). In this context, proximate composition comprised ash, neutral detergent fibre (NDF), fat (reported as ether extract in the CNCPS and RUMNUT databases and other literature), starch, and other soluble non-structural carbohydrates including sugars. Where these proximate values did not sum to 100% in the databases, proportional correctional adjustments were made. To calculate the mass balances we assumed that 2% of the starch content and 10% of soluble non-starch carbohydrate of the source grain remained unfermented by yeast enzymes during ethanol production. These were arbitrary assumptions, but were defensible as discussed below. Any contribution to distillers grain protein from yeast, nor loss of fat from the high drying temperatures employed, could not be determined by this methodology.

It is noted that the adoption in the late 1990's of dry grinding and batch fermentation in the "new-generation" plants producing distillers grain products from corn in the USA, has resulted in increased extraction efficiency with a decline of starch content in corn DDGS from 10-15% to <5% ^[2.]. Accordingly data from reports post 1995 are more pertinent for the present exercise.

Calculation of the theoretical nutritive value of distillers grains from Australian barley, corn, sorghum and wheat therefore required the proximate composition of the source grain, reported completely for each sample. This requirement meant that the value of seemingly large databases (e.g. that of the Australian Livestock Feed Ingredient (ALFI), and from the DPI (NSW) "Nutritive value of feeds" (<u>http://www.agric.nsw.gov.au/tools/fes/index.html</u>) was limited, because the required analyses were rarely done on individual samples, and there often was a large difference in sample numbers contributing to means for individual analyses. Complete analyses for barley, sorghum and wheat grain were available from the "Premium Grains for Livestock Production" project, jointly funded by the GRDC and MLA, as contained in the ruminant feedlot software, "AUSBEEF", while limited data for corn were derived from the Australian Food Information Centre (AFIC) listings. These were used to generate compositional data for grain and derived distillers grains, as described in Table 2.2.

	Refs	Starch (%)	Crude Protein (%)	Fat (%)	Neutral detergent fibre (%)	Ash (%)	Phosphorus (%)	Sulphur (%)	Acid detergent fibre (%)	Metabolisable energy (MJ)	Net energy for maintenance (MJ/kg DM)	Net energy for gain (MJ/kg DM)
Distillers products from barley												
Dry distillers grain	1	[17]	30	4	45	4.0	0.7	0.4	22		7.6	4.9
"	2		29		56							
"	3			6		4.2						
Ш	4	2	27	7	42	5.7	0.9			12.2		
Wet distillers grain	5	1	21	8	67	6.0	0.0			12.2		
Wet distillers grain		I	21	0	07	0.0						
Distillers products from corn												
Dry distillers grain	6	5	32	12		4.3			17			
"	7	[11]	30	11	42	5.8	0.9	0.5	16	15.7		
II	8	6	31	15	34	4.6	0.9	0.6	17		10.4	7.3
"	8	6	30	18	31	5.5	1.1	0.6	22		10.9	7.8
"	9	5	32	15	32	4.8	1.0	0.4	17		10.6	7.5
II.	10	5	32		52*		0.8	0.4	17		10.0	7.5
"	11	5	18	11 11	52 51	6 2	0.8	0.7				
u.		5	10	11	51	2						
	1		04	40	40		0.7	0.5	00		40.4	0.0
	1		31	10	40	4	0.7	0.5	22		10.4	6.9
	4	_	30	11	39	5	0.8	0.5	16		10.4	6.9
"	12	2	35	9	30	4	0.8		19	14.8		
II	13	5	31	13	34		0.9	0.6	17			
II	11		30	12	34	5	0.9					
Wet distillers grain		5	30	14	52	1						
ű	1		28	10	40	6	0.8	0.5	16		10.6	7.1
Wet distillers grain	8											
minus solubles	o	7	39	11	45	2.2	0.5	0.5	24		10.1	6.7

Table 2.1. Chemical composition (dry matter basis) of distillers grains from the northern hemisphere

	Refs	Starch (%)	Crude Protein (%)	Fat (%)	Neutral detergent fibre (%)	Ash (%)	Phosphorus (%)	Sulphur (%)	Acid detergent fibre (%)	Metabolisable energy (MJ)	Net energy for maintenance (MJ/kg DM)	Net energy for gain (MJ/kg DM
Distillers products from sorghum												
Dry distillers grain	1	[9]	31	10	47	3	0.7	0.4	19		8.6	5.7
"	1	[9]	32	10	44	3	0.6	0.5	13		8.6	5.7
ш	14	L 1 2	23	7		4	-	-		10.9	-	
n	15	5	50	, 11		4	0.8			1010		
"	11	7	30 31	12	51	2	0.0					
н	16	i	30	12	51	2 5	0.8				8.9	5.8
"	17		30 29			5	0.0				0.3	0.0
	17			9								
"	18	0.7	29	9								
-	1	6.7	36		57	_						
Wet distillers grain	11	[9]	32	10	44	3	0.6	0.5	13		8.9	5.9
ű		10	32.	11	45	3						
Distillers products from wheat	10											
Dry distillers grain	10	3	45	3	47*	6	1.1	0.5	12			
- "	10	4	31	4	57*	9	1.2	0.6	11			
п	10	5	39	5	50*	6	0.8	0.4	11			
"	2		44		36		0.4					16.0
II	19		40	4	31	4.4						13.0
"	4	5	30	6	35	5.0	0.9			12.5		
"	21	0.5	43	7	~ -	5.3						
"	10	0.0	39	8		5.5	1.0		17.1			
Wet distillers grain	20		26		75	1.6						24.0
vvet distillers grain	5	n	26 31	7								
		2	31	7	64	5.0						17.5

*total carbohydrates Values in brackets by difference, starch plus non-starch polysaccharides

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		Fat	Protein	Ash %	Starch	Fibre	Soluble
		%	%	70	%	%	carbohydrate
Barley grain	Av	3	10	3	60	10	14
Darloy grain	5%	3	7	3	63	10	14
	-5%	3	13	3	57	10	14
Distiller's grain	Av	11	35	9	4	36	5
from barley	5%	12	28	10	5	40	6
	-5%	10	42	8	4	33	5
Corn grain	Av	4	10	2	70	12	4
oom gram	5%	4	10	2	74	8	4
	-5%	4	10	2	67	15	4
Distiller's grain	Av	14	34	6	5	41	1
from corn	5%	16	38	6	6	32	1
	-5%	12	30	5	4	47	1
Sorghum grain	Av	3	8	1	75	10	3
oorginalin grain	5%	3	8	1	78	6	3
	-5%	3	8	1	71	14	3
Distiller's grain	Av	13	33	4	6	42	1
from sorghum	5%	15	40	5	8	31	2
	-5%	11	29	4	5	50	1
Wheat grain	Av	2	13	3	65	9	8
J	5%	2	11	2	67	8	8
	-5%	2	15	3	62	10	8
Distiller's grain	Av	7	45	9	5	31	3
from wheat	5%	7	41	9	5	33	3
	-5%	7	49	8	4	30	3

Table 2.2. Chemical compositions (dry matter basis) of Australian grains

The average proximate composition of Australian barley, corn, sorghum and wheat was taken from Rendell ^[3]. It was a negotiated position with the MLA Oversight Committee that the data provided by Rendell represented average starch of Australian grains. Variations in composition were accommodated by increasing and decreasing the Rendell values by 5% and adjusting the other chemical constituents accordingly (Peter, can you improve on accordingly)

The CNCPS software (v. 5.0, level 1) was used to evaluate the comparative nutritive value of the grain and calculated distillers grain, in a diet that provided, on a dry matter basis, 10% roughage (9% crude protein) and a 75% concentrate mixture. The ratio of grain:distillers grain or grain:cotton seed meal adopted for each simulation was that required to give a crude protein content of 15% (dry matter basis) for the entire diet, as is the effective limit tolerated by feedlot operators (Kevin Roberts, pers. comm.). The concentrate component comprised a grain with its daughter distiller's grain or cottonseed meal. No additional attempt was made to balance the ration in any other way. For example, the fat content of the ration was not considered, nor were the practical limitations to the inclusion of cotton seed meal. The aim of the simulations was to evaluate the maximal inclusion level of distiller's grain allowable with the constraint involved, and to illustrate its potential to replace a commonly used protein supplement.

For inputs, values for ash, NDF, fat, starch and (non-starch) soluble carbohydrate of the grain were the average values ^[3] or as calculated with variation from the mean grain starch of \pm 5% which should encompass the range of grain qualities likely under Australian conditions. The lignin content of the fibre fraction (NDF) of the grain, which determined the digestibility of NDF, used for input into the CNCPS software was the mean value of the relevant grain in the AUSBEEF database (barley,0.056, corn 0.069, sorghum 0.14, wheat 0.081). Lignin/NDF values for distillers grain, for barley and wheat (0.076, 0.24) were taken from the RUMNUT database, for corn the CNCPS value (0.23) was adopted, and for sorghum a value of 0.22 was assumed. Where lignification of distillers grain was markedly higher than the source grain, as was the case for wheat and sorghum, the effect of the increase was to reduce the ME content of distillers grain by approx. 7%.

On the basis of results obtained from the simulations, it would have been possible to refine the diet formulations to minimize urea excretion, but this was not done because acceptably precise results would require better definition of digestion and availability of dietary protein than was available. The aim of the simulations was to evaluate the maximal inclusion level of distillers grain allowable with the constraint involved, and to illustrate its potential to replace a commonly used protein supplement.

2 NUTRITIVE VALUE OF AUSTRALIAN GRAINS AND ESTIMATED NUTRITIVE VALUE OF DERIVED DISTILLERSGRAINS

Values for the 3 grain qualities, with respect to starch, within each of the four grains are given in Table 2.3, together with the method of calculation. The standard error of the mean starch content for the 4 grains in the Ausbeef (Australian Feed Information Centre) database was 4.5-4.4%, thus the variation induced by simulating a 5% difference from the mean starch content could be a conservative estimate of the possible variation of grain quality used as feed for the ethanol plant.

The inclusion of distillers grain level allowed by the dietary limit of 15% crude protein, was 23% for average barley, 26% for average corn, 29% for average sorghum, and 11% for average wheat (Table 2.3). If the variation of crude protein content (calculated by inducing the \pm 5% in starch content) adequately represents variation encountered in Australian grains used for ethanol production, a maximum of 20% of distillers grain from barley, corn and sorghum can be included. In contrast, as little as 5% distillers grain from wheat varieties was allowable with wheat of high protein content.

As judged by the net energy (NE) content for either maintenance or gain (NE_m, NE_g) for "average" barley, corn, sorghum and wheat, the energy value of all grains and derived distillers grain was similar, with the exception of sorghum distillers grain, which was about 10% lower (Table 2.3). Variation in grain quality resulted in relatively low variability in NE_m and NE_g (range of 0.5 MJ/kg) within grains, and in distillers grain from barley and wheat, but distillers grain varied markedly within corn and sorghum by about 1.6-2.1 MJ/kg. The reason for this appeared to relate to the variations in fat content of distillers grain of corn and sorghum, and the poor availability of NDF of sorghum. The effect of flaking for Australian average sorghum was examined by application of the level 2 CNCPS software and the appropriate defaults for flaked sorghum in the CNCPS database. Values for NE_m and NE_g were increased by 0.2 units compared to level 1 estimates presented in Table 2.3.

The value of distillers grain relative to cottonseed meal in rations formulated to be 15% CP, was comparable for barley, wheat and sorghum, and slightly superior for corn. The best single (negative) predictor of the nutritive value of distillers grain was NDF content of the parent grain (data not shown).

For barley, corn and wheat based diets, the predicted daily liveweight gain did not vary by 0.1, or at the most 0.2, kg/d irrespective of whether cottonseed meal or distillers grains were included in the diet (1.9 - 2.1 kg/d). For sorghum, predicted liveweight gain varied from 1.7 kg/d for low starch sorghum and sorghum distillers grain to 2.1 kg/d for high starch sorghum and distillers grain.

	Grain (% of diet DM)	Distille rs grain (% diet DM)	Cottonsee d meal (% of diet DM)	Net energy for maintenanc e (MJ/kg) Grain/Distill ers grain	Net energy for gain (MJ/kg) Grain	Liveweig ht gain (kg/d)	Metabolisabl e Energy of diety (MJ/kg)	Fat (% of diet DM)
Barley				oro gram				
Average	52	23	-	8.9/8.7	6.1/5.9	2.1	11.7	4.3
+5%	36	40	-	8.9/8.4	6.0/5.7	2.0	11.6	6.1
-5%	62	13	-	8.8/8.8	6.0/6.0	2.1	11.7	3.4
Average	57	-	18			2.0	11.4	2.9
+5%	52	-	23			1.9	11.3	3.0
-5%	63	-	12			2.1	11.5	2.8
Corn								
Average	49	26	-	9.1/8.8	6.2/6.0	2.1	11.9	5.8
+5%	53	22	-	9.2/9.9	6.4/6.9	2.0	11.6	5.8
-5%	45	30	-	8.9/8.0	6.1/5.3	1.9	11.5	5.8
Average	56	-	19			2.0	11.5	3.5
+5%	56	-	19			2.0	11.6	3.5
-5%	56	-	19			1.9	11.4	3.5
Sorghum Average	46	29		8.8/7.9	6.0/5.2	1.9	11.4	5.5
+5%	40 52	29	-	8.9/9.1	6.1/6.2	2.1	11.4	5.5 5.5
-5%	40	23 35	-	8.6/7.0	5.9/4.4	2.1 1.7	10.9	5.5 5.5
	40 53	55	- 22	8.0/7.0	5.9/4.4	1.7	10.9	3.1
Average	53 53	-	22			1.9	11.3	3.1 3.1
+5% -5%	53 53	-	22			1.9	11.4	3.1 3.1
Wheat								
Average	64	11	-	8.7/8.8	5.9/6.0	2.0	11.6	2.4
+5%	58	17	-	8.2/8.7	5.5/5.9	2.0	11.5	2.7
-5%	70	5		8.7/8.6	5.9/5.8	2.0	11.5	2.2
Average	63	-	12	5, 6.0	5.0,010	1.9	11.4	2.2
+5%	58		17			1.9	11.3	2.3
-5%	68		7			2.0	11.5	2.1

Table2.3. Nutritive value of distillers grains and predicted liveweight gain of cattle with inclusions of distiller's grains in the diets.

3 DISCUSSION

3.1 Nutritive value

Literature from the USA suggests that the nutrient composition of corn distillers grain, as with many byproduct feeds, is influenced by multiple variables including type of grain used, grain quality, grinding procedures, extent of fermentation, drying conditions, quantity of solubles blended back with the cake and particle separation. An approximately three-fold concentration of protein, fat and fiber is found in distiller's grain compared to corn grain. The resulting product is deemed to be very palatable and its high digestible energy content is associated with high fat content and digestible fibre. Replacement of corn grain with distillers by - product apparently consistently improves feed conversion efficiency ^[4] by the increased supply of nutrients such as fat and protein, but also through importantly reduction the incidence of subclinical acidosis ^{[5].}

In the USA, corn distillers grain appears to be more valued for the dairy industry than for beef cattle, where the high protein content can lead to wastage of nitrogen. Accordingly heat damage of protein and consequent reduction in digestibility during the production of ethanol is a concern with dairy animals, but not for feedlot animals. Shingoethe ^[6] stated that some decreases in dry matter intake can occur when fed high amounts of distillers grain, especially when fed as wet distillers grain.

The present simulation results are somewhat dependent on the value of lignin/NDF attributed to the distillers grain. The increased lignification (presumably by formation of 'artifact' lignin) of distillers grain evident in the databases (RUMNUT and CNCPS) for wheat and corn presumably is a result of heat treatment during the ethanol production process. Heating is stated to result in the decreased nutritive value of DDGS versus wet distillers grain, but we have not attempted to simulate this specifically to evaluate the effect of drying because information seems to be limited to corn for which the mean lignin/NDF in both wet distillers grain and DDGS was similar (20.1 %, Badger State Ethanol data, University of Illinois website at: http://ilift.traill.uiuc.edu/distillers/) However, other authors (Erickson *et al.* 2006 ^[4] have reported that NEg of corn wet distillers grain of 8.03 MJ/kg was about 12% higher than that the value (7.20) for DDGS. We therefore suggest a further discount to ME content of about 5% be made for calculation when considering DDGS.

The predicted starch content for Australian distillers grain was from 4 - 8% in the present simulations. For fat in distillers grains, predicted values were about 7% for wheat and 10–15% for corn, barley and sorghum (see Table 2.2). Approximate literature values for starch and fat content of distillers grain for barley are 2 and 7%; for corn, 5% and 11%; and for sorghum, 5-10% and 13%; and for wheat, 3% and 5% (see Table 2.1). The predicted fat content for Australian distillers grains were therefore in the higher end of the published range for DDGS, possibly because no accounting was made for loss of volatiles from fat during the drying process. Because fat is the most energy-dense constituent of distillers grain and therefore the single most important determinant of nutritive value, its high content in corn distillers grain provides the explanation of the high ME content. It was more difficult to substantiate the assumption that 90% of soluble polysaccharides were metabolized by yeast during ethanol production, although this assumption lead to a predicted content of 1-5% of soluble non-starch polysaccharides in Australian distillers grains, comparable to reported values for sugars of 2-9% for barley, corn and wheat in the RUMNUT database, and for 4% for corn DDGS in the Badger State Ethanol data.

3.2 Growth trials

A direct comparison of wet distillers grains from sorghum and corn was reported by Al-Suwaiegh et al ^[7]. Both distillers products, when they replaced 30% of the dry matter of corn, resulted in 10% greater liveweight gain and 8% greater feed conversion efficiency than the corn-based control. The improved nutritive value (estimated as net energy for gain) of wet distillers grains was calculated to be 33% (corn) and 25% (sorghum) than that supplied by corn by itself; the increased lipid content accounted for about 45% of the increase. Lodge *et al* ^[8] fed (80:20) wet sorghum:corn distillers residues, and reported that efficiency of gain for finishing steers for was about the same as for corn grain, and about 20% higher than sorghum DDGS.

3.3 Quality and consistency

It is thought that some of the lack of consistency in product is introduced at the stage of blending of stillage during the production of distillers grains^[9]. This would apply especially to fat content, as the stillage and distillers grain each contain about 50% each of the fat of the original grain^[10]. Recent surveys both within and between ethanol plants showed large variations for all nutrients measured, although within plants, fat content and ash were more variable than crude protein and NDF^[11].

The variability of nutritive value of DGGS has been largely attributed by Knott *et al* (1997)¹² and Belyea *et al.* (2004)¹³ to the amount of solubles added to the spent grains. The recovery of dry matter in fermentation residues has been summarized by Mustafa^[10] as being 29, 35, 32 and 41% from corn, wheat, barley and sorghum respectively. This report also highlights the differences in chemical composition between thin stillage and distillers grains fraction of the fermentation products. For example, in wheat residues, the thin stillage fraction contains 37% of the residual protein but only 13% of NDF.

The data set from the Badger State Ethanol Plant on the U of Illinois website (<u>http://ilift.traill.uiuc.edu/distillers/nutrient_profiles/midwestplant.cfm</u>) shows that the variability measured for 56 samples taken over a 2-year period was comparatively minor. For crude protein, the coefficient of variation was 6.6% for fat, 10.1%, NDF 12.3%, and for calculated net energies of lactation, gain and maintenance, were 7.6-9.2%.

4 GENERAL CONCLUSIONS

Given the uncertainties in the calculations made in this section, the broad conclusion that can be made is that the value of the distillers grain to supply net energy is comparable to the parent grain, with the possible exception of sorghum, for which the common practice of grain flaking, and the relatively poor digestibility of the fibre in distillers grain, is likely to lead to poorer nutritive value in the distillers grain. If a dry distillers grain product is to be considered, then the net energy content in the distillers grain product would probably be discounted by at least 5%.

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APPENDIX 3

Ethanol production from grain

Life cycle and techno-economic assessment

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GLOSSARY

AD	Anaerobic digestion
AD-GTCC	Anaerobic digestion – gas turbine combined cycle
ar	As-received basis
Beer	Liquid produced by the fermentation of starchy material derived from grains or other plant sources.
CO_2	Carbon dioxide
CO _{2-e}	Carbon dioxide equivalent
CRAC	China Resources Alcohol Corporation
db	Dry basis
Dehydration	Process of removing remaining water from ethanol/water mixture after distillation
DDG	Distillers Dried Grains-obtained after the removal of ethyl alcohol by distillation from the yeast fermentation of a grain or grain mixture by separating the resultant coarse grain fraction of the whole stillage and drying it by methods employed in the grain distilling industry. The predominating grain is declared as the first word in the name.
DDGS	Distillers Dried Grains with Solubles-product obtained after the removal of ethyl alcohol by distillation from the fermentation of grain or grain mixture by condensing and drying at least ³ / ₄ of the solids of the resultant whole stillage by methods employed in the grain distilling industry. The predominating grain is declared as the first word in the name. DDGS is sometimes referred to as Meal
DWG (WDG)	Distillers Wet Grains-product obtained after the removal of ethyl alcohol by distillation from the yeast fermentation of a grain mixture.
DOE	Department of Energy (USA)
E10	Ethanol/petrol blend containing 10% by volume ethanol
E25	Ethanol/petrol blend containing 25% by volume ethanol
E85	Ethanol/petrol blend containing 85% by volume ethanol
EC	European Commission
EBITA	Earnings Before Interest, Tax and Amortisation
ETBE	Ethyl tertiary butyl ether- oxygenated fuel blended with gasoline to make it burn more cleanly
Fermentation	Process of converting sugars into ethanol with yeast
FBR	Fluidised bed reactor
FFV	Flexible Fuel Vehicle

Gelatinisation	Process of hydrolysing and swelling of grain in hot water to obtain starch in solution
GGE	Greenhouse gas emissions
GHG	Greenhouse gases (carbon dioxide, methane and nitrous oxide)
GRDC	Grain Research and Development Corporation
ha	Hectare of land; 10,000 m ²
HHV	Higher heating value (or gross specific energy) basis which includes the heat of condensation of water vapour at 25°C.
IDGCC	Integrated drying gasification combined cycle (gas turbine) – emerging electricity generation process for Victorian brown coal (42% thermal efficiency, with 60-65% moisture coal)
KPI	Key performance indicator
kWh	Kilowatt hour (3.6 MJ)
L	Litre (a capital letter has been used for clarity)
LCA	Life cycle analysis
MTBE	Methyl-t-butyl ether-octane enhancing additive
Multiple effect evaporation	A multiple step process in which heat from the evaporated liquid in one stage is used to evaporate liquid in the next stage (by reducing system pressure), thereby reducing the overall energy consumption.
MWh	Megawatt hour
N ₂ O	Nitrous oxide; greenhouse gas equivalent to 310 that of CO_2 (on a mass basis)
NGCC	Natural gas combined cycle electricity plant.
NREL	National Renewable Energy Laboratory (US DOE)
OECD	Organisation for Economic Co-operation and Development
PAJ	Petroleum Association of Japan
QG	Quick Germ process
QGQF	Quick Germ Quick Fibre process
RFS	Renewable Fuels Standard
R&D	Research and development
R&M	Repairs and maintenance
RO	Reverse osmosis
Saccharification	Process of converting starch into dextrin sugars for fermentation
SMHEA	Snowy Mountains Hydro Electric Authority

Stillage	Residue of non-fermentable (or non-fermented) solids and water after removal of ethanol from fermented beer by distillation; thin stillage is produced after removal of solids
SSF	Simultaneous Saccharification and Fermentation
SSYPF	Simultaneous Saccharification Yeast Propagation and Fermentation
Stover	Dried stalks and leaves of a cereal crop, used as fodder after the grain has been harvested.
Syrup	Concentrated product from stillage after evaporation of water, sometimes called Condensed Distillers Solubles (CDS)
VEETC	Volumetric Ethanol Excise Tax Cedit
VHG	Very High Gravity
WDG	Wet Distillers Grains-product obtained after the removal of ethyl alcohol by distillation from the yeast fermentation of a grain mixture
WUE	Water use efficiency; expressed as kg grain/mm H ₂ O/ha

Currency conversion used in this report for comparisons

1A\$ = US\$0.70 1A\$ = Euro 0.60 1A\$ = 0.39 GBP

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1. EXECUTIVE SUMMARY

This study is a component of a project for the Meat and Livestock Association, undertaken by CSIRO Livestock Industries, and Energy Technology.

The role of CSIRO Energy Technology (CET) was "to provide a technical assessment of the energetic costs and benefits of ethanol production from grain, under Australian crop and ethanol production conditions", and to assist CSIRO Livestock Industries to "determine a realistic feed value of both the wet and dried Wet Distillers Grain products under Australian conditions and establish a protocol, which accounts for the inherent variability in the product due to differences in the base product, ethanol extraction efficiency and water content, by which this value can be calculated". In assisting with the latter objective, CET was tasked with determining a realistic economic and environmental value of wet distillers grain, by examining the costs and greenhouse gas emissions of drying and transport.

These objectives for CET were addressed by carrying out a life cycle and techno-economic analysis for ethanol production from wheat and sorghum, using a number of options for processing the stillage. The analysis was based on a hypothetical plant located at Gunnedah, with a capacity of 160 ML of ethanol per annum.

Whilst a mature technology, ethanol production is continuing to evolve, with improvements throughout the entire process. Anaerobic digestion of stillage is becoming of increasing interest in the USA as a result of over supplies of distillers grain, as well as for offsetting increasing gas and electricity prices.

The analysis considered the life cycle issues of resource energy, greenhouse gas emissions (GGEs), and water consumption, as well as techno-economics.

Resource energy quantifies energy depletion, and relates only to fossil energy inputs; solar energy used for growing the grain is excluded, since it does not represent a depletion of energy resources.

Greenhouse gas emissions are emissions of CO_2 and CH_4 that are generated in the production and combustion of fossil fuels, as well as nitrous oxide produced from the use of nitrogenous fertilisers. Carbon sequestered from the atmosphere by grain, provides a GGE credit.

Water consumption relates to the amount of fresh water used in the production of fertilisers, fuels, etc (in the form of process water), and is used to quantify the depletion of fresh water resources. Water from rainfall used in grain production is not included

The study considered 3 systems for the Life Cycle Analyses (LCAs):

- 1) grain production (wheat and sorghum),
- 2) grain through to ethanol with 7 stillage processing options, and
- 3) grain through to 1 GJ of delivered heat energy (*ie* as combusted ethanol).

For ethanol production, the base process routes were fermentation with the production of dry distillers grain, and fermentation with anaerobic digestion and electricity production. This resulted in 7 case studies, for alternative stillage processing:

- Case 1 Wet Distillers Grain (WDG) direct to feedlot.
- Case 2 Dry Distillers Grain with Solubles (DDGS) with conventional drying.
- Case 3 DDGS with high efficiency drying.

- Case 4 Anaerobic digestion, with gas engine electricity generation (33% efficiency; HHV basis).
- Case 5 Anaerobic digestion, with combined cycle electricity generation from biogas (50% efficiency).
- Case 6 WDG for electricity generation by fluidised bed combustion (20% efficiency).
- Case 7 WDG for electricity generation using integrated drying and gasification combined cycle (IDGCC; 40% efficiency).

LCAs

For grain production, the major resource energy component is for the production of fertiliser (70% of the total). GGEs are dominated by the CO_2 taken up by the grain during photosynthesis, while fresh water is dominated by the water used to grow the grain (500-1000 m³/t grain). It should be noted that the CO_2 sequestered in the grain will ultimately be returned to the atmosphere, partly during production of ethanol, and also when the ethanol is combusted. However, the LCA methodology (with the boundary conditions of either grain production, or ethanol production) requires that the CO_2 sequestered in the grain be included. Values without such sequestration have been included for comparison with other non-compliant LCA studies.

When the grain is processed to ethanol, all indicators are dependent on the processing of the stillage, and by-product credits. Process water consumption is again several orders of magnitude less than that used for growing the grain.

There are 3 key findings for resource energy for ethanol production:

- With direct sale of WDG, the resource energy is considerably lower than that for DDGS, due to the large amount of energy required for drying (can be substantially reduced using a higher efficiency process).
- When the stillage is anaerobically digested, the resource energy also becomes negative, since there is no requirement for purchased electricity or natural gas for ethanol production.
- There are also significant credits for by-product fertilisers and exported electricity. If the WDG is combusted to produce electricity (requires a technology similar to high moisture lignite or biomass), a negative overall resource energy is produced.

The main findings for GGE for ethanol production are as follows:

- All cases have a negative GGE, due to sequestration of CO₂ as grain.
- Direct use of WDG by feedlots gives a lower GGE than for DDGS, due to the emissions associated with drying (again, reduced by a higher efficiency process).
- Use of WDG or DDGS as feed to replace grain increases the overall GGE, as this displaces grain production and lowers the CO_2 being sequestered by photosynthesis.
- WDG can be transported for a large distance (>1000 km) before the GGEs from transport exceeds the GGE from drying and transport of the DDGS (*cf* the economical distance of only 50-60 km).
- Anaerobic digestion of the stillage gives lower GGE, due to the use of combined heat and power; *ie* the use of waste heat from power generation for the fermentation. A similar conclusion applies to the combustion of WDG for electricity generation.

• All of the alternative technologies reduce the overall GGE, with the highest efficiency electricity generation case (with biogas combined cycle, or IDGCC) virtually offsetting the upstream GGEs for ethanol production.

Comparison with other LCA studies

In comparison with the other Australian studies on wheat production, similar GGEs and process water values were obtained, when compared on a similar basis. The values for resource energy, however, vary considerably (some of which may be attributed to different locations).

For ethanol production, comparison with other studies is complicated by uncertainties in how by-products have been credited, and in some cases by the use of petrol blends as the functional unit. In addition, many of the studies, incorrectly, do not consider the CO_2 sequestered by the grain through photosynthesis, as required by LCA methodology; this significantly reduces the GGE benefit of ethanol production from grain.

Comparison of ethanol and petrol

Using current technology, the life cycle GGEs for ethanol are always less than those for petrol, with ethanol cases involving exported electricity being very much lower. This benefit is likely to be greater in the future due to the potential use of CO_2 capture technologies in the ethanol plant and in power generation from stillage.

Most previous studies have compared ethanol and petrol on the basis of equivalent energy delivered - as fossil energy replacement. Most US studies (based on corn) have shown that, on a fossil fuel basis, the production of ethanol results in approximately 30% more energy than the fossil energy used in its production. The present study has shown similar results for the WDG case. DDGS results in a small negative net energy.

If DDGS were to be the likely by-product from ethanol production in Australia, then, from a resource energy perspective, ethanol production would not contribute to a reduction in the overall energy required for transport, when taking a life cycle approach.

For anaerobic digestion (with electricity generation using internal combustion engines) there is a marked improvement in net energy -2.5-3 times better than for WDG, or than for previous overseas studies.

Overall, ethanol production from grain gives significant resource energy and GGE benefits in comparison to petrol. The exception is for resource energy when DDGS is the by-product. Of course, a number of other issues also need to be taken into account, such as grain availability, acceptability, economics, *etc*.

Techno-economics

Because of the potential variations in key cost parameters, a matrix of values was used for grain price, electricity price/cost, and by-product credits. The findings are that:

- The techno-economic analysis shows the dominating role that the grain feedstock plays (50-80c/L of the ethanol production cost).
- The next most significant issue is the choice of stillage processing whether to produce WDG, DGGS, or biogas/solid fuel for electricity production. In practice, the choice of process will also depend on a number of interrelated factors capacities, the process route, by-product credits, and the ability to exploit opportunity biomass, such as straw.
- Sorghum gives lower unit feed cost, but overall production costs are similar due to lower credits (higher level of starch in the sorghum produces a higher yield of ethanol, but less electricity and fertiliser credits).

- The cost of ethanol production was 57-103 c/L for wheat, and 62-96 c/L for sorghum, depending on the combination of assumptions.
- The amount of power generated and exported is very dependent on the amount of stillage, the type of stillage processing, and the generation technology. For the alternative stillage processing options, the cost of ethanol production is lowest for AD-GTCC, due to its high efficiency and low capital cost (particularly for generation plant over 50 MW).

Production of WDG versus DDGS

An interesting question for the study was the trade-off between selling WDG directly, or drying the WDG to provide DDGS, as an animal feed. Drying would cost around \$37-61/t DDGS depending on energy costs, and, from a cost perspective, WDG can only be transported around 50-70 km before it is economically preferable to produce DDGS.

WDG, with its limited storage life, handling characteristics, significantly lower value, and reliance on local use, is likely to provide a lower co-product credit than the equivalent dried product. Overall, credits will depend on the marketability of the various products for the particular plant location.

Concluding comments

The variability of grain production in Australia, likely to increase with climate change, provides a strong driver for location of the ethanol plant adjacent to alternative sources of grain supply, *eg* imports or transfers from other regions of the country. This favours location at a port, as being planned by Primary Energy for plants at Kwinana, and Brisbane. The biodigestion of the stillage (thereby avoiding production of DDGS) avoids the issue of location, in the proximity of markets for the DDGS by-product.

From both the techno-economics, and the LCA results, it is apparent that biodigestion of the overall stillage has a number of important benefits:

- Reduces the net energy input to the ethanol plant.
- Generates excess electricity, and fertiliser credits, which exceed the credits which are associated with the sale of the DDGS.

A potential consequence for the feedlot industry is that the digester route does not produce any distillers grain; *ie* does not provide a feed component to partially replace the feed value of the original grain. However, the impact of diverting the WDG away from the feedlot industry may be alleviated to some extent by the potential for importing surplus distillers grain from the USA. At least in the short term, this is likely to be available at an attractive price compared to grain. However, it should also be noted that this surplus (and increasing costs of energy supplies) is now driving interest in the USA in anaerobic digestion of the stillage, which would be expected to impact on availability and price of DDGS for Australian import.

Finally, there is some doubt as to the long term availability of grain in Australia for conversion to liquid fuels at an economic price (lack of rainfall, competing uses for grain leading to price increases). There is also the developing technology for conversion of cellulose to ethanol, which is likely to shift the focus to the cheaper source of biomass. As the situation unfolds, and new regulatory environments develop, further techno-economic and LCA studies would be worth consideration.

2. BACKGROUND AND GLOBAL ETHANOL SCENE

Renewed interest in ethanol production and technology is very evident in many parts of the world. Figure 1 summarises the world production of ethanol (all grades) in 2005^[1].

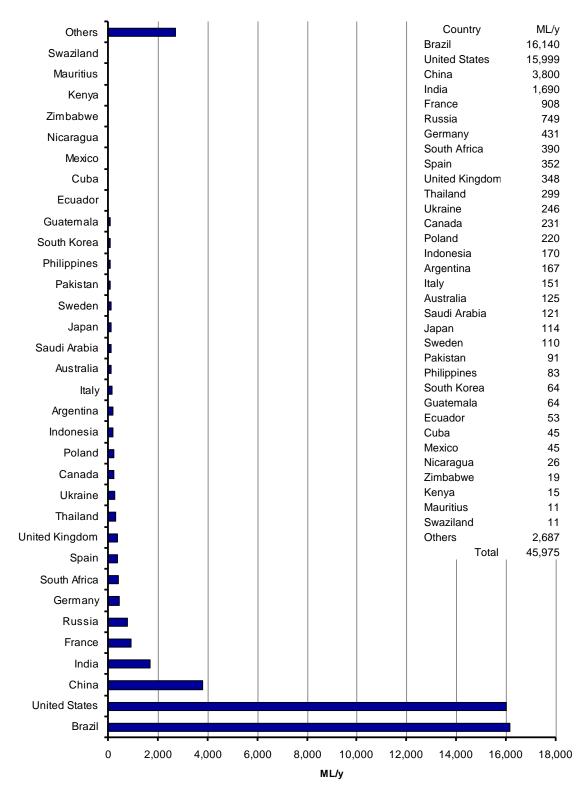


Figure 1 World production of ethanol (all grades)

The total world production of 46 GL/y is approximately equivalent to 140% of Australia's total petrol, on an energy content basis. Currently Brazil and the USA are the major

producers of ethanol, with Australia's total existing production capacity equivalent to one medium sized plant.

Rapid expansion in the world wide production of ethanol has occurred over the past 2 to 3 years as a result of:

- Recent increases in the cost of crude oil and the current high petroleum prices.
- The desire to create less dependence on imported fuels and extend existing gasoline capacity.
- An increasing demand for more renewable fuels.
- Attempts to reduce greenhouse gas emissions.
- An attempt to reduce exhaust emissions and health risks.
- The phasing out of methyl tertiary butyl ether (MTBE) as an oxygenate additive for gasoline, coupled with the suitability of ethanol as a substitute for MTBE.
- The existence of government policies in some countries to promote the ethanol industry.

The current position, and some recent developments, in different countries are summarised briefly below. This enables Australia's current and planned ethanol industry to be placed in an international perspective. International developments impact on grain price, cost of imported ethanol, and the rate of technological progress.

2.1. United States

The current USA ethanol production capacity is 16 GL/y, with 97 plants now in operation. Twenty three plants, with a total additional production design capacity of 40 GL/y, are currently under construction, and one new or upgraded plant is being brought into service approximately every 10 days at the present time^[2]. With the current gasoline usage of about 600 GL/y, around 5% of the gasoline pool will be supplied by ethanol in the near future.

The majority of ethanol is produced from corn, mainly using the dry milling process (discussed later), with sorghum starting to make a small, but increasingly important, contribution outside the traditional corn belt, where water issues are becoming important.

While the low prices for corn have been an important driver for fuel ethanol production, there have been a number of government (Federal and State) support measures driving the rapid growth of the industry.

The USA currently uses ethanol blends containing 5.7%, 7.7% and 10% by volume ethanol, as well as an E85 blend (85% ethanol, 15% gasoline). Legislation is currently underway for an E20 blend. Ford, Chrysler and General Motors all produce Flexible Fuel Vehicles (FFVs), and there are now over 5 million FFVs in use. There are 650 E85 retail stations in the USA^[2].

Fuel ethanol expansion has been assisted greatly by the government subsidies which started 25 years ago, with an exemption from the Federal excise tax on gasoline, various state tax incentives, capital subsidies and loans. The most important incentive is the Federal tax credit that is valid until 2010, extended from the initial expiry date of 2007, and redefined by Congress in 2004 as the Volumetric Ethanol Excise Tax Credit (VEETC). This is currently US 52 cents/gal (Aust 19.55c/L) of pure ethanol, when used in a 10% blend with gasoline. Since January 1993, ethanol-gasoline blends, containing 7.7% or 5.7% ethanol (produced from renewable resources), have received a prorated exemption.

As well as Federal support, a number of individual State governments offer incentives for fuel ethanol production. Some of these incentives include: direct payments on a production (per gallon) basis, use in public fleets, additional fuel tax exemptions, market mandates, direct grants or low interest loans to assist funding of new plants, and credits against the producer's income tax liabilities^[3].

In 2005, Pimentel and Patzek^[4] estimated the total annual Federal and state subsidies for ethanol in the USA at more than US\$3billion.

The Energy Policy Act of 2005 includes numerous provisions for corn-to-ethanol and lignocellulosics-to-ethanol^[5,6]. Among the provisions, the Act:

- Establishes definitions for the renewable fuels program, including cellulosic biomass ethanol, waste-derived ethanol, renewable fuel, and small refineries.
- Sets a Renewable Fuels Standard (RFS), which provides for a phase-in for renewable fuel volumes over seven years--beginning with 4 billion gallons by 2006, and ending at 7.5 billion gallons in 2012. Refiners are allowed to use renewable fuels when, and where, they are most effective.
- Creates a cellulosic biomass ethanol program, which;
 - establishes a cellulosic biomass (apparently ethanol) program of 250 M gallons in 2013,
 - counts every gallon of cellulosic- or waste-derived ethanol as 2.5 gallons toward RFS requirements,
 - includes a loan guarantee program of \$250 M per facility,
 - creates a \$650 M loan guarantee program for cellulosic ethanol, and
 - creates \$550 M "Advanced Biofuels Technologies Program".
- Updates the small ethanol producer definition from 30 to 60 M gallons/year. This change allows the newer, larger farmer-owned plants access to the existing small ethanol producer tax credit (SEPTC). The Act creates a similar provision for small agri-biodiesel producers.
- Eliminates the oxygenate standard-but allows refiners who choose to continue using MTBE to do so as of August 2005, 25 States have banned MTBE.
- Exempts small refineries from the renewable fuels mandate for five years.
- Establishes a sugar-to-ethanol program, which creates a;
 - \$36 M program to convert sugar to ethanol in Hawaii, Florida, Louisiana, and Texas (the U.S. sugar cane growing states),
 - \$250 M loan guarantee program for sugar-to-ethanol facilities
 - \$50 M loan guarantee program for sugar cane-to-ethanol facilities.

In his State of the Union address to the US congress on January 29, 2006, President Bush reaffirmed his support by stating that "We will also fund additional research in cutting-edge methods of producing ethanol, not just from corn, but from wood chips, stalks, or switch grass".

2.2. Brazil

Until now, Brazil has been the world's largest producer of fuel ethanol, although continuing major expansion of the US industry means that this position will shortly be challenged. Brazil currently produces around 18 GL/y fuel ethanol, with production forecast to reach 26 GL/y in 2010. In contrast to the US, the Brazilian ethanol industry is based almost entirely on sugar cane feedstock. Ethanol produced from cane is less expensive than from grain, and hence Brazil is in a good position to capitalise on export markets for their product (exported 2.4 GL/y in 2004 to a variety of world markets, with the largest exports to India and the US).

Brazil has a favourable climate, plentiful land and rainfall, in the centre-south of the country, with 50,000 sugar cane growers and 346 mills and ethanol distilleries. However, forecasts for ethanol production are difficult due to uncertainties resulting from the variable weather (droughts can result in below average yields) together with the complication that sugar cane serves as a raw material for markets of sugar and ethanol (both local and export). A large number of plants are dual plants, and can switch easily between sugar and ethanol, based on relative prices.

Bagasse is used extensively for process energy, and provides surplus power for sale. Current sugar production uses more than 50 commercial cane varieties, and improved management practices have resulted in significant improvements in recent years. Between 1975 and 2000, sugarcane yields per hectare increased by 33%, sugar content of cane by 8%, ethanol yield from sugar by 14%, and there were major increases in ethanol fermentation productivity.

Ethanol is distributed through 160 operating distributors and 32,030 petrol stations (92% of the total stations). Flex-fuel vehicles were first introduced in 2003, with 31 new models and 7 automakers now in operation. These vehicles can use blends of petrol and neat ethanol, from 0 to 100%. Today, Flex-fuel vehicles account for 73% of light vehicle sales in Brazil^[7].

As with the US, government policies and incentives in Brazil have assisted in establishing the ethanol business. In the mid-1970s, Brazil launched the National Fuel Alcohol Program, or Proálcool (the world's first major program for the production of renewable fuels), with the objective of increasing the share of domestically produced fuels in the country's fuel pool. The program employed various forms of support, and has been extremely successful.

High petrol prices in recent years, and the new generation of flex-fuel vehicles, have solidified the Brazilian consumers' preference for lower cost ethanol fuels. Of the flex-fuel vehicles (also called "hybrids"), VW has the lead over other manufacturers selling flex-fuel vehicles in Brazil.

Vehicles that ran solely on 100% ethanol fell out of favour in the 1990s, because of an alcohol shortage. The ethanol market became liberalised between 1997 and 1999, when guaranteed ethanol prices, distribution controls and financial incentives for new plants were gradually abolished.

State intervention is now restricted to provisions for ethanol blending (companies have to add between 20% and 25% to fossil petrol, depending on situation and markets) and minor tax reductions for ethanol storage and use of strategic reserves (value-added tax, and fuel and other taxes, are about 50% of that applied to petrol).

Tokgoz and Elobeid have reported^[8] that the indicative cost of ethanol from sugar cane in Brazil (without subsidies), at US\$0.83 per gallon (Aust 31.3c/L), is lower than the cost of production from corn in the US^[9], at US\$1.09 per gallon (Aust 41c/L). Whilst the absolute costs of production will depend on many factors, these figures, together with the high costs in the US of transporting ethanol supplies from the Midwest to major population areas, has led to an increase in competitiveness of Brazilian imports, despite the steep tariffs.

With the likely ethanol and sugar prices remaining competitive in the near future, Brazil is expected to continue to increase sugar cane production for both of these commodities. The country has enough land to easily double sugar cane harvested. In terms of ethanol, production is expected to double by $2015-16^{[8]}$.

2.3. Canada

Canada currently produces a relatively small volume of ethanol (≈ 250 ML in 2004equivalent to 0.7% of the country's petrol consumption). Assuming the government's target for future fuels is reached, production would need to increase to 1.4 GL in 2007^[3]. The logen Corporation operates a demonstration plant in Ottawa to produce ethanol from straw, although commercial quantities are not produced. Iogen is currently looking to attract C\$400 M for a full scale production plant to use 700,000 t/y of straw, and other agricultural wastes, to produce 220 GL/y of ethanol. It was claimed (in 2005) that ethanol can currently be produced from the straw for C40c/L, but logen want to reduce this to C32c/L eventually^[10].

Under its Climate Change plan (part of the response to meeting its Kyoto commitments on greenhouse gas abatement), the Federal government established a target (by 2010) of having 35% of the national fuel supply provided by E10, together with 500 ML of biodiesel produced and consumed. Up to C\$118 M has been provided in repayable contributions to 11 projects across the country, which, in combination with existing production, will allow Canada to meet its climate change target for ethanol 2 years earlier^[9]. A fuel excise tax exemption of US\$0.10/L on fuel ethanol blended with gasoline is provided by the Federal government.

In addition to the Federal government initiatives, several Canadian Provincial governments (including British Columbia, Alberta, Saskatchewan, Manitoba, Ontario and Quebec) offer various road tax exemptions for ethanol-based fuel blends. Saskatchewan, Manitoba and Ontario also apply mandatory blending rates.

2.4. China

China is the third largest producer of ethanol with some 1.5 GL of fuel ethanol generated in 2004, with production expected to increase to around 2.5 GL by 2010^[3]. The majority of ethanol is produced from grain (largest plant is in the Northeast, with a current capacity of 375 ML/y), with about 10% from sugar cane and 6% from paper pulp waste. Feedstock priority is afforded to biofuel producers from the State grain reserves at competitive prices.

Surplus grain stockpiled in the 1990s, together with the rapidly growing demand for transport fuels and a desire to reduce air pollution, resulted in China launching a fuel ethanol program in 2000. Fuel ethanol is exempt from the 5% consumption tax and 17% value-added tax.

A number of provinces use 10% ethanol fuel blends exclusively throughout their whole area, while some use E10 blends in part.

Expansion of the Chinese ethanol industry will be challenged by the need to conserve grain supplies for food security, and sugar shortages have deferred potential expansion in ethanol production from this source.

2.5. India

India is the fourth largest producer of ethanol, with a capacity in 2004 of \sim 2.7 GL, although only \sim 1.7 GL was produced, and \sim 100 ML were blended with petrol. Based on

the current ethanol fuel program, it is anticipated that ~1.5 GL will be produced^[3,9,11] in 2010.

The industry has developed from a pilot program launched in 2001 by the Indian government, to examine the feasibility of blending ethanol with gasoline to absorb surplus sugar. The sale of E5 (5% blend of ethanol with gasoline) was approved by the government in 2002, and mandated in a number of states and territories from 1 January 2003. Currently, E10 blends are used in 10 larger producing States and three contiguous Union Territories. The government introduced an excise duty exemption of Rs0.75/L for ethanol sales in February 2003. Additional fiscal measures have been introduced in some States to encourage local ethanol production.

As a result of a drought in 2003-2005, sugar crops and molasses output were significantly reduced, and ethanol feedstock prices escalated to a point where ethanol production in the Southern States was channelled to the industrial and potable alcohol sector. As a result, the ethanol blending obligation was suspended in late 2004. However, with the recovery of sugar cane production, ethanol production is being re-established.

The major expansion in ethanol production is reported to be taking place in Uttar Pradesh, Maharashtra and Tamil Nadu, the key sugar producing states, and will use mainly cane sugar molasses as a feedstock.

2.6. European Union

Total production of ethanol from the EU (in 2004) was 526 ML, with the major production coming from Spain (254 ML), France (102 ML), Sweden (71 ML) and Poland^[3,1]. Three major plants, having a combined capacity of 600 ML/y, have recently started operating in Germany (2004 production of 25 ML). Minor volumes of ethanol are produced in the Netherlands, Latvia, Lithuania and Italy. New plants in the United Kingdom, Belgium and Austria are due for commissioning, or are currently being planned. Fuel ethanol in the EU is largely overshadowed by the increasing biodiesel market. In 2004, biodiesel production was close to 2.2 GL, with the biggest producer being Germany (1.15 GL in 2004), followed by France (387 ML) and Italy (356 ML).

Two major biofuel directives were adopted by the European Commission in 2003:

- The "promotional" directive (Directive 2003/30/EC) required Member States to achieve a 2% share of renewable fuels (pure biofuels, blended fuel or Ethyl Tertiary Butyl Ether (ETBE)) by the end of 2005, and a 5.5% share by the end of 2010.
- The Directive on the Taxation of Energy Products (Directive 2003/96/EC) allows Member States to exempt, in full or part, products that contain renewable substances (bioethanol or biodiesel).

As well as these two Directives, the Reform of the EU Common Agricultural Policy (June 2003) maintained/introduced financial support for farmers growing energy crops as feed stocks for biofuels production. This Policy includes a carbon credit payment^[3] of EUR45 per hectare for land producing "energy crops" that are processed to fuel or gas (provided that a contract is concluded with the processor).

It appears that, based on Member State submissions to the European Commission (2005), the EU will only have reached a 1.4% share of renewable fuels by the end of 2005 (compared to the target of 2%).

A "Biomass and Biofuels Action Plan" published by the European Commission in December 2005, together with information contained in a communication on biofuels

published in February 2006, aims to increase the use of renewable energy sources. The Commission estimates that about 150 Mt of biomass based, oil equivalent fuels will be produced by 2010, compared to 69 Mt in 2003.

A more detailed analysis of the various developments, and specific taxation regimes for individual countries within the EU, has been presented by Agra^[3].

2.7. Thailand

Since 2002, the Thai government has supported the establishment of a large scale fuel bioethanol industry based on cassava, sugar cane and rice as preferred feed material, as a result of concerns over rising oil costs and the desire to replace MTBE^[3]. To encourage the development of an E10 fuel mix, the government has announced it will waive excise tax, contribute to the State Oil Fund and Energy Conservation Fund, provide investment concessions for new plants, allow duty concessions on imported machinery, and give an eight year corporate tax holiday to ethanol production.

2.8. Russia

Russia recently confirmed plans^[12] to build its first ethanol plant, to be located in Mikhailovka in the Volgograd region (a major grain growing area). The plant will produce 300,000t/y of ethanol from 900,000t/y of grain, and is anticipated to cost US\$200-250 M. Work will begin in spring 2007 (to be completed in 2 years).

Three local companies have formed a consortium to fund 40% of the project, with the remainder coming from loans. The opportunity to take advantage of high oil and gas prices, together with the rising demand for renewable fuels and an alternative outlet for the region's wheat production, are cited as the main reasons for the development.

The majority of the ethanol is likely to be exported, as a result of the existing tax arrangements in Russia, since local consumption is discouraged by high taxes.

The co-product of distillers grain is planned to be consumed by some 12 huge pig farms to be established in the area.

2.9. Japan

After the US, Japan is the largest consumer of gasoline, and the Japanese government has allowed the sale of gasoline containing a 3% ethanol blend (E3, made from sugar cane, soybeans, wheat and other grains) since August 2003. Concerns over higher NOx emissions and health concerns, as well as costs, have resulted in little apparent progress with this objective. Under the Kyoto Greenhouse Gas Initiative, the Japanese "Kyoto Protocol Target Achievement Plan" includes a goal to use 500 ML fuel derived from biomass in transport fuels by 2010.

To achieve this aim, it has planned to increase domestic ethanol production in stages, and is promoting the development of ethanol technologies and demonstration plants using waste biomass and energy crops.

The Petroleum Association of Japan (PAJ) is suggesting the use of a 7% ethyl tertiary butyl ether (bio-ETBE-made by compounding ethanol and isobutane) blend with gasoline as an alternative to ethanol, with the aim of a voluntary target of 20% of the total gasoline demand by $2010^{[13,14]}$. It has been claimed that gasoline blended with ETBE would require less investment than direct ethanol injection into gasoline, and could use idle MTBE facilities (ceased production in 2000 and 2001 due to health and environmental concerns).

Whether Japan will import ethanol or ETBE is yet to be determined, although the PAJ appears to favour the ETBE route. At the earliest, procurement of these imports is not likely to commence until at least 2008.

2.10. Australia

The existing production capacity for ethanol in Australia is ~ 155 ML/y (see Table 1), although the actual production (2005-2006) was ~ 105 ML (fuel and industrial use) due to limitations in market demand. Contract commitments for ethanol for blending with petrol are only 21 ML.

Plant/location	Production capacity, ML/y	Feed material	Product mix
Manildra, Nowra NSW	90	Starch plant by-products, wheat, sorghum, rice	E10, industrial
CSR Sarina sugar mill, Qld	55	Molasses	E10
Rocky Point sugar mill, Qld	10	Molasses	E10
Total	155		

Table 1 Current operating ethanol plants in Australia

Table 1 and Table 2 summarise details of the Australian operating and planned ethanol plants. A number of other potential plants have been foreshadowed in recent years, and some additional plants to those listed in Table 2 may be in the process of evaluation, as the overall ethanol market develops^[15].

In 2000, for biofuels, the Federal government waived the fuel excise tax payable on petrol and diesel (38c/L), and in September 2001, the Coalition election policy outlined their policy for "Biofuels for Cleaner Transport". In September 2002, the government ended the fuel excise exemption, and replaced it with an ethanol production subsidy at the same rate for one year. The Federal government legislated in April 2003 to restrict ethanol blended in gasoline to 10%, and it came into law on 1 July 2003.

On 25 July 2003, the government announced its intention to provide one-off capital grants (administered by Invest Australia) up to \$A37.6 M for Australian projects that provide new or expanded biofuel capacity. On 1 April 2004, the senate deferred the introduction of phasing in of the subsidy until 1 July 2011. From 1 July 2011 to 1 July 2015, this support will be reduced through the phasing in of an excise tax for alternative fuels (including biofuels), resulting in an excise of 12.5c/L payable in 2015. This is a 50% discount on the normal excise of 25c/L for mid energy content fuels (ethanol inter alia).

The Federal Government's Biofuels Task Force report, released in September 2005, recommended a target use of 350 ML/y by 2010 (biofuels-ethanol plus biodiesel). The initial less than enthusiastic response from oil companies, together with market resistance, meant that the government would struggle to see this achieved. As a result of the Prime Minister calling a meeting with oil company representatives in September 2005, voluntary commitments to take up and use 89-124 ML in 2006 (increasing to 403-523 ML by 2010) were obtained, and a Biofuels Action Plan agreed from the major oil companies. To date (June 2006), it appears that contract ethanol commitments of only 21 ML have been made.

In conjunction with the industry-government partnership established through the development of the Action Plan, together with the 10% cap on ethanol blends and the

37.6 M Capital Grants program, the government released a number of other initiatives^[16,17] to support the partnerships. These initiatives include:

- Use of E10 blends by the Commonwealth vehicle fleet.
- Simplification of the ethanol label, increasing the number of fuel quality compliance inspections to ensure motorists receive high quality fuel that is safe for their vehicles.
- Vehicle testing of E5 and E10 blends.
- Consideration of minor specification changes to help encourage development of biofuels.
- Working with Federal Chamber of Automotive Industries to ensure accurate information about compatibility of vehicles with ethanol.

The Government will monitor and review progress on a six-monthly basis.

Plant/location	Production Feed material capacity(ML/y) nominal rate		Reference
Dalby Bio-Refinery Ltd, Dalby Qld	80 (40 initially) Caltex and independents	Sorghum	[18,19]
Primary Energy Pty Ltd, Kwinana, WA	160 BP E10 fuel	Wheat 400,000 t/y	[18,20,21]
Primary Energy Pty Ltd, Gunnedah, NSW	80	Wheat and sorghum 200,000 t/y	[18,22,23]
Primary Energy Pty Ltd, Brisbane (Pinkenba), Qld	160	Wheat, sorghum and barley 400,000 t/y	[24,25]
Australian Ethanol, Swan Hill, Vic.	Blend for transport fuel	Barley, corn, wheat, sorghum 300,000 t/y	[18,26,27]
Bundaberg Sugar	10-14 E10 domestic market	Cane juice and molasses	[18,28]
Lemon Tree Ethanol Pty Ltd, Milmerran, Qld	60 E10	Cereal grains	[18,29]
Grainol, Kwinana, WA	190	Wheat and barley 500,000 t/y	[30]
Babcock and Brown, Rockdale Beef Feedlot, Yanco, NSW	150 Australian transport fuels market		[31,32]
Downs Fuels Farmers Pty Ltd, Darling Downs, Qld	80 (initially) 160 (later)	Sorghum (mostly) 200,000 t/y (initially)	[33]

Table 2 Proposed ethanol plants for Australia

3. ETHANOL PRODUCTION TECHNOLOGY

3.1. Overall process

Although ethanol is generally produced by the fermentation of sugars, the process of saccharification (conversion of starch to sugar) has provided the basis for an ever increasing, cost effective production of bioethanol, for use in blending with gasoline fuel, from a wide range of grains, including corn, wheat, sorghum, barley, rice and others.

The longer term potential of converting cellulose and hemi cellulose from straw, stalks, grasses and waste material to ethanol, whilst currently technically feasible, needs to be demonstrated at commercial scales of operation with reduced capital and operating costs. While the primary focus of this report is on the use of grains as feedstock, a brief summary of developments in the cellulose technology route are also presented, since this development could free up supplies of grain for other uses in the longer term.

The basic chemical conversion of starch to ethanol is represented by:

 $\begin{array}{ccc} \text{Starch from grain} & \rightarrow & C_6O_6H_{12} & \rightarrow & 2C_2H_5OH \,+\, 2CO_2 \\ & (\text{enzyme}) & (\text{yeast}) \end{array}$

Although an alternative wet milling process is available, this report will focus on the dry milling process, as this represents the currently favoured route. In the USA, dry milling plants have been constructed almost exclusively over the past 15 years, due to the limited market potential for the range of co-products produced from the wet milling option. Some brief additional comments about the wet milling option are included later. An example of this technology is shown in Figure 2.



Figure 2 Badger State Ethanol Plant at Monroe, Wisconsin, USA (190 ML/y)^[34] Figure 3 shows a typical flowsheet for the basic dry milling grain to ethanol process.

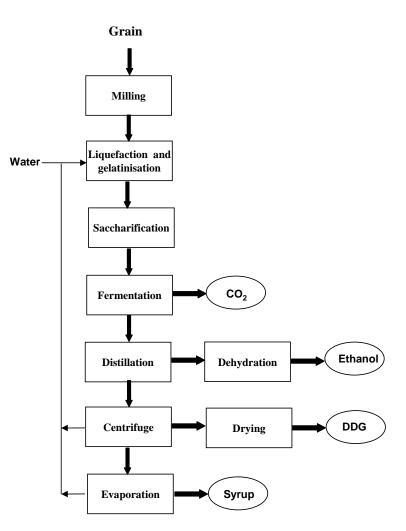


Figure 3 Basic dry milling ethanol process

3.2. Process steps

The individual process steps in the above diagram are discussed briefly below.

3.2.1 Grain grinding and slurry preparation

The feed grain is mechanically ground in a hammer mill to a coarse meal or flour, typically to a size of 0.25mm to 0.85mm. The choice of particle size can affect the later processing, and is chosen to allow water access to the starch inside the grain.

3.2.2 Gelatinisation

After making a slurry with warm water to a concentration that optimises water uptake and viscosity, the mixture (mash) is cooked with steam at a temperature of between 80 and 100°C, to assist in gelatinising (hydrolysing and swelling) the starch into solution^[35]. Grain type has a significant effect on processing, and the size distribution and cook temperatures are chosen to produce optimum conditions. If the slurry is too hot, it can generate a high viscosity, and, if too cold, longer processing residence times are necessary.

This heating process also sterilises the mash. Typically, a small amount of thin stillage from the bottom of the beer still is recycled to the slurry to acidify the mixture to a pH of 4.8 - 5.2 (for corn), and encourage optimum enzyme activity.

3.2.3 Saccharification

An alpha amylase enzyme is added to convert the starch into dextrin sugars (saccharification). The mash is then cooled to around 60°C, to achieve a suitable reaction rate whilst avoiding undesirable side reactions and reduced ethanol yields^[36]. After cooling, a glucoamylase enzyme is added to make the sugars more readily available for the yeast reaction.

3.2.4 Fermentation

The mash is further cooled to around 32°C to enable the yeast to grow and multiply during the fermentation process, which takes place over a period of 36-72 hours. Longer times are likely to increase the risk of infection by undesirable organisms and shorter times allow higher productivity. Ongoing research is aimed at minimising fermentation times and some operators have reported fermentation times of 23 hours. In the majority of ethanol plants, the fermentation process, and to allow sterilisation between batches. It is noted that the Manildra plant in Nowra utilises a multi-stage continuous fermentation process, and sterility is controlled by monitoring lactic acid and other critical components, and making adjustments to maintain an appropriate level of control over the various reactions that may take place^[37]. Fresh yeast is prepared separately, and introduced at the beginning of each batch (or as required in the continuous process).

The fermentation tanks are agitated and the slurry circulated through external heat exchangers, to maintain optimum temperature during fermentation and to remove the heat generated from the yeast reaction. Various additives are used to control foaming during fermentation, and buffers, nitrogen sources and minerals are utilised to produce the optimum yeast properties and maximise ethanol output from the fermentation broth.

3.2.5 Distillation

Once fermentation is complete, the fermentation mash (beer) is stored in a beer-well before transfer to the distillation stage, and the fermentation tanks cleaned for the next batch. The beer contains about 6-12% ethanol, together with all of the solids from the original feedstock and from the added yeast. The beer is continuously pumped to a multistage distillation unit which produces an overhead stream containing >90% ethanol with water.

3.2.6 Dehydration

Ethanol and water cannot be separated to produce 100% ethanol by simple distillation, as the mixture forms an azeotrope containing 95% ethanol. Removal of the water in the azeotropic mixture is achieved (in some of the older plants) by azeotropic distillation using an azeotropic breaking solvent (such as benzene), or more generally using vapour phase dehydration with molecular sieves. The molecular sieve adsorbs the ethanol while allowing the water to pass through. When the adsorber bed is saturated, the feed is switched to a parallel adsorber, and the ethanol desorbed to yield an almost pure anhydrous ethanol product. Typically, three adsorbers are used.

3.2.7 CO₂ recovery

Carbon dioxide produced in the fermentation is collected, scrubbed to remove any ethanol, and recovered as a by-product in some operations (for example to produce dry ice pellets for use in dry ice blasting, as a clean alternative means of sand blasting).

3.2.8 Solids separation

After distillation and dehydration, the residual liquid (whole stillage), containing all the insoluble material, soluble non-starch components and the yeast which has grown during fermentation, is pumped to a mechanical separation step or solid bowl decanter centrifuge to recover most of the solids. The typical product from a decanter centrifuge (Wet Distillers Grain-WDG) contains ~30-35% solids. A large proportion of the underflow from the centrifuge (thin stillage) is recycled to the front end of the process to minimise water usage, with the remainder concentrated by multiple effect evaporation to recover water for recycle. In some ethanol plants, all or part of the thin stillage is used for irrigation of adjacent farming operations.

The concentrated syrup product (sometimes called Condensed Distillers Solubles, CDS) typically contains ~30-35% solids, and is either blended with the WDG or sold separately as a high fat animal food. The product containing the syrup is marketed as wet distillers grain with solubles (wet cake or WDGS).

3.2.9 Drying

WDG is commonly sold to local feedlots and dairies. However, it only has a shelf life of around 3 days, and direct usage is usually restricted to feedlots within close proximity to the plant. Alternatively, the wet product (usually including the syrup) is dried to yield a product containing ~10% moisture (Dried Distillers Grain with Solubles-DDGS). This product is easily transported and can be readily stored for long periods.



Figure 4 DDGS in storage at a US ethanol plant (Mid-Missouri Energy, Malta Bend)^[34]

Some early dryers resulted in thermal damage to the product, and inconsistent quality, odour and texture, from uneven temperatures and overheating. Modern dryers generally allow a much more consistent product to be generated. Two main types of dryers have been used: the rotary dryer and the ring dryer (often called flash and ring dryers). Approximately 85% of ethanol plants currently use rotary dryers.

Rotary dryers utilize either steam tubes or direct fired heating, and ring dryers use direct fired heating with large volumes of air. Typically, steam dryers use 1kg of steam to remove between 0.6 and 0.7 kg of water, with some economies resulting from recycling. In direct fired systems, 2.8-3.1 MJ of energy is utilised to remove 1 kg of water.

The conventional, direct fired, rotary dryer has an inlet air temperature of 300-650°C, with an outlet temperature of around 98°C, and is run in co-current mode, *ie* the hottest gases are in contact with the wettest solids. Rapid evaporation occurs as a result of the fine particle sizes and convective heat transfer. The high evaporation of water also results in cooling of the grain, and minimises degradation of the protein and other nutrients. The dried product migrates to the outlet of the drum, due to the movement of the heated air.

Once discharged from the dryer, the product is separated from the air flow by cyclones. The exhaust gas either exits the plant directly, or is treated in either a wet gas scrubber or thermal oxidiser, to remove residual organics (and eliminate odours).

A proportion of the dried product is commonly recycled back to the inlet and mixed with wet feed to maintain a more uniform condition in the dryer, and assist with additional conductive heat transfer.

Although the ring dryer has many similar features to the rotary kiln, the drum does not rotate and the material is conveyed through the dryer pneumatically, with large amounts of air at velocities high enough to induce centrifugal forces on the particles. This centrifugal action separates the dried material from the wetter product, which tends to migrate toward the outer wall of the ductwork as the drier, lighter material migrates toward the inner wall. Dried product is discharged through an opening in the ductwork, where it is separated and collected in the cyclones.

Handling and storage of the product is important, as spontaneous combustion can occur in bulk piles if the material is too hot. Consequently, most plants cool the DDGS with ambient air before storage. Fine dried residue can sometimes form small balls when the material comes in contact with sticky recycled syrup.

3.3. Plant Capacities

Ethanol plant capacities have gradually increased over the years as demand has increased, and as pressures to reduce operating costs have been placed on the industry. In the 1980s, US plants typically produced 80 kL/y to 25 ML/y. In 2005, 17 of the operating plants (87 in total) had a capacity less than 150 ML/y, with 23 plants having a capacity in the vicinity of 200 ML/y. Seven plants with capacities greater than 380 ML/y were in operation^[2]. A 100 ML/y US plant typically employs 32 workers, whereas a 380 ML/y plant can operate with only 45 employees^[38].

Initial development proposals for new Australian plants were based on plants having a capacity around 80 ML/y. However, more recent proposals have moved toward larger capacities (160 ML/y) to achieve more attractive financial outcomes based on economies of scale.

3.4. Plant capital cost

Plant capital cost data is difficult to obtain for Australia due to lack of recent completed ethanol projects. Nominal cost data has been estimated for an Australian plant with DDGS as by-product, using a number of industry sources – a rule of thumb is that the capital cost is A 1.0 M/ML annual capacity.

For the biodigestion of stillage option, the costs of the digester and associated plant is probably offset substantially by the removal of the evaporator, dryer and separation equipment for DDGS production.

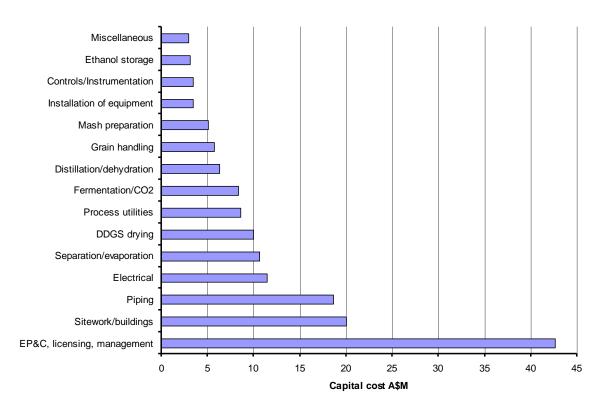


Figure 5 Breakdown of capital cost for ethanol plant with anaerobic digestion

4. GRAIN AND PROCESS PARAMETERS

Whilst the primary feedstock for ethanol production in Brazil is sugar cane, and in the USA corn, the feedstock for the major proportion of ethanol production over the next decade in Australia will be a variety of grains, with a small proportion from sugar cane by-products (primarily molasses). The requirements for feed grains, and the associated ethanol and by-product yields are given below. Some comments on energy and water consumption are also provided.

4.1. Grain requirements

The particular type of grain used will depend on many factors, including the plant location, cost and availability of grain, transportation costs and opportunity for maximising ethanol yields. While more details related to grain availability, location and cost are included in the other sections of this report, it is important to appreciate some of the technological issues that are affected by changing grain types, since this can have a significant effect on the plant design, as well as ethanol production yields and costs. These aspects are discussed below, and are essentially focussed on the dry milling production process as outlined earlier.

Grains, such as wheat, corn, barley, sorghum and other cereals, typically contain 55-70% starch, and various varieties have been adapted to yield high starch levels.

Table 3 summarises some indicative grain analyses for varieties grown in Australia[39,40,15]. These figures are meant to provide indicative numbers only, since wide variations (especially in starch) have been reported[41].

Component	Unit	Corn	Wheat	Barley	Sorghum
Moisture	% ar	12.0	10.0	12.0	12.0
Starch	% db	70.0	65.3	60.0	74.6
Protein	% db	9.5	13.0	10.0	8.0
Fibre	% db	11.5	9.0	10.2	10.0
Fat	% db	3.9	2.0	3.0	3.1
Ash	% db	1.6	2.5	2.5	1.0
Other solubles	% db	3.5	8.7	14.3	3.3

Table 3	Typical	orain	feedstock	analyses
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Note: Moisture levels have been modified to represent levels considered appropriate for Australian grains.

The grain feedstock typically contributes 60-70% of the overall ethanol production cost, and optimisation of both the feedstock and plant design are important aspects for any project. Ethanol plants can use sub-standard grains which may have been affected by adverse weather conditions, physical damage or contamination.

4.2. Ethanol yield

Ethanol yields are basically related to the available starch, together with the efficiency of fermentation and recovery of the ethanol. Whilst there is not necessarily a direct

quantifiable correlation between ethanol yield and starch content for the various grain types, or more particularly for mixed grain feeds^[42], it is reasonable in the current context to assume that the ethanol yield is directly proportional to starch content. An indicative practical yield is 620 L/t of starch, and Table 4 shows the relative difference in unit ethanol production (based on this figure) for the range of grains of current interest to Australian ethanol producers^[15,40,43]. These calculations show that a plant processing sorghum (with the higher starch level quoted) would produce approximately 24% more ethanol compared to the same quantity of barley, or an additional 12% compared to wheat. It is noted, however, that starch levels can vary significantly for grain produced in different areas and under varying seasonal conditions.

Parameter	Unit	Corn	Wheat	Barley	Sorghum
Moisture	% ar	12.0	10.0	12.0	12.0
Starch	% db	70.0	65.3	60.0	74.6
Ethanol yield	L/t grain	382	365	327	407
Grain to produce	t/160 ML	419,000	439,000	489,000	393,000
Wet distillers grain	t/160 ML	386,000	481,000	591,000	310,000
Dry distillers grain @10% moisture	t/160 ML	129,000	160,000	197,000	103,000

Table 4 Ethanol production for various grain feedstocks

The amount of distillers grain produced is inversely proportional to the ethanol yield, as expected.

4.3. Distillers grain yield

Variations in grain properties and processing will have an influence on the properties and yields of wet and dry distillers grain. Indicative yields for both wet distillers grain (30% solids) and dry distillers grain (90% solids) for a 160ML/y ethanol plant are shown in Table 4. These figures have been estimated by assuming that all of the grain protein, fat, fibre, solubles and ash, together with 2% of the starch, report to the distillers grain.

There is some uncertainty about the role that the grain "solubles" play in determining ethanol and distillers grain yields for the various feedstocks. In the above estimates it has been assumed that all the solubles report to the distillers grain^[37]. Refinements to these estimates, based on operational experience and research for different grains, could result in minor changes to the absolute yields.

4.4. CO₂ generation

Fermentation of starch produces carbon dioxide (as shown in Equation1). Typically, the quantity of CO_2 produced is 498 kg/t of starch.

4.5. Water consumption

Water is a key component in the processing of grain to ethanol, with several process circulation loops used in a typical plant. The hydrolysis slurry feed concentration is similar for all types of grain, and therefore feeds richer in starch, such as sorghum, require less water than grains with lower starch (such as barley). The consequence of this process parameter is that plants using sorghum as a primary feedstock require less process volume (and less power) than those processing the poorer starch grains (with subsequent savings in both operational and capital costs). Plants designed for mixed or variable feedstocks need to utilise a conservative process flowsheet, and hence would be based on the higher water utilisation requirement.

The plant uses water for cooling to control fermentation temperatures, for boiler blowdown and other process steps, as well as water makeup for that lost in the WDG. Where DDG is produced, this water is normally lost to atmosphere, unless an advanced drying process is used.

Total consumption ranges from 1-3 m^3/kL of ethanol depending on the process.

4.6. Energy consumption

Process energy and electricity typically account for approximately 10-20% of the operational cost for a bioethanol plant^[38]. This cost is affected largely by the availability and cost of the energy source. For new plants, ICM give natural gas consumption of 10 MJ/L ethanol. The ICM process is approximately 3 MJ/L less, without the dryer (*ie* when WDG is produced).

5. NEW DEVELOPMENTS AND POTENTIAL TECHNOLOGICAL IMPROVEMENTS

In the past, the viability of bioethanol plants was seriously threatened by the fall in oil prices, and the cyclical increases in the price of feedstocks brought about by demands in other areas. Consequently, there has been a continual attempt to improve the biological efficiency of ethanol production, and to characterise the properties and identify cost-effective markets for the co-products. At the same time, improvements in the performance of the various unit operations aimed at reducing capital equipment cost have made significant contributions.

In the US industry, ethanol yields in the 1980s were typically around 340 L/t (for corn feedstock), with production costs around A95c/L. Technological advances and refinements have resulted in typical current yields of up to 420 L/t, with a production cost of approximately A50c/L.

To some extent, the current boom in ethanol demand, coupled with taxation relief policies and unprecedented high fuel prices, has resulted in high rates of return (typically 3 years in the USA), and has delayed the impetus to adopt new technologies. However, research and development work will continue to play an important part in improving the technology and range of co-products for future ethanol plants.

Some of the technological improvements that have been demonstrated, foreshadowed, or are under development are briefly summarised below.

5.1. Liquefaction, saccharification and fermentation

Industrial enzymes were first introduced into ethanol production in the 1950s. Since then, major improvements have led to significant advances both in performance and reduced costs. Ongoing research and development is continually offering new options for improvements.

The new generation of alpha amylases used to break down the starch do not require the addition of lime (as originally used) to stabilise the enzyme and tolerate lower pH, so that a higher proportion of thin stillage can be recycled. These enzymes also reduce the mash viscosity (leading to improved fermentation rates) and reduced calcium oxalate production^[44]. Improved enzyme performance and cost of production have reduced the unit cost of enzymes by as much as 75%. Improved enzymes that allow reduced mash viscosities have allowed higher dry solids concentrations (increased from 35% to 38-40%) and, as noted above, have reduced the amount of water (per tonne of feed grain) that needs to be heated in the cooking process. It has been estimated that for a 150 ML/y ethanol plant, approximately 15 tonnes per day of steam would be saved by using the higher concentrations^[44].

Wheat, rye and barley contain non-starch polysaccharides (grain cell walls), and these create a gel complex when in contact with water, resulting in a very high viscosity. Enzyme research has permitted the development of a product range that optimises the activities and performance for different grains without creating viscosity problems^[41].

Similar improvements in glucoamylase and protease enzymes (required with some grains to release the starch bound in the protein matrix) enable multiple grain feedstocks to be processed by utilising the appropriate enzyme mix, resulting in optimum ethanol productivity.

Although significant progress has been made in the development of thermotolerant yeasts, fermentation is currently limited to temperatures below 38° C. The primary driving force for higher fermentation temperature is to increase the rate of fermentation, while a number of process modifications would be required to accommodate higher reaction rates (such as increased rates of cooling and enhanced CO₂ scrubbing).

The production of glycerol during fermentation can occur when various dissolved salts are present due to osmotic or chemical stress, resulting in a lower ethanol yield. Extension of present research with yeasts, produced using techniques such as "metabolic flux engineering", could lead to improved commercial practices.

Combined saccharification and fermentation (simultaneous saccharification and fermentation (SSF)) is a batch system which improves the kinetics of saccharification by removing (fermenting) the glucose as fast as it is formed. In continuous fermentation processes, where there is continuous dilution of the high glucose feed in the first-stage fermenter, saccharification to high glucose levels helps reduce fermentation time. However, in batch fermentations, osmotic shock created by high glucose concentrations can stress the yeast. SSF improves ethanol yields and accelerates ethanol production, thereby reducing the potential for bacterial growth in the fermenter.

Incorporation of yeast propagation with the SSF combination has been included in some plant designs (known as the Simultaneous Saccharification, Yeast Propagation and Fermentation Process (SSYPF)) with the objective of increasing yeast contact time and reducing bacterial growth^[44]. These processes also reduce the storage and handling of large stocks of yeast.

Raw starch hydrolysis (cold cook process) represents a new process that enables the conversion of starch to fermentables, without the cooking component. This has been made possible by the development of some innovative low temperature alpha-amylase and glucoamylase enzymes. Whilst a number of companies have unveiled various versions of this process, the combined efforts of Broin and Novozymes (BPX process) over several years has been reported to have resulted in the successful implementation of the technology in twelve Broin-managed dry milling facilities, having a total ethanol production of almost 2.3 GL/y^[41,45,46]. It is claimed that this route to ethanol reduces energy costs by 8-15%, provides additional starch accessibility for conversion, results in higher ethanol yields and increased nutrient quality in feed co-products, and lowers the capital costs for new plants. There are, however, some cost offsets through increased enzyme costs, and increased cleaning frequency and associated costs.

Processes such as Very High Gravity (VHG) fermentation (originally explored at the University of Saskatchewan), using highly concentrated mash with greater than 30% solids, have the potential to produce ethanol concentrations as high as 23% v/v. However, concentration levels as high as 23% have apparently only been achieved in the laboratory. Many major breweries throughout the world are said to be experimenting with VHG processes^[44].

5.2. Modifications to the front end of the dry milling process

A number of process modifications to the front end of the ethanol process have been investigated in an attempt to increase the variety and value of co-products, especially given the potential for oversupply of DDGS. Whilst this may not become a serious problem in Australia in the near term, it is useful to briefly review some of the new and developing options in this area. While detailed descriptions of individual flowsheets are outside the scope of this review, extensive publications are available by referring to Singh (University of Illinois, Urbana-Champaign).

5.2.1 Dry fractionation

The dry fractionation process^[41,47,48,49,50,51], effectively separates the grain into its main components; germ (oil), pericarp fibre, and endosperm (ethanol). This separation increases the value of co-products and reduces the amount of solids processed through the fermentation and distillation processes, thereby enabling a decrease in enzyme consumption, and a slight increase in the ethanol content of the mash (12-14%). These improvements reduce process energy consumption and potentially increase the capacity of the plant.

The reduced fibre (cellulose) content of the DDGS with dry fractionation makes the DDGS suitable as feed for swine, poultry, and fish.

Several variations on dry fractionation have been developed by various technology suppliers, including: Cereal Process Technologies, LLC (CPT based in Memphis, Tennessee); Ocrim SpA (based in Cremona, Italy); Applied Milling Systems (AMS based in Houston, Texas), Satake Corporation (based in Tokyo, Japan and also with a major division in Cheshire, England), Monsanto (based in St. Louis, Missouri), and the FWS Group (based in Winnepeg, Manitoba, Canada). Broin has an agreement to use technology developed in collaboration with Satake, while ICM is using AMS's dry fractionation technology. Dry fractionation is more appropriate for new plants to take full advantage of the potentially higher ethanol capacity.

The following typical yields of the various co-products from this process (for corn feedstock) have been presented by Locke^[41]; per tonne of corn, 380-410 L ethanol, 62 kg corn germ (35-40% oil), 69 kg corn fibre (60%-70% carbohydrates) and 140 kg modified DDGS. Other indicated advantages include improved yield of oil extraction from the germ, increased ethanol yield (435 L/t fibre) and, importantly, higher protein content in DDGS (from 28% to greater than 58%, with a significant increase in estimated value).

5.2.2 Modified dry grind processes.

Research into improved techniques on the front end of the dry grind process (using the addition of water), aimed at recovering germ, pericarp and endosperm fibre as co-products, has attracted significant interest in the USA. A number of these are briefly outlined below.

a) Quick Germ (QG) process

In this process, the grain is firstly soaked and ground in a degermination mill, and the germ is separated in a series of germ clones before being dried. The underflow from the cyclones is then further ground to produce a mash, which is processed using the usual dry grind ethanol route^[52]. Typically, 1 tonne of grain feed (corn/sorghum) produces 59 kg dried germ, 385 L ethanol and 208 kg DDGS. Potential advantages over the conventional process include the recovery of valuable germ, an increase in plant ethanol capacity, and an increase in the protein content of the DDGS.

b) Quick Germ Quick Fibre (QGQF process)

This process is somewhat similar to the QG process, except that, after soaking, both the germ and pericarp fibre are recovered from the germ clones, and the pericarp and germ are then separated, after drying, in an air separator. Again, the underflow from the germ clones is further ground before processing using the usual ethanol route^[53].

Typically, 1 tonne of grain feed (corn/sorghum) produces 73.4 kg fibre, 61.2 kg germ, 400 L ethanol and 143 kg DDGS. In this case, the recovery of coarse fibre as a valuable co-product is achieved, as well as an increase in the plant ethanol capacity, an increase in the protein content of the DDGS, and a reduction in the fibre content of the DDGS.

c) Enzymatic dry grind (E-Mill) process

After soaking, as in the above processes, the ground product is pumped to an incubation stage where enzymes are added. After further grinding, the germ and pericarp fibre are separated as in the QGQF process. An additional grinding step then allows the endosperm fibre to be separated prior to the processing of the residual material to ethanol and DDGS^[54]. The resultant ethanol concentration is higher (with increased plant ethanol capacity), protein content of DDGS is increased, fibre in the DDGS is very low, and germ, pericarp and endosperm fibre are recovered prior to ethanol processing. Typically 1 tonne of grain feed (corn/sorghum) produces 73 kg pericarp fibre, 61 kg germ, 73 kg endosperm fibre, 400 L ethanol and 69 kg stockfeed product.

5.2.3 Modifications to the back end of the dry grinding process

The Elusieve process^[55] utilises the conventional dry grind ethanol process flowsheet, but includes a sieving separation section to separate an enhanced heavier DDGS fraction from the lighter fibre. This process modification uses the conventional dry grinding process route up to the DDGS product, but separates an enhanced DDGS with higher protein and lower fibre content. The fibre can be used for recovery of higher value products (including corn fibre oil and corn fibre gum). Typically, 1 tonne of corn/sorghum grain feed produces 416 L ethanol and 277 kg DDGS. Srinivasan et al^[55] have indicated that a payback period of 1.2 to 2.2 years could be achieved for a 145 ML/y plant using the Elusieve process.

5.3. Other process technology advances

5.3.1 Anaerobic digestion of ethanol fermentation residues

In a typical dry grind ethanol process, the grain residue is recovered and sold either as wet distillers grain or subsequently dried and marketed as dry distillers grain.

In some locations and applications, significant interest in the anaerobic digestion of the residues is developing as a result of oversupplies of distillers grain, but also as a means of combating the significant (and increasing) operating costs of natural gas and electricity. Another driver is the potential greenhouse gas credits that can result from the generation of electricity from the methane produced by the digestion process. Anaerobic digestion also produces compost and fertiliser co-products that can provide additional income, albeit with additional capital costs for the overall plant.

In a variation of the above arrangement, some combined feedlot/ethanol plants utilise the animal manure from the feedlot in a digester to generate methane, and utilise the distillers grain as feed. If too much distillers grain is produced, it is then diverted to the digester to optimise the value and feed/solids balance^[56].

Anaerobic digestion to generate methane from manures and other organic feed materials has been utilised for many years, with many plants in operation throughout the world. In ethanol production, anaerobic digestion has been incorporated into a number of plants. Typically the stillage from the beer column is fed to one or more digesters, and the methane generated is used in a turbine to generate electricity and steam. The residue from the digester is processed in an ultrafilter, ammonia stripper and reverse osmosis plant to produce an organic fertiliser, nitrogen and phosphorus/potassium fertiliser concentrates, as well as potable water that can be recirculated to the ethanol plant^[57].

For a plant producing 150 ML ethanol (using 400,000 tonnes of grain feedstock), EnviroPlus have reported the following products from one of their biodigesters:

• 120 Mm³ biogas (or 200,000 MWh of green electricity)

- 150,000 tonnes of organic fertiliser
- 20,000 tonnes of ammonia
- 375,000 tonnes of CO_{2-e}
- RO quality water
- steam.

EnviroPlus state that the electricity generated allows the total plant to operate without any fossil fuel or electricity, which results in the revenue from ethanol alone being a smaller percentage of the total revenue (around 75% compared to at least 85% for a normal plant). In addition to the 40,000 MWh per year typically required for this size plant, some 160,000 MWh per year of electricity is reported to be available for export, and the 1,650 TJ per year natural gas requirement is eliminated. The additional cost for the plant containing the digester operation is estimated to be \$35 M (compared to the traditional plant cost of \$85 M). The additional \$35 M involves the installation of the power plant. Indicative revenue of \$100 M for the combined plant compares to the \$90 M for the traditional plant (EBITDA of \$36 M cf \$26 M, respectively).

5.3.2 Optimisation of water in wet distillers grain

Typically, the wet distillers grain is recovered from the beer column stillage in a solid bowl decanter centrifuge, to yield a product containing 30-35% solids. Developments in decanter centrifuge technology have been reported to produce material up to 40% solids. In addition, the use of an additional step involving a pressure dryer/filter could result in a solids concentration of up to 58%^[58]. This reduction in product water content could offer improvements in product handleability and value, as well as significant savings in the cost of drying. Alternatively, the drier product has potential as a feedstock for combustion to generate steam in the process.

5.3.3 Biomass gasification and alternative energy supplies

Anaerobic digestion (5.3.1) offers one option to reduce (or eliminate) the demand for natural gas). Other options that are being investigated or installed include biomass gasification (using wood waste, DDGS, wheat straw), methane from local coal seams, fluidised bed reactors (using waste syrup, and, in some cases, waste or cheap coal). In one US plant (Corn Plus in Winnebago, MN)^[59], the distillers grain dryer stack gases are recycled to the FBR which acts as a thermal oxidiser to reduce emissions. Other cogeneration technologies have the potential to impact on ethanol operating costs, and refinement of these in the future (to take advantage of local synergies and materials) will play an important role.

5.3.4 Biobutanol

Significant interest in developing processes and equipment for the production of biobutanol, as an alternative to ethanol, has recently $emerged^{[60,61]}$.

Butanol has a lower vapour pressure and a greater tolerance for water contamination in gasoline blends, thereby facilitating its use in existing gasoline distribution channels (notably pipelines where ethanol attracts water and results in corrosion). It is also claimed that butanol can be blended with gasoline at higher concentrations without the need to retrofit vehicles, and that it offers better economy than similar gasoline-ethanol blends.

BP has recently announced^[61] that it will invest \$500 M over ten years to establish a bioscience energy research laboratory to concentrate on research and development in the

bioscience sector related to the production of new, cleaner energy. A major part of this development involved extending its partnership with DuPont to develop, produce and market advanced transportation biofuels. The two groups have been working with British Sugar to convert a UK ethanol fermentation facility to produce *n*-butanol (termed *biobutanol*), with the product expected to come to market as a gasoline biocomponent in 2007.

Since both biobutanol and bioethanol have similar production routes and feedstocks, existing ethanol production facilities can be retrofitted. Feasibility studies for more production facilities are in progress, with initial feedstocks of sugar, maize, wheat, and cassava. Cellulosic materials from fast-growing energy crops are also being considered.

5.4. Lignocellulosic route to bioethanol

The long term production of bioethanol to meet increasing demands in many parts of the world cannot be achieved with grain or sugarcane based feedstocks alone, and major research and development programs over many years have sought to utilise a large variety of cellulosic materials as alternative feedstocks. Although a number of processes have been proposed, and to some extent demonstrated, to date, the additional processing and associated capital costs to generate a fermentable material have generally resulted in unacceptable production costs.

For over a century, the potential for producing ethanol from abundant lignocellulosic materials has been of great interest to many advocates of renewable biomass energy and ethanol fuels. By comparison with the grain/starch route to ethanol, lignocellulosic materials require pretreatment to generate the sugars that can be fermented to ethanol.

Potential lignocellulosic materials include wood, agricultural field crop residues (wheat straw, barley straw, bagasse), and grasses (switchgrass is a popular option in the USA^[62]). A range of nominal analyses^[63,64,65] for a selection of potential feedstocks are summarised in Table 5, noting that analyses can vary substantially between samples and locations.

	(wt%, dry basis)					
Component	Corn (kernels)	Corn stover	Wheat straw	Switch grass	Poplar (hardwood)	Pine (softwood)
Starch $(C_6H_{10}O_5)_n$	72.0	0.4	0.9	0.3	0	0.1
Sugar (C ₁₂ H ₂₂ O ₁₁)	2.0	0	0	0	0	0
Cellulose (C ₆ H ₁₀ O ₅) _n	4.2	37.3	45.2	39.9	42.7	63.5
Hemicellulose						
$(C_{5}H_{8}O_{4})_{n}$	6.3	22.7	18.9	22.2	19.8	4.6
$(C_6H_{10}O_5)_n$	0	1.4	0	0	4.2	0
Lignin	-	17.5	20.3	18.3	27.7	31.4
Other (protein, oil, extractives, acetate)	14.0	14.6	6.4	14.5	4.6	0.2
Ash	1.5	6.1	8.3	4.8	1.0	0.2
Carbon	45.7	43.7	43.2	46.7	48.5	52.5
Typical moisture wt%	15	15	15	50	50	50

Table 5 Analyses for a selection of potential lignocellulosic feedstocks

Note zeros in the table may simply mean that no values were reported for the particular components.

Lignocellulosic materials are made up of lignin (a very high molecular weight, tar-like polymeric material containing phenolic-propane units), cellulose (polymers of the C6 sugar glucose), and hemicellulose (polymers of both C5 and C6 sugars). Converting the cellulose and hemicellulose to ethanol requires first separating them from lignin ("pre-treatment"), then hydrolysing them to simple sugars, and finally fermenting the sugars to ethanol with suitable microorganisms - specifically, genetically modified yeasts or bacteria.

Numerous approaches have been examined for pre-treatment of the feedstock to remove lignin from cellulose. These can generally be categorised as follows (with some typical references):

- Mechanical such as milling, grinding, and other forms of comminution, such as rapid decompression ("steam explosion" or "ammonia explosion"^[66])
- Thermal using hot water, hot chemical solutions, or high pressure steam
- Chemical using acids or alkalis^[67]
- Organosolv using solvents, such as ethanol and acetone^[68,69]
- Combination processes-using two or more of the above (typical approach)

A number of government and private organizations associated with government funded research, enzyme and micro-organism developers, process engineering and plant design/construction firms, and process developers, are actively working towards commercialisation of these approaches.

Within the USA, the DOE/NREL (National Renewable Energy Laboratory) at Golden, Colorado have spent several hundred million dollars in lignocellulose to ethanol R&D - both in awards to industry, institutional and university contractors, as well as in-house R&D. Outside the USA, there appear to be relatively small ongoing R&D activities in this field in Canada, the European Union, Japan and some other countries.

In the area of cellulase enzymes, the two largest manufacturers in the world, Genencor International (Palo Alto, California), and Novozymes Inc. (Denmark and Davis, California) have benefitted from partnerships with the DOE/NREL, with Novozymes announcing in 2005 that they had reduced the cost of the cellulose enzyme for hydrolyzing corn-stover cellulose from more than US\$1.30 to 2.6-4.8 c/L.

Genencor is also working with Cargill Dow LLC to create advanced enzyme systems for a biomass project supported by the DOE^[70], and in May 2006 announced its participation in a 1.2 M euro research consortium to develop economic ethanol production from paper pulp through the use of know-how and infrastructure in the French forest products industry^[71].

A number of other biotech companies, including the Diversa Corporation (San Diego, California), Codexis Inc. (Redwood City, California), Athenix Corp. (Research Triangle Park, North Carolina) and the J. Craig Venter Institute (Rockville, Maryland) are undertaking research and development with cellulase enzymes.

Genetic engineering approaches to developing improved microorganisms for fermentation have been undertaken by various laboratories. Genetically modified microorganisms generally tend to be less robust than the conventional wild organisms, and in some cases lead to lower ethanol yields from glucose; hence some of the increased ethanol yields from the C5 sugars will be offset by the poorer yields from the C6 sugars. The ethanol concentration in lignocellulosic-to-ethanol fermentation beer may be limited to 3-5%, requiring significantly higher quantities of steam compared to the grain based option fermentation option (6-12%).

Some of the key lignocellulosic process developers are:

Iogen Corporation,	Based in Ottawa, Canada (reportedly using continuous dilute acid pre-treatment and enzyme hydrolysis of cellulose). A 3-4 ML/y pilot plant started operation in 2004, but is being operated at only 25% of this capacity. Iogen is currently looking to attract C\$400 M for a full scale production plant to use 700,000 t/y of straw and other agricultural wastes to produce 220GL/y of ethanol. It was claimed (in 2005) that ethanol can currently be produced from the straw at C40c/L, but that logen want to reduce this to C32c/L eventually ^[10] .
Swan Biomass Company	A spin off company from Amoco), near Chicago, Illinois (dilute acid pre-treatment followed by simultaneous saccharification and fermentation). Like Iogen, Swan Biomass carried out some pilot plant investigations at NREL's facilities in the 1990s, and have worked with molecular geneticists at Purdue University to produce genetically engineered yeasts that produce at least 30% more ethanol from plant material than the unmodified version of the yeast ^[72] . Although little recent information has been published, the company has been pursuing at least one major project – a possible US\$300 M sugar cane based ethanol facility in the Imperial Valley of Southern California, with a planned ethanol production of $300ML/y^{[73]}$.
Arkenol Fuels	Based in Irvine, California) has developed a concentrated sulphuric acid hydrolysis process, and claims that it will use

Based in Irvine, California) has developed a concentrated sulphuric acid hydrolysis process, and claims that it will use a "naturally occurring yeast" that can efficiently co-ferment C5 and C6 sugars^[74]. Although early interest focussed on agricultural field crop residues, interest has now moved to the use of "green" material (tree trimmings, yard wastes, etc), and other urban wood wastes (MSW) that currently go to landfills or composting. This has resulted from the apparent difficulty in financing projects based on the crop residues. Several years ago, Arkenol licensed its technology to JGC Corporation in Japan, which built a 2 t/d (waste wood) pilot plant in Izumi. This plant has operated for 3 years, producing 265 l/t waste wood. JGC plans to build small plants around Japan, and possibly in Thailand and Indonesia.

BC International Recently renamed to Celunol Corporation, based in Dedham, Massachusetts plans to commercialise its proprietary dilute acid hydrolysis technologies to produce ethanol and other specialty chemicals in biomass refineries. In 1995, BCI secured an exclusive worldwide licence from the University of Florida (UFL) to commercialise the mixed sugars fermentation technology based on their genetically engineered bacteria (E.coli). Although a number of problems have been experienced in their attempts to commercialise the technology (supported by an US\$11 M grant from the US DOE), BCI has reported its intention to go ahead with plans to build a 380 ML/y ethanol plant in Louisiana using the UFL bacteria^[75].

Abengoa Bioenergy A subsidiary of Abengoa S.A. (Spain) is the largest ethanol producer in Europe, and is now building a 5 ML/y wheat straw-to-ethanol plant at Salamanca, with start up scheduled for late 2006^[76].

Masada OxyNOL Based in Birmingham, Alabama apparently is no longer in business as its only project was for sale in 2004 after the main financial backer died^[77]. Masada had been promoting an MSW-ethanol project at Middletown, New York based on sulphuric acid hydrolysis. The large tipping fees and additional revenue from recycled materials associated with the MSW feedstock would obviously play a key role in the economic viability of this operation.

Agrol BioTechnologies Ltd Based in Surrey, UK, this company plans to commercialise biomass refining based on the patented thermophyllic bacillis strains developed at Imperial College^[78].

Novozymes This Denmark based company has announced plans to collaborate with the China Resources Alcohol Corporation (CRAC) in developing cellulosic ethanol. Both parties have signed a three year development agreement, and, as an extension of this agreement, CRAC plans to build a pilot plant for cellulose ethanol in Zhaodong, China^[79].

Xethanol Corporation Have recently announced^[80] it will construct a 190 ML/y cellulosic ethanol plant, scheduled for operation in mid 2007, on the site it is acquiring from Pfizer pharmaceutical in Augusta, Georgia, USA. The plant is being designed to run on a variety of feedstocks from the local forest products industry, so that they can run at capacity when production

begins in mid 2007. By combining Xethanol's proprietary technologies with those of Praj, they believe they can produce low cost ethanol.

Other players Lignol Innovations (Vancouver, Canada) and ICM (through partnerships with Genencor and Novozymes). These two groups are planning to further develop their R&D interests in this area.

Note, although lignocellulosic-to-ethanol economics have not yet been established with any real reliability, predicted capital costs have generally been estimated to be 2.4 to 4 times that of a grain based ethanol $\text{plant}^{[81]}$. The lower figure (2.4x) represents the somewhat optimistic scenario projected by NREL for a mature version of their (yet unproven) technology using the Z. mobilis microorganism. One of the key factors in the overall economics will be the delivered cost of feedstock material. Credits that may be applicable for tipping fees (where feedstocks are otherwise taken to waste facilities) have been recognised as making a significant contribution to reducing operating costs for this plant option.

The US EPA Act 2005, which promises substantial governmental assistance to commercial lignocellulosic based plants, is likely to provide a strong incentive for scale up of laboratory scale processes currently under development. As noted above, five major process developers, Iogen, Swan Biomass, Arkenol, BCI and Xethanol appear to moving toward substantial sized plants.

6. TECHNOLOGY SUPPLIERS

Although there are a large number of ethanol plants in operation around the world, it appears that these have generally been supplied by a limited number of technology companies with specialised expertise in various aspects of the technology, plant design, training and operation. With the recent interest in the potential expansion of the ethanol market in Australia, interested parties have tended to work with existing international companies to utilise the experience and expertise gained in other parts of the world.

Whilst confidentiality limits specific details in relationships between some of these companies and potential customers, several companies are exploring participation in the Australian market. A brief background on some of these technology companies is summarised below, as a basis for demonstrating the expertise and experience available. It is not intended to present an exhaustive list, but to outline the involvements known to exist in some of the proposed Australian developments.

6.1. ICM Inc.

ICM Inc. is a process engineering company founded in 1995 and based in Colwich, Kansas, and is probably the leading dry milling ethanol process technology supplier in the USA, having supplied the technology for some 37 plants in operation and 29 additional plants under construction^[38,82]. In the USA, ICM's plant construction partner is Fagen Inc., which is based in Granite Falls, Minnesota. ICM have supplied two coal-fired bubbling-bed fluidised bed combustion (BFBC) boiler units for plant steam, as an alternative to natural gas-fired boilers. ICM has not been involved in the design of wet milling plants.

6.2. Delta-T Corporation

The Delta-T Corporation, based in Williamsburg, Virginia, was formed in 1984, based on molecular sieve technology for dehydrating ethanol. Delta-T apparently built the first commercial molecular sieve unit for the vapor-phase dehydration of ethanol, to offer an alternative to the conventional azeotropic distillation process, and the company claims that, today, its molecular sieve units are drying and purifying alcohol at over 50 installations worldwide.

Delta-T provides technology, plants, systems, and services to the fuel, beverage, industrial, and pharmaceutical alcohol markets. It claims to have provided expertise in producing, drying and purifying alcohol at over 70 international sites. The company recently formed an alliance with (TIC) The Industrial Company (industrial plant construction) and T.E. Ibberson (detailed engineering design and grain handling). Delta-T are reported^[83] to be providing the ethanol technology for the planned Primary Energy plant at Gunnedah, with the anaerobic digester design coming from Europe^[84]. It is reported that Delta-T has 10 ethanol plants under construction at present (July 2006), in the US and Canada^[85].

6.3. Broin Companies

Broin Companies is a group based in Sioux Falls, South Dakota, and is reported to be the second largest supplier of ethanol plants in the industry. Broin has been in the ethanol industry 20 years, and has designed and constructed 23 operating ethanol plants, with a further nine currently under construction or development. By mid 2007, the Broin Companies will have annualised production exceeding 3.8 Gl of ethanol[86]. Broin are reported to have 3 new plants under construction at present in the US and Canada^[85].

6.4. Katzen International Inc.

Katzen International Inc is based in Cincinnati, Ohio, and has been a prominent process engineering company in the fermentation and related chemical engineering fields since Dr. Raphael Katzen founded the company in 1955. Katzen International built one of the early large-scale corn-to-ethanol plants (230 ML/y) in South Point, Ohio (commissioned in 1984). Katzen was also prominent in numerous assessments of converting lignocellulosic feedstocks to ethanol in the 1980s and 1990s. While Dr Katzen retired from the company in the 1990s, Katzen International remains active in the ethanol and sugar fields worldwide. One new plant is reported to be under construction in the US at present^[85].

6.5. Vogelbusch GmbH

Vogelbusch GmbH is based in Vienna, Austria, and is a major global player in the engineering and construction of plants for bioethanol production. The Houston based subsidiary Vogelbusch U.S.A. Inc. has supplied some 14 ethanol plants in the United States with a total capacity of 2.7 GL/y, and has an additional 600 ML/y of capacity under construction or design. Vogelbusch was also a pioneer in the development of molecular sieve dehydration of ethanol^[87]. Grainol have reported that they intend to use Vogelbusch (in conjunction with Vireol of Great Britain) for their proposed plant in Western Australia^[88,89].

6.6. Praj Industries

Praj Industries started in India in 1984, with the objective of providing designs and equipment to the distillery industry, based on the assumption of the Indian sugar industry being the backbone of the rural economy, and that there was a big future for added value for the industry through ethanol and other co-products. Praj offers solutions for distillery and brewery wastewater treatment and utilisation, and has spread its reach beyond India to over 30 countries. The company claims to be one of the world's largest suppliers of molasses based distillery technology, plant and equipment, and offers packages for multiple feedstocks, including cane molasses, cane juice and filtrate, starch based raw material like corn, sorghum, wheat, tapioca, and tropical sugar beet^[90].

6.7. Bioscan A/S

Bioscan A/S, based in Odense, Denmark, produces biodigesters for a wide range of applications and has considerable experience in the technology and operation of large scale systems in ethanol and related agricultural installations. The BIOREK[®] process and associated technology developed by Bioscan was designed and built for large scale livestock (primarily swine) operations, and can be used in any process where large amounts of organic materials, sludges and municipal, agricultural or food wastes are produced.

The BIOREK[®] process utilises an ultra-filtration system which allows for continuous recycling of undigested organics, as well as reclamation and re-introduction of active organic enzymes. Reverse osmosis is used to produce potable water.

Application of biodigesters to process ethanol stillage and produce biogas (typically around 55% methane and 45% carbon dioxide), organic fertilisers, aqueous ammonia and potable water is a fairly recent innovation, and offers an alternative to producing the conventional distillers grain products.

Bioscan technology will be utilised by Primary Energy Pty Ltd in their proposed plants in Kwinana, Brisbane and Gunnedah.

The Econcept Bio-Energy Corporation of Kelowna BC in Canada are promoting their ENVIROPLUSTM biodigestion system, which appears to be based on the Bioscan BIOREK[®] technology^[91]. Econcept and Canadian based Outlook Resources have recently announced the signing of a Memorandum of Understanding to form a new company, Nexus Bio-Energy Corporation, to pursue the development of the ENVIROPLUSTM technology for ethanol and biogas projects.

7. LIFE CYCLE ANALYSES

This section of the report details the life cycle analysis (LCA) for a number of production systems for ethanol in Australia. For the purposes of this study, only GGEs, and the consumption of resource energy and fresh water, will be considered in the LCAs. A description of these LCA indicators, as well as an overview of the systems studied, are given below.

LCA Indicators

It should be noted that these indicators are proxies for a wide range of impacts - environmental and resource depletion:

- *Resource energy* relates only to fossil energy inputs, since they contribute to depletion of fossil energy resources. It is expressed as GJ consumed to produce the functional unit (in this study, either 1 tonne of grain, 1000 litres of ethanol, or 1 GJ of delivered energy by combustion of the ethanol). The resource energy for each fuel type/energy source is calculated on a "GJ/GJ of delivered energy" basis; this value is calculated from the resource in the ground, through to the energy form delivered to the production system for the functional unit. Solar energy used for growing the grain is excluded, since it does not represent a depletion of energy resources.
- *GGEs* are emissions of gases into the atmosphere that affect the temperature and climate of the earth's surface; the main ones are carbon dioxide (CO₂), methane (CH₄) and nitrous oxide (N₂O). These gases (in particular, CO₂ and CH₄) are generated in the production and combustion of fossil fuels, with nitrous oxide produced, eg, from the use of nitrogenous fertilisers. Each of these gases has a different weighting in terms of their impact on heat retention in the atmosphere: with carbon dioxide as unity, methane has a value of 21, and nitrous oxide a value of 310. The overall impact is quantified on a "tonnes of carbon dioxide equivalent" basis, expressed as t CO_{2-e}. When inputs to the process contain carbon sequestered from the atmosphere (eg biomass in general, and grain in particular for this study), the GGE value represented by this is taken to be a credit in the LCA methodology, ie it appears as a negative value.
- *Water consumption* relates to the amount of fresh water used in the production of fertilisers, fuels, etc (in the form of process water), and is used to quantify the depletion of fresh water resources. It is expressed on a volume per functional unit basis, eg m³/t of grain, or per kl of ethanol. The water falling as rain on crops is not included, since this water is not considered to be available as run off, allowing collection and use, eg for domestic or more intensive agricultural purposes. However, estimates for the water required for growing of the grain is noted in the relevant section for comparison with process water consumption.

Systems Studied

The systems studied are:

- The production and storage of the grains (wheat and sorghum).
- The production of ethanol with 7 variants for the range of by-products, for each of the grains.

The production of the two grains being used in the study, wheat and sorghum, have been considered independently to enable ease of comparison with an MLA sponsored LCA

study currently underway at the University of New South Wales, examining the grain-to-feedlot process chain.

This study is based on a hypothetical ethanol production facility located in Gunnedah, NSW, with an assumed plant capacity of 160 ML/year of ethanol. It is assumed that the grain production is in the Tamworth/Gunnedah region (transported to Gunnedah for storage). This location was chosen by the MLA as representative of a large grain growing region, with scope for ethanol production.

For ethanol production, 2 grain feeds will be used: 100% wheat, and 100% sorghum. Both wet and dried distillers grain options will be considered.

The wet distillers grain options include:

- The sale of wet distillers grain to feedlots at 70% moisture
- Biodigestion to produce fuel gas for the process with some electricity for export to the grid (using two alternative generation technologies of different efficiencies)
- The combustion of wet distillers grain to produce electricity for the process, as well as export electricity (using two alternative generation technologies of different efficiencies).

The dry distillers grain scenarios only cover the drying of the distillers grain to be sold to feedlots at 10% moisture. This can be carried out with either conventional drying (lower energy efficiency), or with new, higher efficiency drying technology.

In carrying out the LCA, fertiliser by-products from biodigestion will also be included as credits.

Therefore, the cases studied were:

- Case 1 WDG direct to feedlot.
- Case 2 DDGS with conventional drying.
- Case 3 DDGS with high efficiency drying.
- Case 4 Anaerobic digestion, with gas engine electricity generation (33% efficiency).
- Case 5 Anaerobic digestion, with NGCC electricity generation (50% efficiency).
- Case 6 WDG for electricity generation by fluidised bed combustion (20% efficiency).
- Case 7 WDG for electricity generation using integrated drying and gasification combined cycle (40% efficiency).

The life cycle inventories were carried out using the CSIRO Xe model, and, unless otherwise noted, the associated database was used for all of the sub-systems; *eg* grid electricity, fuels, some fertilisers.

7.1. Grain Production

While the technology for ethanol production is described in detail in Section 2.2, it is useful to provide some comments on grain production in the context of this LCA.

Grain crops in the Gunnedah area are typically not irrigated: all water for grain production is therefore assumed to be from natural rainfall (*ie* dryland cropping). It is assumed that a stubble retention practice is used; this reduces erosion and conserves water and nutrients (compared to some overseas practices of stubble harvesting or burning).

In grain production, in addition to the carbon dioxide emissions associated with the use of fossil fuels for soil preparation, seeding, spraying of herbicides and pesticides, and harvesting, there are substantial emissions of nitrous oxide from nitrogenous fertiliser application and land disturbance.

In addition, CO_2 from the atmosphere is sequestered as forms of carbon in the grain. Although all sequestered CO_2 is ultimately released back into the atmosphere through combustion of the ethanol and from other steps in the life cycle, its inclusion is required by LCA methodology, and enables the GHG effects of ethanol to be correctly calculated for comparison with the fuel it is intended to displace (*ie* petrol). *Note that the GGE results for grain production will be given with and without the allowance for CO*₂ *sequestration by the grain, for the purposes of comparison with other studies.*

Functional Units

In establishing the basis for the LCA, it is important to define the functional unit(s), options to be considered, and the related boundary conditions. This study is a cradle-to-gate analysis for the production of 1 tonne of dried grain in storage; both wheat and sorghum are considered separately.

System boundary

The system boundary for the life cycle analysis for the production of 1 tonne of grain, whether wheat or sorghum, is shown in Figure 6. The boundary considers inputs required for grain cultivation and harvesting, grain transport to the storage silo in Gunnedah, and for handling and maintaining grain within the silo. It is assumed that there is only a modest drying requirement for part of the summer grain crop (further discussed below).

In addition, direct emissions at the farm site are calculated (*eg* tractor and harvester fuel consumption and emissions, and nitrous oxide emissions from the use of nitrogenous fertilisers).

The consumption of resources, (energy and water), and the emissions of greenhouse gases, (on a CO_2 equivalent basis), are then totalled and attributed to 1 tonne of dried and stored grain.

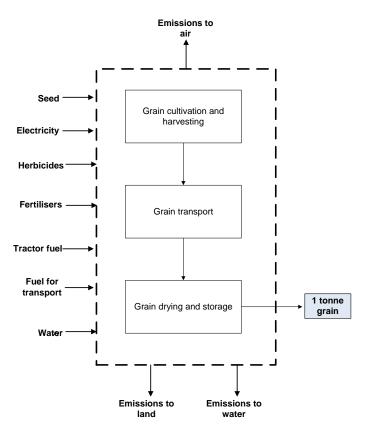


Figure 6 System boundary for LCA of grain production

Fertilisers and consumables

A summary for the usage of fertilisers, herbicides and diesel for wheat and sorghum grown in the Gunnedah region are shown in Table 6. It should be noted that the data for fertilisers used in wheat growing has been based on advice from the District Agronomist (total of 60kg N/ha), rather than the significantly higher values for fertiliser use given in the DPI Farm Enterprise Budget Series data sheet (2006) for the North East Region.

Input		Usage for 1 t wheat	Usage for 1 t sorghum
Ammonia (82%N)	kg	19.0	-
DAP (18%N, 20%P)	kg	9.3	8.0
Urea (46%N)	kg	-	42.0
Glyphosate	kg	0.7	0.5
Herbicide	kg	0.3	0.7
Diesel	GJ	0.34	0.24

Table 6 Fertiliser, herbicide and diesel use per tonne of grain^[92,93]

These applications typically yield 3.5 t of wheat/ha, and 5 t of sorghum/ha for the Gunnedah region^[93].

The factors affecting the formation of N₂O have been detailed in a report for the GRDC by Rodriguez *et al*^[94]. Key factors such as soil moisture, soil temperature, amount of inorganic nitrogen added, and soil and crop management practices (*eg* fallow periods), all affect N₂O emissions. It is therefore difficult to assign a specific value to N₂O emissions from a grain crop. Rodriguez *et al* have recommended that, as representative figures for grain

production, a value of 0.25 kg N/ha should be used for the loss of nitrogen as N_2O due to soil disturbance, and that the loss due to fertiliser application, whatever the form of nitrogenous fertiliser used, be taken to be 1% of the N applied (again as N_2O). These recommended values have been used in this study.

As N₂O has a Global Warming Potential (GWP) of 310 times greater than CO₂, this emission will be shown to be very significant in the overall GGEs for grain production.

Water consumption during grain production

In the present study, fresh water consumption for grain production was considered in 2 categories:

- From rainfall and soil moisture, used in the growing of the grain.
- Process water, obtained from various water supplies, and used in consumables (mostly fertiliser and electricity).

For dry land crops, as assumed for this study, water used in the growing of the crop can be from rain that falls during the growing cycle, or from soil moisture (storage of rainfall). The total amount of water available to a crop depends on both these sources of water and evaporation. The water use efficiency (WUE) for grain growing is dependent on a number of factors, and has been increasing due to the greater use of nitrogen fertilisers, and more water efficient grain varieties. CSIRO Sustainable Ecosystems^[95] has advised that indicative WUE for wheat and sorghum is in the range 10-20 kg grain/mm H₂O/ha. The water consumptions for the grain crops are therefore in the range 500-1000 m³/t grain. The data sheets for wheat from the NSW Department of Agriculture for Winter 2006,^[96] provide a WUE value at the bottom of this range, 9.5 kg grain/mm H₂O/ha (*ie* 1,050 m³/t grain).

CSIRO^[95] has advised that the water required for growing of wheat in Victoria, or sorghum in Queensland, would also fall in the above range.

Data for the fertilisers was mostly from the Xe LCA model. Data for the production of herbicides and pesticides has not been published, but it would be expected to be negligible, given the amount used per tonne of grain (an assumption made in previous studies by others).

Transport

There are a number of transport inputs:

- Delivery of fuel and fertilisers to the farm.
- Delivery of grain from the farm to the storage silo; an average distance of 70 km (assumes that grain is received from within a radius of 100 km).

For fertilisers, in order to represent average Australian figures, the transport emissions and energy requirements are based on the percentage of fertiliser that is imported, relative to that which is produced in Australia. For the portion that is sourced from overseas, the assumed freight distance is 15,000 km by sea, and 350 km by road. For locally produced items, the transport distance is assumed to be 350 km by road (Newcastle to Gunnedah). Table 7 shows the percentages of each material imported, or supplied, from Australian sources.

Product	Imported	Australian
	%	%
Ammonia	0	100
Monoammonium phosphate	79	21
Diammonium phosphate	34	76
Urea	85	15
Diesel	0	100

Table 7 Transport breakdown for farm consumables

The resource energy and GGE factors for the transportation steps are shown in Table 8. Water consumption is assumed to be insignificant.

Transport mode	Vehicle	Resource energy (MJ/t.km)	GGE emissions (kgCO _{2-e} /t.km)
Road ^[97]	20 t diesel tanker	1.0	0.07
Road ^[97]	19 t diesel flat-top	1.1	0.08
Sea ^[98]	20,000 t bulk carrier	0.1	0.007

Table 8	Transport	resource	energy	and	GGEs
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In this analysis, for road transport, one way operation was assumed, with the vehicle returning empty. In practice, back loading could be applicable, but would only make a small contributor to the LCA KPIs.

Farm machinery

It is assumed that the average tractor requirement is 0.635 tractor-hour/ha per season, for land yielding 3.5 t of wheat or 5 t sorghum. The fuel consumption is assumed to be 48 L/h. These figures are based on data from the NSW DPI. Diesel fuel is assumed to have an energy density of 38.6 GJ/m³, with a GGE factor of 69 kg CO_{2-e}/GJ from combustion.

While the energy required to make the machinery used on the farm is normally considered to be minor, and is usually ignored, Graboski^[99] has made an estimate for corn production in the USA. His value of 0.32 GJ/ha for the energy embodied in farming equipment has also been verified by a major recent University of California study^[100], and has been used in the present study.

Grain Storage

There are a number of activities^[101] associated with the storage of grain that involve the use of energy, and some small amount of fumigant. These are discussed below, and the figure used for the LCA are given in Table 9.

For ventilation, aeration-cooling electrical energy costs are typically 20-50c/t for winter crops for a season (6 to 9 months of storage). At a nominal power cost of 15c/kWh, the pro-rata electrical energy consumption is 1.3-3.3 kWh/t of storage.

For aeration-drying, electrical energy costs range from \$3.5-\$10/t for removing 4% points of moisture from a summer crop in typical farm stores (usually less than 120 t capacity). At the nominal power cost of 15c/kWh, the corresponding electrical energy consumption is 30-67 kWh/t.

If additional drying is required, there are a number of different drying systems fired by diesel or gas, and these generally result in a 33-150% increase in drying energy over that

for aeration drying. Drying equipment is not commonplace for all tonnage cropped in Australia, and is regional, so you could ignore this figure for an Australia wide estimate. However, for the New England and Liverpool plains areas where summer crops (*eg* sorghum) are more prevalent, it is estimated that 33 to 50% of properties regularly use some form of drying for summer crops (but not as much for winter crops).

Conveying and handling energy costs are typically 10-40c/t per transfer on-farm. For several transfers at 15c/kWh. An average equivalent electrical energy consumption was assumed.

Fumigant (phosphine) is applied per volume of store, with one or two fumigations per season (1.375 g of phosphine per tonne per fumigation). This has not been included in the LCA, again due to lack of production information, and the insignificant mass of fumigant.

The values for electricity use for storage and handling are given in Table 9.

0 00 1		
	Wheat	Sorghum
Ventilation	2.3	2.3
Aeration drying	-	25
Conveying/handling	3.4	3.4
Total (kWh/t)	5.7	30.7

 Table 9 Storage energy requirement (kWh/t of grain)

In the study it is assumed that 50% of the sorghum requires aeration drying. No allowance has been made for drying of wheat.

Fertiliser production

The data for the production of the fertilisers and herbicides mentioned is mostly based on information from prior CSIRO^[102] studies. Table 10 shows major energy consumption by source for fertilisers, pesticides and herbicides.

Material	Electricity (MWh/t)	Natural Gas (GJ/t)	Fuel oil (GJ/t)
Ammonia ¹⁰³	0.08	31.6	5.33
MAP ^a	0.04	0.33	-
DAP ^a	0.03	0.29	-
Urea ^b	0.17	3.91	-
Glyphosate	14.8	111	55.9
Other herbicides/pesticides	5.08	41.4	83.6

Table 10 Consumables for the production of 1 tonne of fertilisers, herbicides and pesticides

Table 11 shows the equivalent total resource energy, GGE emissions and water consumption data per tonne of product.

^a Note that ammonia and phosphoric acid are inputs for MAP and DAP production. The values shown in this table are direct consumables for MAP and DAP production rather than lifecycle values.

^b Note that ammonia is an input for the production of urea. The values shown in this table are direct consumables for urea production, rather than lifecycle values.

Material	Resource energy (GJ/t)	GGE emissions (tCO _{2-e} /t)	Water (kL/t)
Ammonia	44.9	2.03	25.2
MAP	12.0	0.69	10.8
DAP	19.6	1.0	14.1
Urea	31.6	1.59	14.5
Glyphosate	340	21.4	22.6
Other herbicides/pesticides	194	10.1	7.6

Table 11 Resource energy, GGEs and water per tonne of fertilisers, herbicides and pesticides

Energy and emissions factors for main fuel sources

The major energy sources used in the production of fertilisers, grains and ethanol are natural gas, fuel oil, diesel and electricity. For NSW conditions, the resource energy and GGE for the sub-systems of each energy source, are given in Table 12.

Energy Source	Resource energy (GJ)	Total (kg CO _{2-e} /GJ)
NG	1.08	64.0
Fuel oil	1.15	84.1
Diesel	1.15	80.7
Electricity	1.89	268

Table 12 Resource energy used per GJ of delivered energy

7.2. Ethanol production

LCAs are affected by the choice of system boundaries, the functional unit, by-products, and how the impacts from these are allocated. In the present study, credits for the by-products have been allocated to the main product or functional unit (*ie* 1 kL of ethanol). The credit has been calculated as the avoided impacts due to displacement of other products. For example, production of export electricity replaces electricity from the NSW grid, organic by-products displace nitrogen and phosphate fertilisers.

This study is based on a hypothetical ethanol production facility located in Gunnedah, NSW, with an assumed plant capacity of 160 ML/year of ethanol. It is assumed that the grain production is in the Tamworth/Gunnedah region (transported to Gunnedah for storage). This location was chosen by the MLA as representative of a large grain growing region, with scope for ethanol production.

Ethanol production was for 100% wheat, and 100% sorghum. Both wet and dried distillers grain options will be considered. The wet distillers grain options include; biodigestion to produce fuel gas for the process with some electricity for export to the grid, the sale of wet distillers grain to feedlots at 70% moisture, and the combustion of wet distillers grain to

produce electricity for the process as well as export electricity. The dry distillers grain scenarios only cover the drying of the distillers grain to be sold to feedlots at 10% moisture. Fertiliser by-products from biodigestion will also be included as credits.

Functional Units

The basis for the LCA studies is a cradle-to-gate analysis for the production of 1,000 litres of ethanol (in storage at the production plant). It should be noted that 100% ethanol is considered, not the denatured fuel (containing a small quantity of petrol).

Case Studies

The case studies considered for the ethanol production stage are shown in Table 13 below.

Case	ID	Comments
1	WDG	WDG direct to feedlot.
2	DDGS	DDGS with conventional drying.
3	DDGS – HE drier	DDGS with high efficiency drying.
4	AD – ICE	Anaerobic digestion, with gas internal combustion engine electricity generation (33% efficiency*).
5	AD – GTCC	Anaerobic digestion, with gas turbine combined cycle electricity generation (50% efficiency).
6	WDG-FBC	WDG for electricity generation by fluidised bed combustion (20% efficiency).
7	WDG-IDGCC	WDG for electricity generation using integrated drying and gasification combined cycle (40% efficiency).

 Table 13 Case studies considered for the ethanol LCA

* all thermal efficiencies are on a higher heating value basis (HHV)

These cases were investigated for both wheat and sorghum (*ie* 14 cases in total), with the case study numbers modified with an added w or s, respectively.

System Boundaries

The system boundaries for ethanol production encompass all raw materials and associated energies that are used in the production of the grains, as well as in the production of any consumables utilised as part of ethanol production. It is assumed that the life cycle impacts associated with the construction of the plant, and any associated equipment is negligible, and is not considered in this study; this is based on the resource energy value derived by Graboski^[99] for such capital items for a biorefinery, of 40 MJ/kL of ethanol (*ie* <0.2% of the energy content of the produced ethanol).

The system boundaries for the above case studies are shown schematically below.

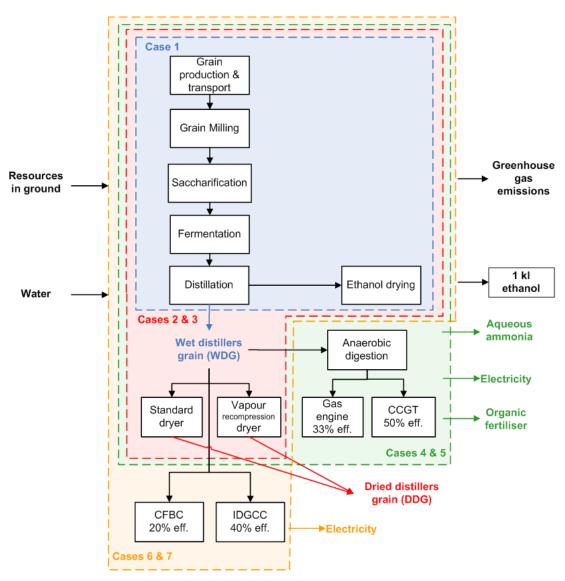


Figure 7 System boundary for LCA of ethanol production^c

^c Note: For the AD cases, separate data is not available for the centrifuge step. As a result, the AD values include any contribution for this source. This is expected to be insignificant in the overall context.

Credits - electricity

The electricity credits depend on the amount of export electricity generated by the plant (depends on the amount of stillage and the efficiency of generation), and the LCA indicators for the grid electricity. In practice, the latter will be location dependent. However, for the purposes of this study, State grid average indicator values have been used.

For cases involving the biodigestion and/or combustion of WDG, there is excess electricity for sale to the grid – this is taken to have a credit for resource energy, GGEs and water, equivalent to those that apply to electricity supplied by the NSW transmission grid (averaged).

If located in other states, for example in Queensland (sorghum based), or in Victoria (wheat based), the indicator values will be significantly different^[104] as given in Table 14.

1 5	5	55	8
	NSW ^d	Queensland ^e	Victoria ^d
Resource energy (GJ)	10.41	10.91	13.74
GGE (t CO ₂)	0.965	0.983	1.437
Fresh water (m ³)	1.51	1.83	2.45

Table 14 Impacts for 1 MWh of electricity from the transmission grid

The study has assumed 4 types of generation technology, according to fuel type (gas or solid), and the effect of this on overall thermal efficiency.

When electricity is generated, the waste heat is used for the majority of heating and steam raising, thereby reducing or eliminating the need for natural gas. It is assumed that 65% of the waste heat energy from the power plant is recovered as steam, and is used to displace the natural gas requirement of the plant (assuming a NG to steam energy conversion efficiency of 80%).

Cases 4w and 4s assume that the electrical efficiency for a gas internal combustion engine is 33%, which is sufficient to supply all of the plants electricity requirement and heating (NG) requirements. Cases 5w and 5s assume that a higher efficiency gas turbine with combined cycle is used, with an electrical efficiency of 50%.

Cases 6w/s and 7w/s deal with the combustion of the WDG by-product, rather than selling it, in either the dry or wet form, to feed lots. Cases 6w and 6s consider that the energy available in the WDG is 5.5GJ/t at 70% moisture, and that the efficiency of conversion to electricity is 20%, whereas Cases 7w and 7s consider the same energy content in grain, but an electrical efficiency of 40%.

Credits – distillers grain

For those cases involving DDGS and WDG, the yield of these products per kL of ethanol are given in Table 15. The yields are derived directly from Table 4.

^d For year ending December 2003; no contribution from SMHEA or interstate transfers

^e For year ending June 2004; no contribution from interstate transfers

By-product	Unit	Wheat	Sorghum
WDG	t	3.0	1.94
DDGS	t	1.0	0.65

This study assumes that a market may exist for both wet as well as dry distillers grain, and hence Cases 1w and 1s have also been included. The decision to consider the sale of WDG is based on the fact that this currently occurs in the USA. From a life cycle point of view, it is assumed that the credits for the DDGS and WDG are the same, due to the same amount of dry matter being present in each case. However, there will be a difference in the environmental impact for transport of WDG relative to DDGS on an energy content basis, due to the transport of the extra water in the case of WDG. All values are shown on the basis of the production of 1kL of ethanol.

For Cases 2w and 2s, the energy required for WDG drying is based on current plant data (2.25 MW of electricity and 1,070 TJ/y of natural gas to produce 18 t/h DDGS). As these energy consumptions are for standard rotary drum drier technology, a higher efficiency process has been used for Cases 3w and 3s. It was assumed that drying energy can be reduced by 50% with advanced technology (*cf* lignite drying).

Credits - fertiliser values

For Cases 4 and 5 (anaerobic digestion of the stillage), there are a number of intermediate products (italicised), and by-products, from anaerobic digestion. The quantities of these co-products produced per kL of ethanol are shown in Table 16.

By-product	Units	Wheat	Sorghum	Wheat	Sorghum
		(Case 4w)	(Case 4s)	(Case 5w)	(Case 5s)
WDG	t	3.0	1.94	3.0	1.94
Digestible solids	kg	903	582	903	582
Methane	GJ	12.4	8.0	12.4	8.0
Electricity	MWh	0.99	0.6	1.58	0.98
Fertiliser NPK(6%-8%-8%) (MAP equivalent)	t	0.33 (0.24)	0.21 (0.15)	0.33 (0.24)	0.21 (0.15)
Ammonia	kg	25	16	25	16

Table 16 Anaerobic Digestion - intermediates and by-products

Table 17 Data for combustion of WDG

By-product	Wheat (Case 6w)	Wheat (Cases 7w)	Sorghum (Case 6s)	Sorghum (Case 7s)
WDG (t)	3.0	3.0	1.94	1.94
Electricity (MWh)	0.77	1.69	0.46	1.05

The by-product values from Table 16 and Table 17 are used to calculate credits for the respective LCA cases. The factors used for these credits are shown in Table 18.

Note that the composition of the organic fertiliser is approximately 8% nitrogen and 8% phosphorus. The basis for assigning a credit for this material is the nitrogen content. monoammonium phosphate, (11% nitrogen), is used as the substituting fertiliser which results in 100kg of organic fertiliser being equivalent to 73 kg of MAP. The numbers for the quantity of fertiliser quoted below are those for the 8% fertiliser, for which externalities are applied based on MAP.

Note also that the greenhouse gas emissions credits applied to feed grain are negative. This is a consequence of the fact that grain production is a net consumer of CO_2 .

In addition, the credit applied to the DDGS is based on 85% of the values for the grain, since it has:

- A lower starch content, but is higher in protein and fibre, and
- About 85% of the metabolisable energy content of the original grain (under 11 MJ/kg dry mass for DDG, compared with around 13 MJ/kg dry mass for the feed grain).

As the moisture content of WDG is 70% and for DDGS is 10%, three tonnes of WDG is required to yield one tonne of DDGS. Therefore, the credit applied to WDG as a feedstock for cattle is 28.3% of the value for grain.

Material	Units	Resource energy (GJ/unit)	GGE emissions (tCO _{2-e} /unit)	Water consumption (m ³ /unit)
Electricity (NSW)	MWh	10.41	0.965	1.51
Anhydrous ammonia	t	44.9	2.03	25.2
MAP	t	12.0	0.69	10.8
Wheat	t	1.91	-1.21	0.61
Sorghum	t	2.46	-1.13	0.74

Table 18 Factors used for system displacement credits

7.3. LCA results

In comparing LCA results from different climatic regions, and countries, it must be recognised that there are considerable differences in agricultural practices (crop rotations, fallow periods, rainfall and/or irrigation regimes), and in particular, nitrogenous fertiliser use, which can have a large impact on resource energy, GGEs, and water consumption for the particular grain. To this must be added the variations associated with the grain genetics. These have a major effect on the yields, and starch content. Accordingly, the LCA results given in this report for grain production should be considered as overall approximations, which provide a useful understanding and assist in strategy development.

For ethanol production, there is considerably less variability, since a "standard" industrial process is being considered. However, the biodigestion step is not normally applied in such plants, and therefore:

• The amount of by-products will vary with the grain chemistry and process operating conditions.

• The credits attributed to these by-products will vary with the substitutions and their context (*eg* for electricity, the credit for GGEs will be far greater in Victoria than in NSW, as shown in Table 14).

7.3.1 Grain production

For the production of one tonne of grain stored in a silo in Gunnedah, the LCA values for resource energy, GGEs and water are given in Table 19.

Impact assessment values	Resource energy (GJ/t)	Non-LCA GGE (tCO _{2-e} /t) (without credit for carbon in grain)	LCA GGE (tCO _{2-e} /t) (with credit for carbon in grain)	Water (m ³ /t)
Wheat	1.91	0.22	-1.21	0.61
Sorghum	2.46	0.27	-1.13	0.74

Table 19 LCA for grain (1 tonne stored basis)

The GGE values are shown on 2 bases:

- LCA GGE including both a credit for the CO₂ equivalent of the carbon content of the grain (assuming no net increase from non-grain biomass; *eg* straw), as well as emissions from the use of fossil energy, nitrogenous fertiliser use, and
- Non-LCA GGE with excludes the credit for the CO₂ equivalent of the carbon content of the grain. This enables comparison with studies by others, in which the CO₂ sequestered by the grain is not considered.

The results show that the CO_2 sequestered in the grain is an important part of the life cycle GGE, and reduces the GGE for grain production by around 1.4 tCO_{2-e}/t.

It should be noted that the water consumption values given in Table 19 only relate to process water used to produce fuels, fertilisers, *etc*. As noted earlier, the amount of water for cropping is between 500 and 1000 m^3 /tonne of wheat or sorghum, and is assumed to be satisfied by rainfall and soil moisture.

7.3.2 Ethanol Production

The results are presented as follows:

- Resource energy
 - Tables giving a detailed breakdown for energy consumption for each stage in the production chain, for wheat and sorghum cases separately.
 - A summary graph comparing overall energy for all 14 cases.
- GGE
 - Tables giving a detailed breakdown for GGE from each stage in the production chain, for wheat and sorghum cases separately.
 - Comparison graphs showing a breakdown for GGE from each stage in the production chain for current practices, and for alternative drying and electricity technologies, for both wheat and sorghum.
 - A summary graph comparing overall GGE for all 14 cases.
- Water

- Tables giving a detailed breakdown for process water consumption for each stage in the production chain, for wheat and sorghum cases separately.
- A summary graph comparing overall process water for all 14 cases.

Resource energy

The contributions along the processing chain are shown in Table 20 (wheat) and Table 21 (sorghum), and a summary graph for overall production is given in Figure 8.

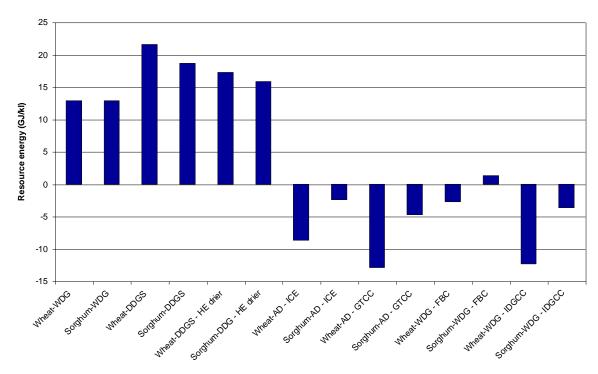
	1w	2w	3w	4w	5w	бw	7w
	WDG	DDG	DDG-HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Fertiliser/pesticide	3.48	3.48	3.48	3.48	3.48	3.48	3.48
Fertiliser degradation	-	-	-	-	-	-	-
Farming machinery	0.27	0.27	0.27	0.27	0.27	0.27	0.27
Diesel for agriculture	0.92	0.92	0.92	0.92	0.92	0.92	0.92
Transport	0.19	0.19	0.19	0.19	0.19	0.19	0.19
Grain storage	0.16	0.16	0.16	0.16	0.16	0.16	0.16
Ethanol production	9.23	9.23	9.23	0.32	2.19	-	-
WDG drying	-	8.61	4.30	-	-	-	-
Anaerobic digestion	-	-	-	-	-	-	-
Electricity generation	-	-	-	-	-	-	-
Other	0.21	0.27	0.27	0.27	0.29	0.22	0.26
Total no credits	14.5	23.1	18.8	5.61	7.50	5.24	5.28
Electricity credits	-	-	0	-10.3	-16.4	-8.0	-17.6
Ammonia credits	-	-	0	-1.12	-1.12	-	-
Fertiliser credits	-	-	0	-2.88	-2.88	-	-
Feed grain credit*	-1.62	-1.62	-1.62	-	-	-	-
Total	12.8	21.5	17.2	-8.69	-12.9	-2.76	-12.3

 Table 20 Resource energy for wheat based cases (GJ/kL ethanol)
 Image: Comparison of the second s

* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

	1s	2s	3s	4s	5s	бs	7s
	WDG	DDG	DDG- HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Fertiliser/pesticide	4.22	4.22	4.22	4.22	4.22	4.22	4.22
Fertiliser degradation	-	-	-	-	-	-	-
Farming machinery	0.15	0.15	0.15	0.15	0.15	0.15	0.15
Diesel for agriculture	0.58	0.58	0.58	0.58	0.58	0.58	0.58
Transport	0.17	0.17	0.17	0.17	0.17	0.17	0.17
Grain storage	0.80	0.80	0.80	0.80	0.80	0.80	0.80
Ethanol production	8.27	8.27	8.27	0.28	1.96	-	1.21
WDG drying	-	5.79	2.9	-	-	-	-
Anaerobic digestion	-	-	-	-	-	-	-
Electricity generation	-	-	-	-	-	-	-
Other	0.06	-	0.07	0.17	0.16	0.12	0.13
Total no credits	14.25	19.98	17.16	6.37	8.04	6.04	7.26
Electricity credits	-	-	-	-6.26	-10.2	-4.79	-10.9
Ammonia credits	-	-	-	-0.73	-0.73	-	-
Fertiliser credits	-	-	-	-1.84	-1.84	-	-
Feed grain credit*	-1.36	-1.36	-1.36	-	-	-	-
Total	12.9	18.6	15.8	-2.46	-4.73	1.25	-3.64

Table 21 Resource energy for sorghum based cases (GJ/kL ethanol)



* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

Figure 8 Overall resource energy consumption per kL of ethanol

From these results, the following conclusions can be drawn:

- For grain production (whether wheat or sorghum), fertiliser production is the major component (70%) of resource energy, with the fuel for agricultural activities of secondary importance: 20% for wheat, and only 10% for sorghum (due to its higher grain yield). Transport and storage of grain are only small contributors (3-10%).
- When the grain is processed to ethanol, the resource energy is very dependent on the processing of the stillage, and what by-product credits are applicable:
 - For the simplest case, direct sale of WDG, the resource energy is considerably lower than that for DDG, due to the large amount of energy required for drying. This difference is considerably reduced if a high efficiency drying process is used.
 - When the stillage is anaerobically digested, the resource energy also becomes negative, since there is no requirement for purchased electricity or natural gas for ethanol production - the methane from biodigestion is used to make electricity, with waste heat displacing the full requirement of natural gas. There are also significant credits for by-product fertilisers and exported electricity.
 - If the WDG is combusted to produce electricity (requires a technology similar to high moisture lignite or biomass), a negative overall resource energy is produced. Again, there is no requirement for purchased electricity or natural gas for ethanol production, since the waste heat from electricity generation is sufficient to provide all required process heating. The large credit for exported electricity (particularly for the 40% electrical conversion efficiency case), produces a negative resource energy for the chain, from grain through to ethanol.

It is relevant to note that the overall resource energy is similar, whether the stillage is anaerobically digested with the methane converted to electricity at 50% efficiency, or the WDG is directly combusted to produce electricity at an overall efficiency of 40%. In practice, the choice of electricity generation process will also depend on the overall capital costs, plus the ability to exploit opportunity biomass, such as straw.

GGEs

The contributions of the various stages along the processing chain, to overall greenhouse gas emissions, are shown in Table 22 for wheat and in Table 23 for sorghum. These values are shown graphically in Figure 9.

	1w	2w	3w	4w	5w	бw	7w
	WDG	DDG	DDG-HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Grain absorption ^f	-3.91	-3.91	-3.91	-3.91	-3.91	-3.91	-3.91
Fertiliser/pesticide	0.17	0.17	0.17	0.17	0.17	0.17	0.17
Fertiliser degradation	0.31	0.31	0.31	0.31	0.31	0.31	0.31
Farming machinery	-	-	-	-	-	-	-
Diesel for agriculture	0.06	0.06	0.06	0.06	0.06	0.06	0.06
Transport	0.01	0.01	0.01	0.01	0.01	0.01	0.01
Grain storage	0.02	0.02	0.02	0.02	0.02	0.02	0.02
Ethanol production	1.40	1.40	1.40	0.82	0.93	0.81	0.81
WDG drying	0	0.55	0.27	-	-	-	-
Anaerobic digestion	-	-	-	0.42	0.42	-	-
Electricity generation	-	-	-	0.61	0.61	1.4	1.4
Other	0.02	0.09	0.09	0.03	0.05	0.02	0.02
Total without credits	-1.92	-1.30	-1.58	-1.46	-1.33	-1.11	-1.11
Electricity credits	-	-	-	-0.95	-1.52	-0.74	-1.63
Ammonia credits	-	-	-	-0.05	-0.05	-	-
Fertiliser credits	-	-	-	-0.17	-0.17	-	-
Feed grain credit*	1.02	1.02	1.02	-	-	-	-
Total	-0.90	-0.28	-0.56	-2.63	-3.07	-1.85	-2.74

Table 22 Greenhouse gas emissions for wheat based cases ($t CO_{2-e}/kL$ ethanol)

* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

 $^{^{\}rm f}$ This is the amount of $\rm CO_2$ sequestered by the grain, calculated from the carbon content

	1s	2s	3s	4s	5s	6s	7s
	WDG	DDG	DDG-HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Grain absorption ^g	-3.42	-3.42	-3.42	-3.42	-3.42	-3.42	-3.42
Fertiliser/pesticide	0.22	0.22	0.22	0.22	0.22	0.22	0.22
Fertiliser degradation	0.30	0.30	0.30	0.30	0.30	0.30	0.30
Farming machinery	0	0	0	0	0	0	0
Diesel for agriculture	0.04	0.04	0.04	0.04	0.04	0.04	0.04
Transport	0.01	0.01	0.01	0.01	0.01	0.01	0.01
Grain storage	0.07	0.07	0.07	0.07	0.07	0.07	0.07
Ethanol production	1.34	1.34	1.34	0.82	0.92	0.81	0.88
WDG drying	0	0.35	0.18	0	0	0	0
Anaerobic digestion	0	0	0	0.27	0.27	0	0
Electricity generation	0	0	0	0.39	0.39	0.9	0.9
Other	0.1	0.1	0.07	0.02	0.02	0.01	0.14
Total without credits	-1.34	-0.99	-1.19	-1.28	-1.18	-1.06	-0.86
Electricity credits	0	0	0	-0.58	-0.95	-0.44	-1.01
Ammonia credits	0	0	0	-0.03	-0.03	0	0
Fertiliser credits	0	0	0	-0.10	-0.10	0	0
Feed grain credit*	0.62	0.62	0.62	0	0	0	0
Total	-0.72	-0.37	-0.57	-1.99	-2.26	-1.50	-1.87

Table 23 Greenhouse gas emissions for sorghum based cases ($t CO_{2-e}/kL$ ethanol)

* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

 $^{^{\}rm g}$ This is the amount of CO_2 sequestered by the grain, calculated from the carbon content

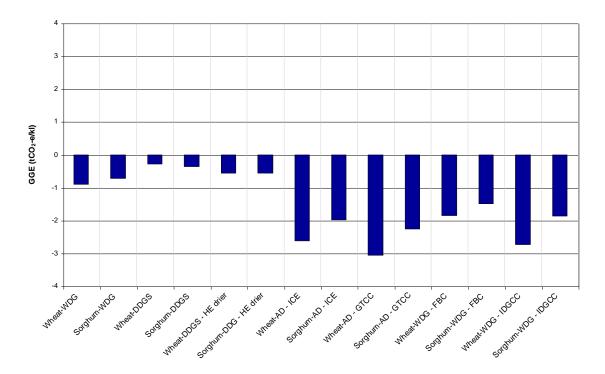


Figure 9 GGEs per kL of ethanol

From these results, the following conclusions can be drawn:

- The majority of the GGEs come from the nitrogenous fertiliser, and the related quantity of nitrous oxide generated from this. However, the overall GGE is dominated by the CO₂ taken up by the grain (3.4-3.9 t CO₂/kL of ethanol) through photosynthesis. This leads to a negative GGE for all cases.
- When the grain is processed to ethanol, GGE are very dependent on the method of processing the stillage, and what by-product credits are applicable:
 - For the simplest case, direct sale of WDG, the GGE value is lower than that when DDGS is the by-product, due to the emissions associated with drying. Higher efficiency drying provides a lower GGE value, as expected. It should be noted that the GGE increases with the feed grain credit as this by-product displaces feed grain, and therefore results in less CO₂ being sequestered by photosynthesis.
 - For anaerobic digestion of the stillage, there are lower emissions associated with ethanol production, due to the use of combined heat and power; *ie* the use of waste heat from power generation for the fermentation *etc*. Again, the electricity cases, whether from AD or WDG, have similar overall GGEs.
 - For WDG combustion, the GGE values are far lower than those for the use of WDG for feed, due to the displacement of grain and production of electricity.

It is instructive to consider GGEs along the processing chain. Figure 10 and Figure 11 show the cumulative values for conventional practices, for wheat and sorghum, respectively. Figure 12 and Figure 13 show similar results for alternative drying and power generation technologies.

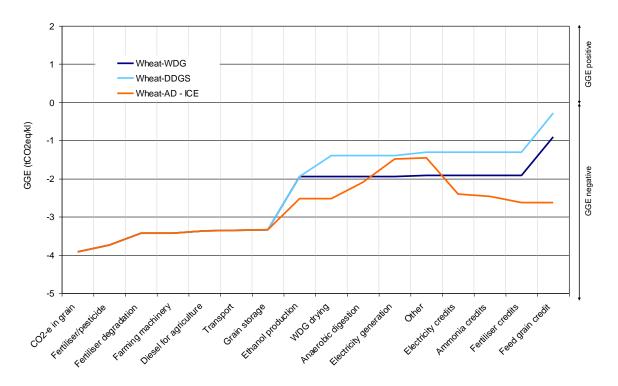


Figure 10 Breakdown of GGE for current practices (wheat)

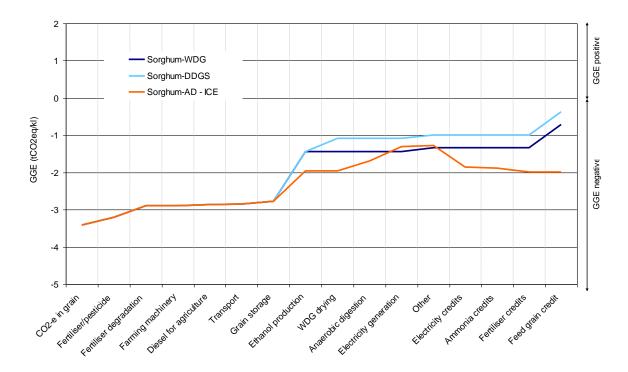


Figure 11 Breakdown of GGE for current practices (sorghum)

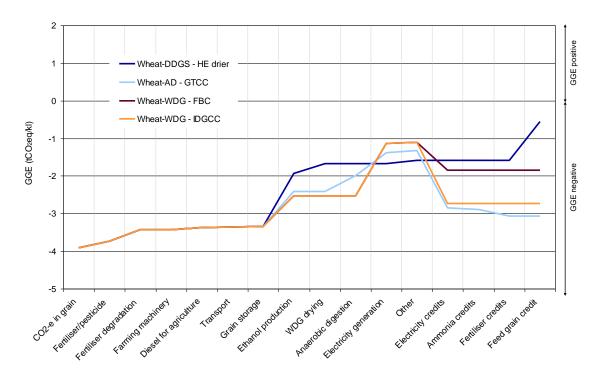


Figure 12 Breakdown of GGE for alternative drying and electricity technologies (wheat)

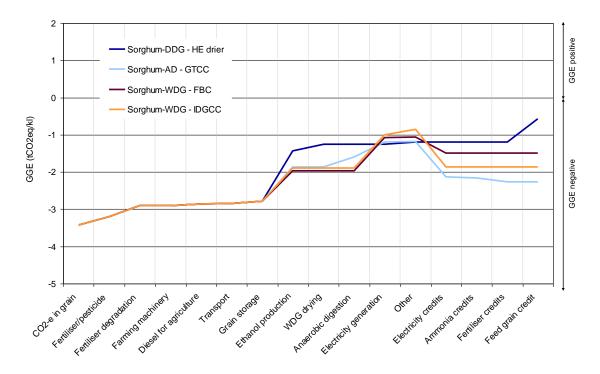


Figure 13 Breakdown of GGE for alternative drying and electricity technologies (sorghum)

These figures clearly show that, for the conventional practices, there is marked reduction in GGE for anaerobic digestion.

All of the alternative technologies reduce the overall GGE, with the highest efficiency electricity generation case (with NGCC and IDGCC) virtually offsetting the upstream GGEs for ethanol production.

Process Water Consumption

The contributions of the various stages along the processing chain, to overall process water consumption, are shown in Table 24 (wheat) and Table 25 (sorghum).

	1w	2w	3w	$4 \mathrm{w}$	5w	бw	7w
	WDG	DDG	DDG-HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Fertiliser/pesticide	1.63	1.63	1.63	1.63	1.63	1.63	1.63
Fertiliser degradation	-	-	-	-	-	-	-
Farming machinery	-	-	-	-	-	-	-
Diesel for agriculture	-	-	-	-	-	-	-
Transport	-	-	-	-	-	-	-
Grain storage	0.02	0.02	0.02	0.02	0.02	0.02	0.02
Ethanol production	3.15	3.15	3.15	1.00	1.00	2.93	2.93
WDG drying	-	0.19	-1.90	-	-	-	-
Anaerobic digestion	-	-	-	-	-	-	-
Electricity generation	-	-	-	-	-	-	-
Other	0.01	0.01	0.01	0.02	-	0.01	0.06
Total without credits	4.81	5.00	2.91	2.67	2.65	4.59	4.64
Electricity credits	-	-	-	-1.49	-2.34	-1.16	-2.55
Ammonia credits	-	-	-	-0.63	-0.63	-	-
Fertiliser credits	-	-	-	-2.58	-2.58	-	-
Feed grain credit*	-0.52	-0.52	-0.52	-	-	-	-
Total	4.29	4.48	2.39	-2.03	-2.90	3.43	2.09

Table 24 Process water consumption for wheat based cases $(m^3/kL \text{ of ethanol})$

* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

	1s	2s	3s	4s	5s	бs	7s
	WDG	DDG	DDG-HE drier	AD-ICE	AD- GTCC	WDG- FBC	WDG- IDGCC
Fertiliser/pesticide	1.71	1.71	1.71	1.71	1.71	1.71	1.71
Fertiliser degradation	-	-	-	-	-	-	-
Farming machinery	-	-	-	-	-	-	-
Diesel for agriculture	-	-	-	-	-	-	-
Transport	-	-	-	-	-	-	-
Grain storage	0.11	0.11	0.11	0.11	0.11	0.11	0.11
Ethanol production	2.28	2.28	2.28	0.95	0.95	2.09	2.09
WDG drying	-	0.12	-1.24 ^h	-	-	-	-
Anaerobic digestion	-	-	-	-	-	-	-
Electricity generation	-	-	-	-	-	-	-
Other	0.02	0.08	0.18	0.01	-	0.16	0.16
Total without credits	4.12	4.30	3.04	2.78	2.77	4.07	4.07
Electricity credits	-	-	-	-0.91	-1.48	-0.69	-1.59
Ammonia credits	-	-	-	-0.4	-0.4	-	-
Fertiliser credits	-	-	-	-1.66	-1.66	-	-
Feed grain credit*	-0.32	-0.32	-0.32	-	-	-	-
Total	3.80	3.98	2.72	-0.19	-0.77	3.38	2.48

Table 25 Process water consumption for sorghum based cases (m^3/kL of ethanol)

* based on the amount of grain replaced in the cattle feed mixture by the distillers grain

The following conclusions can be drawn:

- For grain production (whether wheat or sorghum), there is a significant amount of process (fresh) water associated with fertiliser production. While figures for process water consumption for the other components are not readily available, they are known to be small in this context.
- When the grain is processed to ethanol, the process water consumption per kL of ethanol is dependent on whether the stillage is biodigested, and credits associated with exported electricity:
 - when WDG or DDGS are by-products, the water associated with the WDG is lost to the process, except for the high efficiency drying case (see footnote)
 - for the WDG combustion cases, credits from exported electricity significantly reduce the process water consumption (by around 50% in the higher efficiency case)
 - in the biodigestion cases, water is substantially recirculated after biodigestion).
 There are also substantial credits, and these cases have negative values for overall process water consumption.

^h Note that it is assumed that for vapour recompression drying, (high efficiency drier cases), all removed water is assumed to be recovered as condensate.

It should be noted that, in comparison with these process water totals, the water used for growing the grain (soil moisture and rainfall) is over 2 orders of magnitude higher $(1500 - 3000 \text{ m}^3\text{H}_2\text{O/kl} \text{ of ethanol})$.

These results, summarised in Figure 14 below, show the saving in process water when the stillage is anaerobically digested, and the biogas used for electricity production. In the case of WDG combustion, the water credits for electricity production are offset by the loss of water in the flue gases.

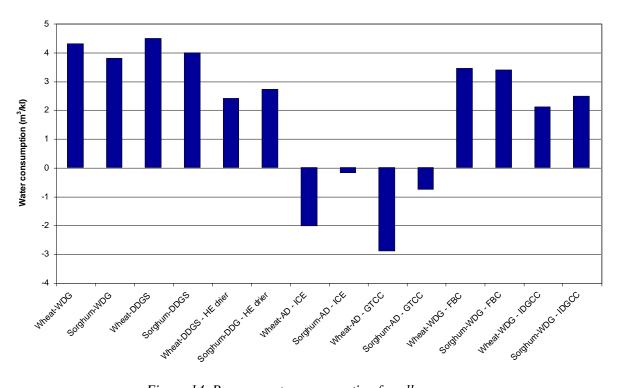


Figure 14 Process water consumption for all cases

7.3.3 Summary of Cases

To enable easy comparison between the cases, across all indicators, the data in the above tables is summarised in Table 26.

Case	Descriptor	Resource energy (GJ)	GGE (t CO _{2-e})	Process water (m ³)
1w	WDG	12.8	-0.72	4.29
1s	WDG	12.9	-0.61	3.80
2w	DDGS	21.5	-0.10	4.48
2s	DDGS	18.6	-0.26	3.98
3w	DDGS – HE drier	17.2	-0.38	2.39
3s	DDGS – HE drier	15.8	-0.46	2.72
4w	AD - ICE	-8.7	-2.63	-2.03
4s	AD - ICE	-2.46	-1.99	-0.19
5w	AD - GTCC	-12.9	-3.07	-2.90
5s	AD - GTCC	-4.73	-2.26	-0.77
6w	WDG - FBC	-2.8	-1.85	3.43
6s	WDG - FBC	1.25	-1.50	3.38
7w	WDG - IDGCC	-12.3	-2.74	2.09
7s	WDG - IDGCC	-3.68	-1.87	2.48

Table 26 Collation of LCA results (per kL of ethanol)

The main points from this summary, are that there are significant differences between the wheat and sorghum cases, associated with the higher yield of ethanol from sorghum (due to the higher starch content), and the correspondingly lower amount of stillage/WDG.

For resource energy, sorghum cases have lower values when WDG or DDGS are byproducts, and have higher values when WDG is combusted, or stillage is biodigested, to produce electricity in both cases, and fertilisers in the latter case. A similar situation arises when GGEs are compared for the two grains (for the same reason).

For GGEs, it is interesting to note that, over all case studies, the GGEs for a 160 ML ethanol plant range over almost 500,000 tpa.

For cases in which WDG or DDGS are by-products, process water consumption is lower for sorghum than for wheat, due to the lower production of WDG when using sorghum. The negative values for process water calculated for the anaerobic digestion cases are due to the recycling of water after the organics have been substantially removed. The lower values for wheat are related to the additional generation of electricity, resulting in a higher water credit.

7.4. Comparison of ethanol and petrol – GGE basis

It is instructive to compare ethanol and petrol^[105, 106] on a GGE basis over their life cycle, through to delivered thermal energy (eg as for an internal combustion engine), with electricity credits now, and projected out to 2050.

For ethanol, the data for 2006 are derived from Table 26, by adding the CO_2 emissions from combustion (1.51 t/kL), and dividing by the energy content of ethanol^[107](23.4 GJ/kL HHV).

The results are given in Table 27, for both current (2006) electricity generation technology, using the NSW grid value of 965kg CO_{2-e}/MWh , and for new generation technologies likely to be applicable in 2050 (*ie* with CO_2 capture, and a grid average GGE of 300 kg/MWh). Technologies for the latter include post combustion capture applied to advanced coal based generation, renewable energy sources (such as solar thermal), and possibly nuclear energy.

By 2050, it is also assumed that similar capture technology will be applied to the ethanol production process, with capture of 90% of the CO_2 from fermentation and anaerobic digestion, as well as CO_2 from electricity generation on site. Note, to allow for the energy required for CO_2 capture, the quantity of electricity generated is reduced by 20%.

Case	Descriptor	t CO _{2-e} /GJ (including combustion)		
		2006	2050	
1w	Wheat-WDG	0.034	-0.001	
1s	Sorghum-WDG	0.039	0.004	
2w	Wheat-DDGS	0.060	0.025	
2s	Sorghum-DDGS	0.053	0.019	
3w	Wheat-DDGS - HE drier	0.048	0.013	
3s	Sorghum-DDG - HE drier	0.045	0.010	
4w	Wheat-AD - ICE	-0.048	-0.087	
4s	Sorghum-AD - ICE	-0.020	-0.058	
5w	Wheat-AD - GTCC	-0.067	-0.088	
5s	Sorghum-AD - GTCC	-0.032	-0.058	
6w	Wheat-WDG - FBC	-0.014	-0.075	
6s	Sorghum-WDG - FBC	0.000	-0.051	
7w	Wheat-WDG - IDGCC	-0.053	-0.085	
7s	Sorghum-WDG - IDGCC	-0.015	-0.048	
Petrol	Petrol	0.077	-0.001	

Table 27 Life cycle GGE for the production and use of ethanol compared to petrol

The results are also shown graphically in Figure 15 (2006) and Figure 16 (includes both 2006 and 2050 scenarios).

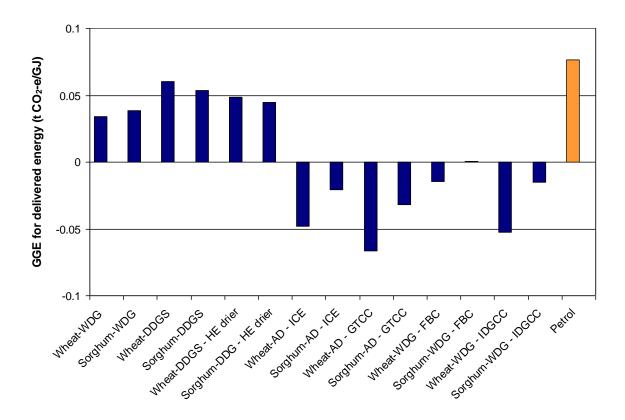


Figure 15 Life cycle GGE for the production and use of ethanol for all cases, compared to petrol (2006 basis).

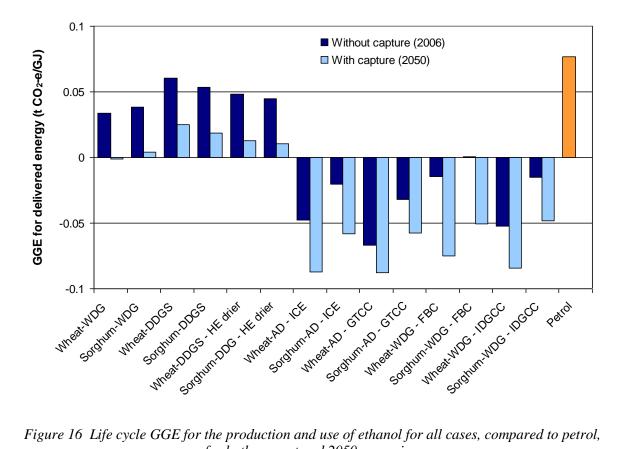


Figure 16 Life cycle GGE for the production and use of ethanol for all cases, compared to petrol, for both current and 2050 scenarios.

From Figure 15, it can be seen that, using current technology, the life cycle GGEs for ethanol are always less than those for petrol, with ethanol cases involving export electricity being very much lower. When a comparison is made with the 2050 scenario included (Figure 15), the projected use of CO_2 capture technologies further reduce the GGEs for the ethanol cases, compared to petrol.

It is clear from these results that ethanol is favoured over petrol as a transport fuel, when only GGE is used for selection. There are of course a number of other issues which need to be taken into account, such as availability, performance in the transport fleet, economics, *etc*.

7.5. Comparison with other studies

There have been a number of LCAs carried out internationally on ethanol production from grain, although in Australia there has only been limited work^[108]. These LCAs have usually been focussed on GGEs and resource energy, and, for many international studies, have been carried out to quantify the energy available from the product ethanol, net of credits, compared to the fossil energy inputs in the production chain.

Because of the importance of the latter, this energy balance is discussed in more detail in a separate section below. In international studies, water data is noticeable by its absence. It should also be noted that there are no published LCAs for ethanol production from grains, in which the stillage is biodigested; the only relevant other work is an internal CSIRO study^[102] by Beer.

In view of the large differences in grain yields in different regions and countries, and differences in nitrogenous fertiliser practice, variations in LCA results are to be expected, particularly up to the grain production stage.

Domestic

The most comprehensive grains related, publicly available, LCA, is that undertaken in 2004 by Curtin University for the Grains R&D Corporation. This study^[109] considered products from Western Australian grains, and was very detailed, with extensive data collection from grain farmers. The wheat-to-beer data (for the pre-farming and farming stage) is relevant to this report.

The functional unit in these studies was a loaf of bread. These results were converted to a tonne of wheat at the farm gate and the data is given in Table 28, with the results from the present study included for comparison.

Parameter	Unit	Value	Present study
Resource energy	GJ	6 (read from bar graph)	1.91
GGEs	t CO _{2-e}	0.32 (80% from N ₂ O)	0.22*
Process water	m ³	0.56	0.61

* the GGE value without carbon sequestration in the grain is used for the comparison, to enable the same basis as the study by Curtin University.

Note that this GGE value is in reasonable agreement with the value for wheat production in the Gunnedah region from the present study, provided no account is taken of the carbon

sequestered in the grain. There is, however, a large difference in resource energy consumption– possibly because of differences in nitrogen fertiliser use (although this should also influence the amount of nitrous oxides released). The value for process water is similar to that from the current study.

Van Berkel has also carried out an LCA for starch production based on Queensland wheat^[110], and, for wheat production, has calculated a resource energy of 4.25 GJ/t starch, and GGE from fossil fuel combustion and electricity use of $0.424 \text{ tCO}_{2-e}/t$ starch. Converted to a wheat basis, assuming that the wheat contains 65% of starch extracted in the process, these values become 2.8 GJ/t for resource energy, and 0.28 tCO_{2-e} for GGE (again without carbon sequestration in the grain), both very similar to the current study.

International

Pringer and Steinberg^[111] have recently given estimates of 3.9 GJ/t for wheat, noting that the dominant contribution is energy embodied in nitrogen fertiliser at 47% of the total energy input, followed by diesel fuel at 25%, with smaller contributions from energy embodied in seed grain, petrol, electricity, and phosphorus fertiliser. Again, the importance of nitrogenous fertiliser is noted (when comparing results between different climatic regimes, the relationship between nitrogenous input and nitrous oxide emissions will vary, resulting in somewhat different overall GGEs).

A 2003 report from the UK^[112] analysed carbon and energy balances for a range of biofuel options, including the production of ethanol from wheat, as well as wheat straw. For comparison, the values for petrol production from oil are also included. The results are expressed on a kL of ethanol basis (including the petrol case) in Table 29. Note, the conversions have assumed a gross CV for ethanol of 29.74 GJ/t, with a density of 0.79 kg/L. IPCC 1996 global warming potentials of 21 for CH₄ and 310 for N₂O were used in deriving a total CO₂ equivalent value for GGEs.

	Sheffield-Hallam University (UK)		Present study	
	Energy (GJ/kL)	Total GGE (t CO _{2-e} /kL)	Energy (GJ/kL)	Total GGE (t CO _{2-e} /kL)
Ethanol from wheat	10.9	0.66	12.8	-0.90
Ethanol from straw	-0.66	0.30		
Unleaded petrol from oil	27.9	1.90		

Table 29 Energy and GGEs for ethanol production - UK study

While the value for resource energy in the present study is comparable to that from the UK study, the value for GGE is very different. This difference is probably due to 2 key factors; the UK study did not include:

- The CO₂ equivalent of the grain (*ie* due to its carbon content).
- Displacement credits (for wheat) for the feed value of DDGS.

Note, the negative value for energy consumption (and methane emissions) for the ethanol from straw case (UK study) is due to the high level of credits for export of electricity and acetic acid. The largest source of GGEs for the ethanol from straw case is the additional ammonium nitrate fertiliser to replace the N lost due to straw removal. As can be seen, this is substantially offset by the credits. It should be noted that such conversion of straw (cellulose) to ethanol is not yet commercially available, but the calculation serves to show the environmental benefits of using such a biomass source, from an LCA perspective.

Comparison of fossil energy inputs to energy available from the bioethanol

There has been considerable debate about the merits of bioethanol production compared to petrol on the basis of equivalent energy delivered (as fuel for an internal combustion engine). While the focus has been generally on fossil energy replacement, there have been several recent studies where GGE have also been considered. This has resulted in a number of different ways of expressing the comparisons:

- Net energy = (energy delivered as liquid fuel) (fossil energy for production)
 - also expressed as a % or a ratio
- Net liquid fuel = (energy delivered as liquid fuel) (energy from liquid fossil fuels for production)
- GGE for energy delivered = GGE for the production and combustion)

A key recent study was carried out by the Argonne National laboratory to compare the net energy value for ethanol produced from corn as a function of time for the various studies^[113], and these are shown in Figure 17 below. For comparison, results for base cases in the present study are included.

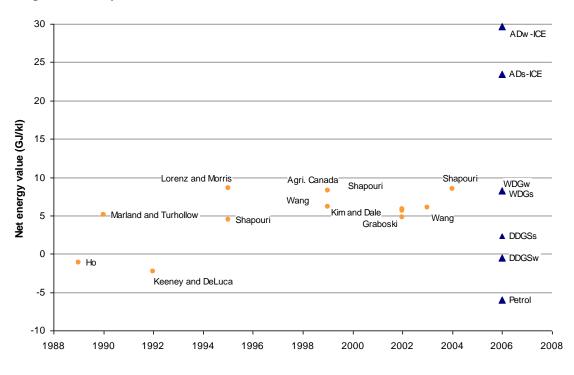


Figure 17 Net energy value for ethanol production from corn, with current wheat and sorghum cases

It can be seen that, on a fossil fuel basis, the production of ethanol from corn results in more energy than the fossil energy used in its production.

The results from the present study are also shown for the 3 base cases (WDG, DDGS, AD-ICE):

- For WDG, the results are comparable with those of other recent studies.
- For DDGS for wheat and sorghum, there is no significant net energy benefit, due to the large amount of energy required for drying. The value for sorghum is higher due to the higher ethanol yield and the correspondingly lower amount of WDG for drying.

- Anaerobic digestion (with electricity generation using conventional internal combustion engines) gives a marked improvement in net energy 2.5-3x higher than for WDG (or from the other studies shown).
 - the net energy is actually higher than the energy content in the ethanol product.

Another major comparative study (corn based) was carried out by the University of California, Berkeley. The results of this study are summarised in Figure 18, with the base case (WDG, DDGS, AD-ICE) results from the current study also included.

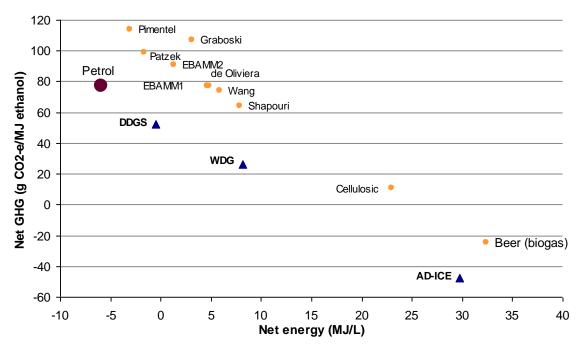


Figure 18 Net GGEs versus net energy for ethanol production from corn, with current wheat cases)

It can be seen that the results of studies by Pimentel and Patzek are inconsistent with those of others, and also with the present study.

The overall analysis of the present study provides similar results to the Argonne study from a net energy point of view. The low net GGE value for cellulosic feedstock is due to the generation and export of electricity from combustion of the lignin, a by-product of ethanol production using this feed. For the present study, this credit was even larger for the AD-ICE case, probably due to the high CO_2 intensity of the NSW grid (compared to the USA).

An alternative to the use of biomass for ethanol production, whether from grain, or in the future from cellulosic material, is to use the biomass as a fuel to raise steam and produce electricity, perhaps as part of a combined heat and power scheme. A report from CONCAWE^[114] has concluded that "the process is considerably simpler, and the crops can now be selected solely on their ability to produce large amounts of biomass from a given land area. Such crops could include various grass varieties or fast-growing wood (short rotation coppicing). Adapted grass varieties can produce some 200 GJ/ha of net biomass energy (i.e. after accounting for the production energy), compared to 30 to 60 in the best scenario for ethanol. When used for power generation this could displace an equivalent fossil fuel energy with a CO₂ emission factor of say 80kg CO₂/GJ (typical of heavy fuel oil or intermediate between gas and coal). This would equate to 16t CO₂/ha, four to eight times more than could be achieved through ethanol production and use".

This emphasis on bioenergy, rather than liquid biofuel is worth considering in any further study of the use of land based biomass to reduce Australia's greenhouse gas emissions, and

to improve energy security. The water use aspects of these alternative bioenergy crops would also need careful consideration.

8. TECHNO-ECONOMIC EVALUATION

The objective of this analysis is to determine the cost of ethanol production for a number of process options, and for a range of economic variables.

As for the LCA, there were 7 cases chosen for the production of ethanol and processing of the stillage – for both wheat and sorghum:

- 1. WDG-WDG transported direct to adjacent feedlot.
- 2. DDGS-DDGS with conventional drying.
- 3. DDGS HE dryer-DDGS with high efficiency drying.
- 4. AD–ICE-Anaerobic digestion, with gas internal combustion engine electricity generation (33% efficiency*)
- 5. AD–GTCC-Anaerobic digestion, with gas turbine combined cycle electricity generation (50% efficiency)
- 6. WDG-FBC-WDG for electricity generation by fluidised bed combustion (20% efficiency).
- 7. WDG-IDGCC-WDG for electricity generation using integrated drying and gasification combined cycle (40% efficiency).

It is realised that there are many factors that will affect the overall economics of new ethanol production facilities in Australia. However, the following analysis is provided to indicate suggested outcomes, as a basis for identifying the major contributors to the ultimate ethanol production cost, together with some of the sensitivities for various production and feedstock options.

It should be noted that data has been obtained/derived from typical information reported by technology providers and project developers. Obviously much more detailed engineering and plant specific information would be required to develop more accurate estimates. BBI International, one of the USA based companies working with new developers, typically estimate that feasibility studies to develop detailed project plans and economics related to a particular greenfield site cost in the vicinity of US\$1 M. Current developers have indicated that significant expenditure, well above this figure, needs to be incurred to reach the stage where funding can be guaranteed and a Development Application lodged.

The location will have a particular bearing on the availability, transport, type and cost of grain, type and cost of energy, as well as some specific design features of the plant and the potential for sale and export of co-products.

Variable costs (administration, marketing, interest, licence fees, taxes, depreciation *etc*) will change for each plant, location and other corporate and local parameters, but typically amount to an additional 7-10 c/L. Capital funding and recovery of investment for the plant will be affected by the levels of debt and equity financing. It seems that a number of proposed Australian plants will involve significant amounts of capital from equity investments. Hence, total overall costs will vary for individual plants and financing arrangements.

The nominal capital cost for a 160 ML/y plant is A\$200 M. This cost is considered a realistic overall cost that includes allowances for a number of essential items (including licensing, cash reserves, insurance etc), in addition to the ethanol plant with digester and power station, and other associated equipment. The typical capital cost for a conventional ethanol plant alone in Australia is of the order of \$1.0/L ethanol produced annually (in this case \$160 M). As this equates to only 15-20% of the production cost of ethanol, minor

variations in capital cost will only have a minimal effect on the overall cost when compared to the much larger variations resulting from grain costs.

It is emphasised that the costs in this section relate to ethanol <u>production</u> costs, with no consideration of government subsidies or charges.

Basis and assumptions

The analysis involves a number of key assumptions and leads to a matrix of cases. These are summarised in Table 30, and further details are provided in Table 31. Note that the base case cost of electricity of 4c/kWh was based on a recent NSW proposal, and may have been a project specific agreement. Grain prices were chosen to represent current values for wheat and sorghum (\$200-250/t), with a higher price of \$300/t chosen to represent a potential future situation (associated with changes in demand and supply, higher fuel and fertiliser costs, lower average rainfall).

	Unit	Base	Medium	High
Grain	\$/t (@10% moisture)	200	250	300
Energy cost				
Electricity	c/kWh	4	5.5	7
Gas	\$/GJ	4	5.5	7
Value of CO ₂	\$/t CO ₂ -e	0	10	30

Table 30 Matrix of key cost variables

The techno-economics considers the base cases (cases 1, 2 and 4 above), followed by a consideration of ethanol production costs as a function of the key cost variables. In addition, to compare the trade-offs between drying of WDG and the reduced transportation costs for DDGS.

Assumption	Comment	Value
Ethanol production	ML/yr	160
Capital cost of ethanol plant	\$M	200
Levelised carrying charge	pa	12%
Grain cost	\$/t	200-300
Cost of natural gas	\$/GJ	4-7
CO ₂ abatement credit	%/t CO ₂ -e	0-30
Basis for CO ₂ abatement credit	Overall GGE	-
Power plant capital cost		
ICE	\$M/MW	1.5
GTCC	\$M/MW	1.1
FBC	\$M/MW	1.5
IDGCC	\$M/MW	1.8
Electricity capital charge	ра	12%
Electricity O&M	ра	4%
Power station capacity factor		95%
Dryer capital cost (conventional)		
Wheat	\$M	8
Sorghum	\$M	5.2
Dryer capital cost (high efficiency)		
Wheat	\$M	10
Sorghum	\$M	6.5
Miscellaneous costs		
Anaerobic digestion cases	c/L	4
Other cases	c/L	0.4
R&M costs	c/L	1
Administration costs	c/L	1
Chemical costs		
Anaerobic digestion chemicals	c/L	7.0
Chemicals other cases	c/L	3.1
Credits		
Electricity cost/credit	c/kWh	4-7
Organic fertiliser credit	\$/t	250
Aqueous ammonia credit	\$/t	100
Greenpower electricity credit	c/kWh	2.5
DDG credit	of grain cost	85%
WDG credit	of grain cost	25%

Table 31 Basis and assumptions for the techno-economics

8.1. Results

The results are presented for the bases cases as a summary table, together with graphs in which the values for GGE are varied (0, 10 and 30/t GGE).

This is followed by a comparison of DDGS with WDG, for a range of transportation distances. Finally, ethanol production costs for a number of alternative stillage processing options are given.

8.1.1 Base cases

The conditions used for the base cases are given in Table 32.

			v				
			Wheat			Sorghum	
Cases		WDG	DDGS	AD-ICE	WDG	DDGS	AD-ICE
Attribute							
Stillage processing			DDG	anaerobic		DDG	anaerobic
				digestion			digestion
Grain moisture	%	10	10	10	12	12	12
Grain starch	% db		65.3	65.3		74.6	74.6
Grain consumption	t/y		439,000	439,000		393,000	393,000
Grain cost	\$/t	200-300	200-300	200-300	200-300	200-300	200-300
Distillers grain price	% of grain	25%	85%		25%	85%	
Electricity cost/price	c/kWh	4-7	4-7	4-7	4-7	4-7	4-7
Natural gas cost	\$/GJ	4-7	4-7		4-7	4-7	
Co-products							
Ammoniacal liquor	t/y		-	16,000		-	10,000
Organic fertiliser	t/y		-	70,000		-	45,000
Export electricity	MWh		-	158,400		-	96,000
WDG	t/y	480,000		-	307,200		
DDGS	t/y		160,000			102,400	-

Table 32 Base case studies for techno-economics

The resulting ethanol production costs for these cases are shown in Table 33, and in Figure 19 to Figure 21.

Stillage option	Grain	Energy price/cost	Ethanol produc	ction cost (c/L)
	\$/t	(c/kWh or \$/GJ)	Wheat	Sorghum
WDG	200	4	62.9	62.4
DDGS	200	4	64.6	63.5
AD-ICE	200	4	70.5	69.4
WDG	250	4	72.8	72.2
DDGS	250	4	74.0	74.1
AD-ICE	250	4	84.2	81.7
WDG	300	4	82.8	82.1
DDGS	300	4	83.5	83.6
AD-ICE	300	4	97.9	94.0
WDG	200	5.5	62.9	62.4
DDGS	200	5.5	65.7	65.8
AD-ICE	200	5.5	69.0	68.5
WDG	250	5.5	72.8	72.2
DDGS	250	5.5	75.2	75.3
AD-ICE	250	5.5	82.7	80.8
WDG	300	5.5	82.8	82.1
DDGS	300	5.5	84.7	84.8
AD-ICE	300	5.5	96.4	93.1
WDG	200	7	62.9	62.4
DDGS	200	7	66.9	67.0
AD-ICE	200	7	67.5	67.6
WDG	250	7	72.8	72.2
DDGS	250	7	76.4	76.5
AD-ICE	250	7	81.2	79.9
WDG	300	7	82.8	82.1
DDGS	300	7	85.9	86.0
AD-ICE	300	7	94.9	92.2

 Table 33 Cost of ethanol production for the base cases (no value on GGE)
 Image: Cost of ethanol production for the base cases (no value on GGE)

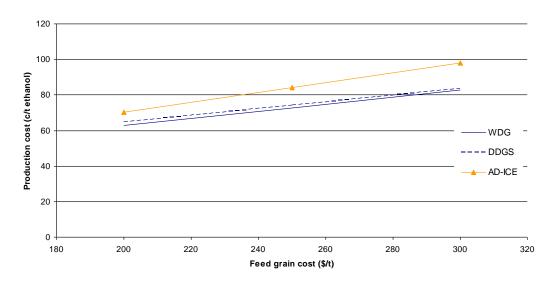


Figure 19 Ethanol production cost for electricity at 4c/kWh and gas at \$4/GJ

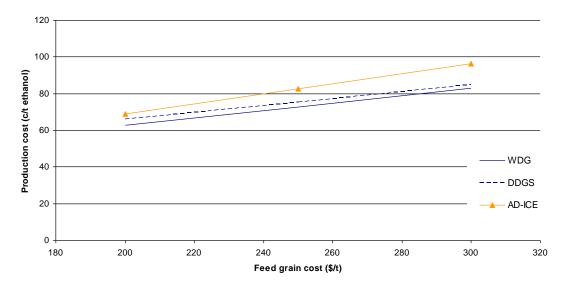


Figure 20 Ethanol production cost for electricity at 5.5c/kWh and gas at \$5.5/GJ

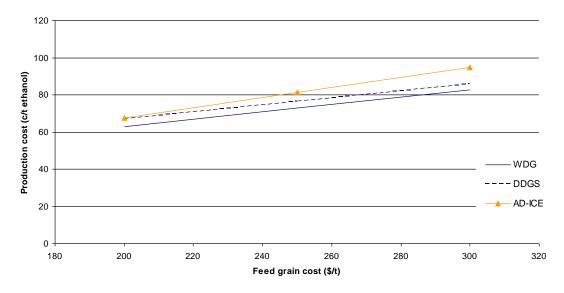


Figure 21 Ethanol production cost for electricity at 7c/kWh and gas at \$7/GJ

These results show that, for a zero value for GGE, the cost of ethanol production is:

- Dominated by the grain price over the range considered.
- Is not significantly affected by the type of feed replacement by-product (*ie* WDG or DDGS).
- Increased by 6-7c/L for the base conditions, and up to 14c/L for high grain cost. This increase is reduced by higher energy costs.
- Not significantly affected by grain type, for the assumptions used.

8.1.2 Trade-off between drying and transport

Drying of stillage is generally assumed to be required to enable distribution of distillers grain to feedlots which are not in the near vicinity to the ethanol plant. A number of different dryers and options are available^[115,116], based on various designs and energy recovery systems. In addition to the need for a reliable market, the cost of the drying operation will play an important role in assessing the value of credits for this co-product from the ethanol process.

The following analysis is included to give an indication of the costs associated with the drying operation. Typically, dryers use natural gas or steam as the heating medium. In some designs, recuperation of some of the energy (for example by recirculating a proportion of the hot exhaust gases to the feed section of the dryer) is incorporated to reduce the input energy consumption. To provide an indication of the relative drying costs, budget data provided by the GEA Process Division of Barr-Rosin for a basic partial gas recycle, direct fired rotary dryer has been used.

Table 34 gives the basis for the calculation of drying costs, for the 3 levels of energy costs.

	Unit	Current	Medium energy cost	High energy cost
WDG (70% moisture)	t/y	481,000	481,000	481,000
DDGS (10% moisture)	t/y	160,000	160,000	160,000
Dryer capacity (moisture removed)	t/h	37	37	37
Drying plant				
Capital cost	\$M	8	8	8
Levelised carrying charge	%pa	10%	10%	10%
Electrical power	MW	2.25	2.25	2.25
Electricity cost	c/kWh	4.00	5.50	7.00
Natural gas rate	MW	34	34	34
Gas cost	\$/GJ	4.0	5.5	7.0
Operating costs				
Capital charge	\$/t DDGS	5.0	5.0	5.0
Electricity	\$/t DDGS	4.93	6.78	8.62
Gas	\$/t DDGS	26.81	36.86	46.91
Total drying cost				
	\$/t DDGS	36.7	48.6	60.5
	c/L ethanol	3.7	4.9	6.1

Table 34 Basis for estimates (based on nominal 160 ML/y ethanol plant

This analysis shows that drying will cost around \$36/t DDGS with current NSW energy costs (as quoted for a recent ethanol plant proposal); however, this cost would nearly double with high energy costs.

The costs of transport of WDG are compared to those for DDGS, on an equivalent moisture basis, in Figure 22. The cost of transport has been assumed to be 20 c/t.km.

The GGE associated with this comparison are shown in Figure 23, with the GGE for the drying of the WDG (to produce DDGS), using both normal and high drying efficiencies, given as the intersection with the ordinate.

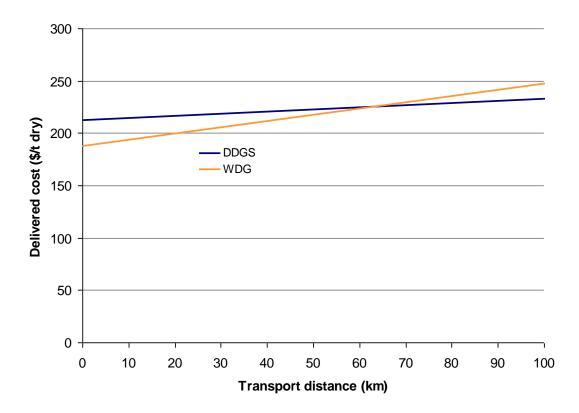


Figure 22 Comparison of delivered costs for DDGS and an equivalent amount of WDG, assuming a transport cost of \$0.20/t.km and a grain price of \$250/t.

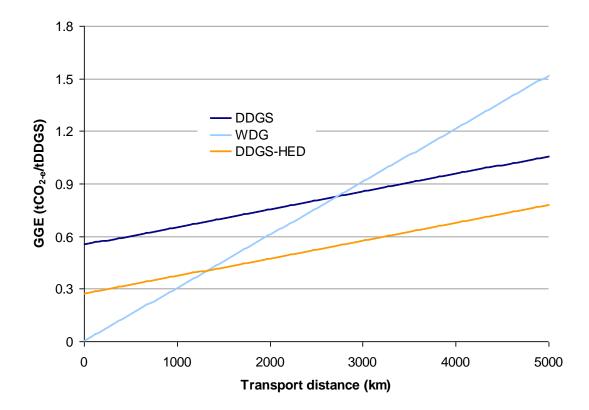


Figure 23 Comparison of GGE for drying/transportation for DDGS to an equivalent amount of WDG

From a cost perspective, Figure 22 shows that, for a transport cost of 20 c/t.km and a grain cost of \$250/t, WDG can only be transported around 60 km before it is economically preferable to produce DDGS. For the lower grain price, the distance reduces to 50 km, and for the higher grain price it increases to 80 km.

From a GGE perspective, Figure 23 shows that the WDG can be transported up to almost 3000 km before the GGE exceeds those associated with producing and transporting the DDGS, when the lower efficiency drying process is used. When the higher efficiency dryer is used, the distance reduces to around 1000 km.

8.1.3 Alternative stillage processing options

The wider range of case studies has been compared to the base cases for the other stillage processing options (cases 3, 5, 6 and 7). In addition, a sensitivity analysis has been carried out to show the effect of grain price, local electricity price/cost, and the value of CO_2 .

The 4 alternative cases are based on the technologies that are most likely to be utilised in integrated grain based plants to be built in Australia in the foreseeable future.

The data and assumptions related to the four case studies are summarized in Table 35.

			Wheat		Sorghum		
Cases Attribute		AD- GTCC	WDG- FBC	WDG- IDGCC	AD- GTCC	WDG- FBC	WDG- IDGCC
Grain moisture	%	10	10	10	12	12	12
Grain starch	% db	65.3	65.3	65.3	74.6	74.6	74.6
Grain consumption	t/y	439,000	439,000	439,000	393,000	393,000	393,000
Grain cost	\$/t	200-300	200-300	200-300	200-300	200-300	200-300
Electricity cost/price	c/kWh	4-7	4-7	4-7	4-7	4-7	4-7
Natural gas cost	\$/GJ	4-7	4-7		4-7	4-7	
Co-products							
Ammoniacal liquor	t/y	16,000	-	-	10,000	-	-
Organic fertiliser	t/y	70,000	-	-	45,000	-	-
Export electricity	MWh	252,800	123,200	270,400	156,800	73,600	168,000

Table 35 Alternative case studies for techno-economics

The results for all of the cases and ranges of variables are given in Table 36 (nil value for GGE), Table 37 (\$10/t GGE) and Table 38 (\$30/t GGE).

Alternative stillage process	Grain \$/t	Electricity c/kWh	Ethanol produc Wheat	ction price (c/L) Sorghum
DDGS-HED	200	4	63.1	62.5
AD-GTCC	200	4	67.0	67.2
WDG-FBC	200	4	75.5	70.8
WDG-IDGCC	200	4	73.2	69.4
DDGS-HED	250	4	72.6	72.6
AD-GTCC	250	4	80.7	79.5
WDG-FBC	250	4	89.2	83.1
WDG-IDGCC	250	4	87.0	81.7
DDGS-HED	300	4	82.0	82.1
AD-GTCC	300	4	94.4	91.8
WDG-FBC	300	4	103.0	95.4
WDG-IDGCC	300	4	100.7	94.0
DDGS-HED	200	5.5	63.7	63.7
AD-GTCC	200	5.5	64.6	65.7
WDG-FBC	200	5.5	74.4	70.2
WDG-IDGCC	200	5.5	70.7	67.8
DDGS-HED	250	5.5	73.2	73.2
AD-GTCC	250	5.5	78.4	78.0
WDG-FBC	250	5.5	88.1	82.4
WDG-IDGCC	250	5.5	84.4	80.1
DDGS-HED	300	5.5	82.6	82.7
AD-GTCC	300	5.5	92.1	90.3
WDG-FBC	300	5.5	101.8	94.7
WDG-IDGCC	300	5.5	98.1	92.4
DDGS-HED	200	7	64.3	64.3
AD-GTCC	200	7	62.3	64.3
WDG-FBC	200	7	73.2	69.5
WDG-IDGCC	200	7	68.2	66.2
DDGS-HED	250	7	73.7	73.8
AD-GTCC	250	7	76.0	76.6
WDG-FBC	250	7	86.9	81.7
WDG-IDGCC	250	7	81.9	78.5
DDGS-HED	300	7	83.2	83.3
AD-GTCC	300	7	89.7	88.8
WDG-FBC	300	7	100.6	94.0
WDG-IDGCC	300	7	95.6	90.8

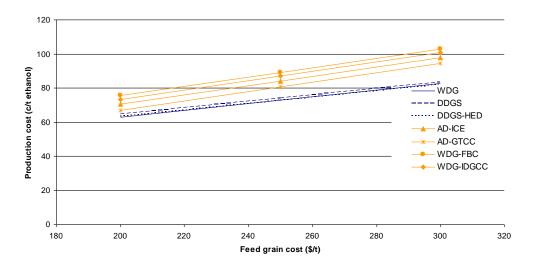
Table 36 Cost of ethanol production for alternative stillage processing (nil value for GGE)

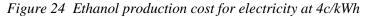
Alternative stillage process	Grain \$/t	Electricity c/kWh	Ethanol produc Wheat	tion price (c/L) Sorghum
DDGS-HED	200	4	64.3	64.2
AD-GTCC	200	4	65.4	66.4
WDG-FBC	200	4	75.2	70.8
WDG-IDGCC	200	4	72.0	66.7
DDGS-HED	250	4	73.7	73.7
AD-GTCC	250	4	79.1	78.7
WDG-FBC	250	4	88.9	83.1
WDG-IDGCC	250	4	85.7	79.0
DDGS-HED	300	4	83.2	83.2
AD-GTCC	300	4	92.8	91.0
WDG-FBC	300	4	102.6	95.4
WDG-IDGCC	300	4	99.4	94.3
DDGS-HED	200	5.5	64.8	64.8
AD-GTCC	200	5.5	63.0	65.0
WDG-FBC	200	5.5	74.0	70.2
WDG-IDGCC	200	5.5	69.4	65.1
DDGS-HED	250	5.5	74.3	74.3
AD-GTCC	250	5.5	76.7	77.3
WDG-FBC	250	5.5	87.7	82.4
WDG-IDGCC	250	5.5	83.1	80.5
DDGS-HED	300	5.5	83.8	83.8
AD-GTCC	300	5.5	90.4	89.5
WDG-FBC	300	5.5	101.5	94.7
WDG-IDGCC	300	5.5	96.9	92.7
DDGS-HED	200	7	65.4	65.4
AD-GTCC	200	7	60.6	63.5
WDG-FBC	200	7	72.9	69.5
WDG-IDGCC	200	7	66.9	63.5
DDGS-HED	250	7	74.9	74.9
AD-GTCC	250	7	74.4	75.8
WDG-FBC	250	7	86.6	81.7
WDG-IDGCC	250	7	80.6	78.9
DDGS-HED	300	7	84.4	84.4
AD-GTCC	300	7	88.1	88.1
WDG-FBC	300	7	100.3	94.0
WDG-IDGCC	300	7	94.3	91.2

 Table 37 Cost of ethanol production for alternative stillage processing (\$10/t GGE)

Alternative stillage process	Grain \$/t	Electricity c/kWh	Ethanol production price (c. Wheat Sorghu	
DDGS-HED	200	4	66.6	66.3
AD-GTCC	200	4	62.1	64.9
WDG-FBC	200	4	74.5	70.8
WDG-IDGCC	200	4	69.4	70.5
DDGS-HED	250	4	76.1	75.9
AD-GTCC	250	4	75.8	77.2
WDG-FBC	250	4	88.2	83.1
WDG-IDGCC	250	4	83.1	82.8
DDGS-HED	300	4	85.5	85.4
AD-GTCC	300	4	89.6	89.4
WDG-FBC	300	4	101.9	95.4
WDG-IDGCC	300	4	96.8	95.0
DDGS-HED	200	5.5	67.2	66.9
AD-GTCC	200	5.5	59.8	63.4
WDG-FBC	200	5.5	73.3	70.2
WDG-IDGCC	200	5.5	66.8	68.9
DDGS-HED	250	5.5	76.6	76.5
AD-GTCC	250	5.5	73.5	75.7
WDG-FBC	250	5.5	87.1	82.4
WDG-IDGCC	250	5.5	80.6	81.2
DDGS-HED	300	5.5	86.1	86.0
AD-GTCC	300	5.5	87.2	88.0
WDG-FBC	300	5.5	100.8	94.7
WDG-IDGCC	300	5.5	94.3	93.5
DDGS-HED	200	7	67.8	67.5
AD-GTCC	200	7	57.4	61.9
WDG-FBC	200	7	72.2	69.5
WDG-IDGCC	200	7	64.3	67.3
DDGS-HED	250	7	77.2	77.1
AD-GTCC	250	7	71.1	74.2
WDG-FBC	250	7	85.9	81.7
WDG-IDGCC	250	7	78.0	79.6
DDGS-HED	300	7	86.7	86.6
AD-GTCC	300	7	84.8	86.5
WDG-FBC	300	7	99.6	94.0
WDG-IDGCC	300	7	91.8	91.9

Table 38 Cost of ethanol production for alternative stillage processing (\$30/t GGE)





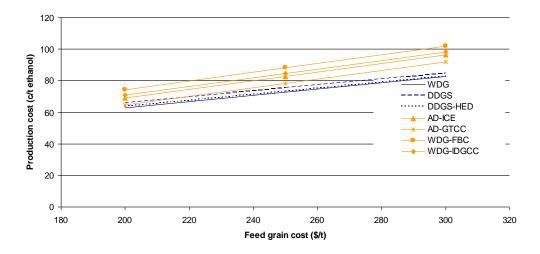


Figure 25 Ethanol production cost for electricity at 5.5c/kWh

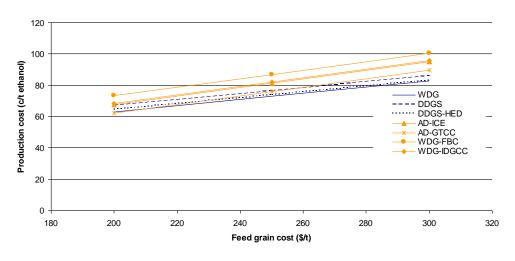


Figure 26 Ethanol production cost for electricity at 7c/kWh

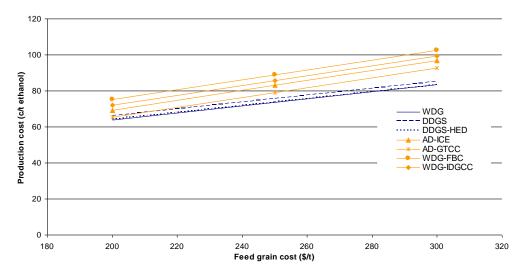


Figure 27 Ethanol production cost for electricity at 4c/kWh and CO₂ valued at \$10/t

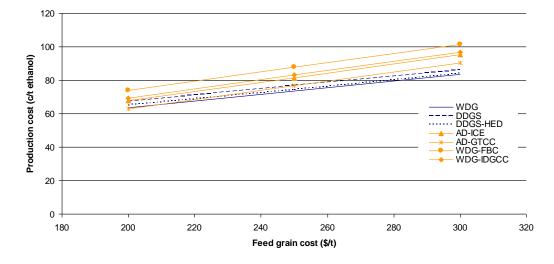


Figure 28 Ethanol production cost for electricity at 5.5c/kWh and CO₂ valued at \$10/t

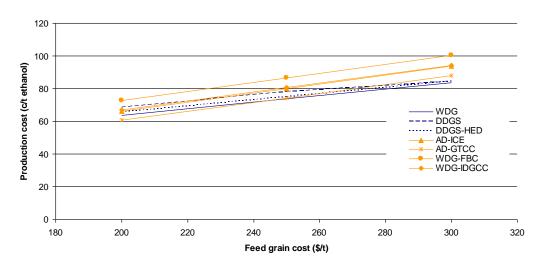


Figure 29 Ethanol production cost for electricity at 7c/kWh and CO₂ valued at \$10/t

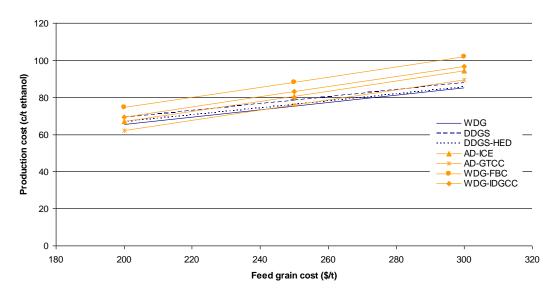


Figure 30 Ethanol production cost for electricity at 4c/kWh and CO₂ valued at \$30/t

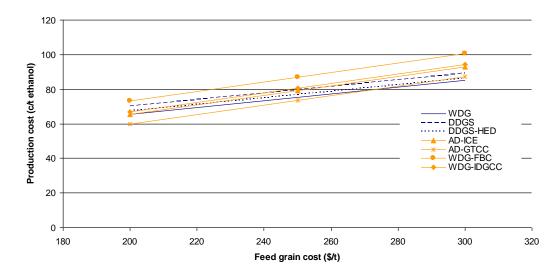


Figure 31 Ethanol production cost for electricity at 5.5c/kWh and CO₂ valued at \$30/t

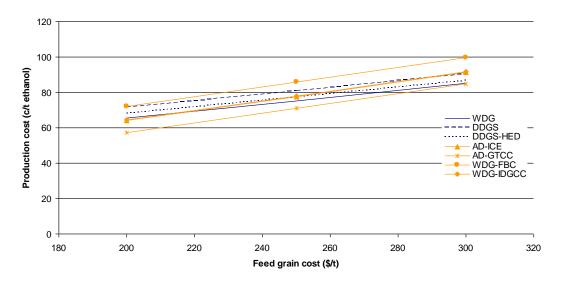


Figure 32 Ethanol production cost for electricity at 7c/kWh and CO₂ valued at \$30/t

The results show that the cost of ethanol production is:

- Increased by 3-12c/L for the alternative processing options (under base conditions).
- The AD-GTCC gives the lowest overall cost of the power generation options, due to its high efficiency and lowest capital cost.
- Lower, for power generation cases, when a value is attributed to GGE;
 - lowest (57c/L) for AD-GTCC, with the high energy cost case and \$30/t GGE.

A breakdown of ethanol production costs is shown for the low, medium and high cost cases (from wheat) in Figure 33, Figure 34 and Figure 35, respectively.

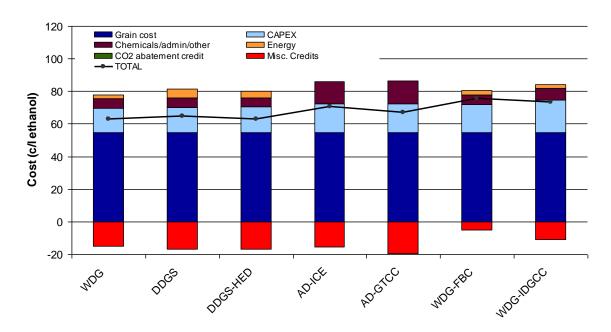


Figure 33 Breakdown of ethanol production cost for electricity at grain at \$200/t, 4c/kWh and CO_2 valued at \$0/t

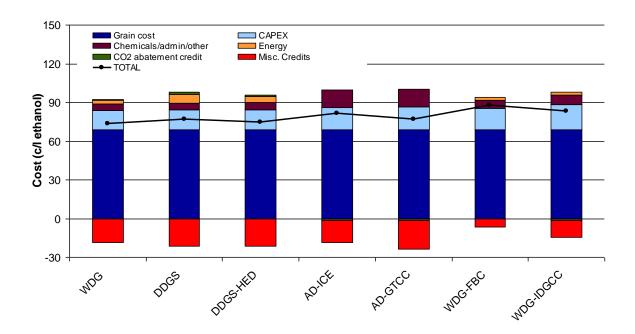
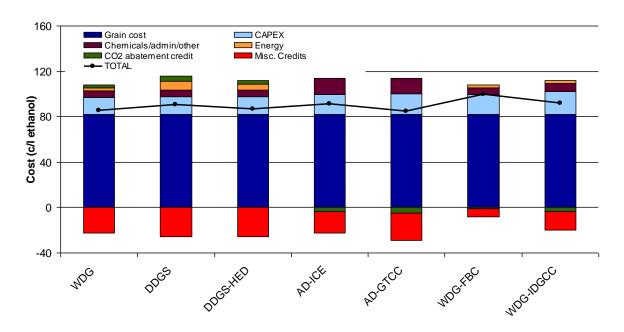


Figure 34 Breakdown of ethanol production cost for electricity at grain at \$250/t, 5.5c/kWh and CO_2 valued at \$10/t



*Figure 35 Breakdown of ethanol production cost for electricity at grain at \$300/t, 7c/kWh and CO*₂ *valued at \$30/t*

Electricity generation

The amount of power generated and exported is very dependent on the amount of stillage, the type of stillage processing, and the generation technology. The results for the average generated and export electricity for the base cases are shown in Table 39, with the results for the alternative stillage processing options shown in

Table 40.

		Wheat					1
Cases		WDG	DDGS	AD-ICE	WDG	DDGS	AD-ICE
Average generation	(MW)	-	-	21.9	-	-	14.1
Average export electricity	(MW)	-	-	19.0	-	-	11.5

Table 39 Power generation for the base cases (160 MLpa plant)

Table 40 Power generation for the alternative stillage processing options (160 MLpa plant)

		Wheat				Sorghum	
Cases Attribute		AD- GTCC	WDG- FBC	WDG- IDGCC	AD- GTCC	WDG- FBC	WDG- IDGCC
Average generation	(MW)	33.2	17.6	35.3	21.4	11.4	22.7
Average export electricity	(MW)	30.4	14.8	32.5	18.8	8.8	20.2

The amount of electricity used by ethanol production is small compared to that which can be generated from stillage processing. This results in significant export electricity, particularly for the high efficiency generation technology. It should be noted that, while these higher efficiencies are not readily achievable at the scale chosen for the ethanol plant, they could be achieved with 2-3x larger ethanol plants (as are being constructed in the USA).

9. CONCLUSIONS

9.1.LCA

The LCA study highlighted the importance of considering a number of alternative technology options related to the processing of the stillage, and these were also included in the techno-economic analysis. More efficient technologies can be used for converting biogas or WDG to electricity, and these substantially reduce the resource energy requirement and GGEs, as well as reducing water consumption.

Resource energy

For grain production, fertiliser production is the major component (70%) of resource energy, with the fuel for agricultural activities of secondary importance: 20% for wheat, and only 10% for sorghum.

When the grain is processed to ethanol, the resource energy is very dependent on the processing of the stillage, and the applicable by-product credits. For direct sale of WDG, the resource energy is considerably lower than that for DDGS, due to the large amount of energy required for drying (can be substantially reduced using a higher efficiency process). When the stillage is anaerobically digested, the resource energy becomes negative, since there are:

- no requirements for purchased electricity or natural gas for ethanol production, and
- significant credits for by-product fertilisers and exported electricity.

If the WDG is combusted to produce electricity (requires a technology similar to high moisture lignite or biomass), a negative overall resource energy is again produced.

It is interesting to note that the overall resource energy is the same, whether the stillage is anaerobically digested with the methane converted to electricity at 50% efficiency, or the WDG is directly combusted to produce electricity at an overall efficiency of 40%.

GGEs

For grain production, the majority of the GGEs come from the production of nitrogenous fertiliser, and the nitrous oxide emissions from its use. However, the overall GGE is dominated by the CO_2 taken up by the grain through photosynthesis. This leads to a negative GGE for all cases.

When the grain is processed to ethanol, GGEs are very dependent on the method of processing the stillage, and what by-product credits are applicable. For direct sale of WDG, the GGE value is lower than that when DDGS is the by-product, due to the emissions associated with drying (again, reduced by a higher efficiency process). The GGE increases with the feed grain credit from WDG/DDGS – as this by-product displaces grain production and lowers the CO_2 being sequestered by photosynthesis. When the transportation of WDG is compared with that for DDGS on a comparable moisture basis, it was shown that WDG could be transported for a large distance (>1000 km), before the increased GGEs from transport of the higher moisture content WDG exceeds the GGE from drying and transport of the DDGS.

Anaerobic digestion of the stillage, gives lower emissions associated with ethanol production, due to the use of combined heat and power; *ie* the use of waste heat from power generation for the fermentation. A similar conclusion applies to the combustion of WDG for electricity generation.

All of the alternative technologies reduce the overall GGE, with the highest efficiency electricity generation case (with NGCC and IDGCC) virtually offsetting the upstream GGEs for ethanol production.

Process water consumption

For grain production, there is a significant amount of process (fresh) water associated with fertiliser production. However, the amount of water used for growing the grain (soil moisture and rainfall) is over 2 orders of magnitude higher ($500 - 1000 \text{ m}^3\text{H}_2\text{O/t}$ of grain).

The process water consumption per kL of ethanol is dependent on whether the stillage is biodigested, and the level of credits associated with exported electricity. When WDG or DDGS are by-products, the water associated with the WDG is lost to the process, except for the higher efficiency drying case using vapour recompression. If the WDG is combusted to produce electricity, the water content of the WDG is also lost.

In the biodigestion cases, water is recirculated after biodigestion, and this and the credit from electricity leads to the lowest process water consumption.

As noted above, in comparison with these process water totals, the water used for growing the grain is very much higher.

Comparison with other studies

In comparison with the other Australian studies on wheat production, similar GGEs and process water values were obtained, when compared on a similar basis. The values for resource energy, however, vary considerably (some of which may be attributed to different locations).

Since the amount and type of nitrogenous fertiliser varies considerably, depending on crop rotation practices, the season, and the region or country, it is not surprising that there are some differences in resource energy and GGE results from LCAs carried out in Australia and internationally. For GGEs, this is further exacerbated by the range of values attributed to nitrous oxide emissions as a percentage of added fertiliser.

For ethanol production, comparison with other studies is complicated by uncertainties in how by-products have been credited, and in some cases by the use of petrol blends as the functional unit. In addition, many of the studies do not consider the CO_2 taken up by the grain through photosynthesis, which makes the GGEs for grain production negative.

Comparison of ethanol and petrol

Using current technology, the life cycle GGEs for ethanol are always less than those for petrol, with ethanol cases involving export electricity being very much lower. When a comparison is made with the 2050 scenario included, the projected use of CO_2 capture technologies further reduce the GGEs for the ethanol cases, compared to petrol.

Previous studies have compared ethanol and petrol on the basis of equivalent energy delivered - as fossil energy replacement.

Most US studies (based on corn) have shown that, on a fossil fuel basis, the production of ethanol from corn results in approximately 30% more energy than the fossil energy used in its production. The present study has shown similar results for the WDG case. DDGS results in a small negative net energy.

Anaerobic digestion (with electricity generation using gas internal combustion engines) gives a marked improvement in net energy -2.5-3x better than for WDG or from the previous studies.

Overall, ethanol is favoured over petrol as a transport fuel, on a resource energy and GGE basis. There are of course a number of other issues which need to be taken into account, such as availability, performance in the transport fleet, economics, *etc*.

9.2. Techno-economics

The techno-economic analysis shows the dominating role that the grain feedstock plays in the overall ethanol production economics - 50-80c/L of the ethanol production cost.

The next most significant issue is the choice of stillage processing – whether to produce WDG, DGGS or biogas/solid fuel for electricity production. In practice, the choice will also depend on the size, overall capital costs, by-product credits, and the ability to exploit opportunity biomass, such as straw.

Sorghum gives lower unit feed cost, but overall production costs are similar due to lower credits (higher level of starch in the sorghum produces a higher yield of ethanol, but less electricity and fertiliser credits).

Over the full range of cases considered, the cost of ethanol production varied over the range, 57-103 c/L for wheat, and 62-96 c/L for sorghum.

Electricity generation

The amount of power generated and exported is very dependent on the amount of stillage, the type of stillage processing, and the generation technology. For the alternative stillage processing options, the cost of ethanol production is:

- Increased by 3-12c/L for the alternative processing options to generate electricity (under base conditions).
- The AD-GTCC gives the lowest overall cost of the power generation, due to its high efficiency and lowest capital cost (particularly for generation plant over 50 MW).
- Lower, for power generation cases, when a value is attributed to GGE;
 - lowest (57c/L) for AD-GTCC, with the high energy cost case and \$30/t GGE.

The amount of electricity used by ethanol production is small compared to that which can be generated from stillage processing. This results in significant export electricity, particularly for the high efficiency generation technology. It is noted, that these higher efficiencies are not readily achievable at the scale chosen for the ethanol plant; however, these could be achieved with 2-3x larger ethanol plants (as are being constructed in the USA).

Transportation of WDG versus DDGS

This analysis shows that drying will cost around \$37-61/t DDGS depending on energy costs.

From a cost perspective, WDG can only be transported around 50-70 km before it is economically preferable to produce DDGS.

In allowing for the credits from the sale of distillers grain, it has been assumed that the product is dried to provide more flexibility in storage and use. Wet distillers grain, with its limited storage life, handling characteristics, significantly lower value, and reliance on local use, is likely to provide a lower co-product credit than the equivalent dried product. Overall, credits will depend on the marketability of the various products.

Plant location

From a economic risk management perspective, it will be necessary to take into account the availability of feedstock grain in a particular rural location (likely to be rather variable, due to drought cycles, and the increasing likelihood of lower rainfall in many grain growing regions, due to climate change). This will also impact on grain price; the level of economic impact will depend on contractual arrangements for grain feedstock. The higher cost of locating a plant near a port would be a small component of the overall plant cost, and be offset by infrastructure advantages.

There is therefore a strong driver for location of the ethanol plant adjacent to alternative sources of grain supply, *eg* imports or transfers from other regions of the country. This favours location at a port, as being planned by Primary Energy for plants at Kwinana, and Brisbane. For Primary Energy, the Kwinana site is also adjacent to the BP Refinery, with BP being a key customer for the ethanol.

The biodigestion of the stillage (thereby avoiding production of DDGS) avoids the issue of location, in the proximity of markets for the DDGS by-product. There is also the possibility that the oversupply of DDGS in USA is likely to introduce cheaper imported material and hence the profitability for Australian plants producing DDGS could be affected.

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